

Article

Reverse Water-Gas Shift Iron Catalyst Derived from Magnetite

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Abstract: The catalytic properties of unsupported iron oxides, specifically magnetite (Fe_3O_4), were investigated for the reverse water-gas shift (RWGS) reaction at temperatures between 723 K and 773 K and atmospheric pressure. This catalyst exhibited a fast catalytic CO formation rate ($35.1 \text{ mmol h}^{-1} \text{ g}_{\text{cat}}^{-1}$), high turnover frequency (0.180 s^{-1}), high CO selectivity ($> 99\%$), and high stability (753 K, $45000 \text{ cm}^3 \text{ h}^{-1} \text{ g}_{\text{cat}}^{-1}$) under a 1:1 H_2 to CO_2 ratio. Reaction rates over the Fe_3O_4 catalyst displayed a strong dependence on H_2 partial pressure (reaction order of ~ 0.8) and a weaker dependence on CO_2 partial pressure (reaction order of 0.33) under an equimolar flow of both reactants. X-ray powder diffraction patterns and XPS spectra reveal that the bulk composition and structure of the post-reaction catalyst was formed mostly of metallic Fe and Fe_3C , while the surface contained Fe^{2+} , Fe^{3+} , metallic Fe and Fe_3C . Catalyst tests on pure Fe_3C (iron carbide) suggest that Fe_3C is not an effective catalyst for this reaction at the conditions investigated. Gas-switching experiments (CO_2 or H_2) indicated that a redox mechanism is the predominant reaction pathway.

Keywords: RWGS; iron oxides; CO_2 conversion; gas-switching

1. Introduction

Today's anthropogenic emissions of carbon dioxide to the atmosphere amount to about 35,000 Tg per year, and the greenhouse effect of these accumulated emissions has been recognized as an alarming hazard to the well-being of modern societies. Although multiple approaches have been considered to mitigate these emissions, recently more emphasis has been placed on the potential synergy of carbon capture and the utilization of these large outflows of carbon dioxide. Among several possibilities, a recent National Academies of Science and Engineering report [1] on CO_2 waste gas utilization highlights the conversion of CO_2 by hydrogenation into CO and water—the reverse water-gas shift (RWGS) reaction, Equation (1)— as critical, and points to the need for improved catalysts with high stability and durability.

The RWGS reaction can be part of a two-step hydrogenation process for the conversion of CO_2 to valuable products. First, CO_2 is reduced to CO via the RWGS reaction, and second, CO can be converted to either hydrocarbons via the Fischer-Tropsch (FT) process or methanol via CAMERE (CARbon dioxide hydrogenation to form METHanol via a Reverse WGS reaction) process [2]. The RWGS reaction is an endothermic reaction ($\Delta H^\circ_{298 \text{ K}} = 41.2 \text{ kJ mol}^{-1}$), and thus is thermodynamically favorable at higher temperatures.



Noble metals such as Pt [3–5] and Pd [6,7], and other various metals such as Cu [8–11], Ni [12,13] and Fe [14] supported on oxides were reported to be active for the production of CO. Among them, Cu-based materials have been widely studied, and thus have also been investigated in many

instances for the RWGS reaction. For example, Cu-Ni/Al₂O₃ [15], Cu/ZnO [16], Cu-Zn/Al₂O₃ [16] and Cu/SiO₂ promoted with potassium [17] have all shown good RWGS activity. However, Cu materials tend to deactivate by sintering (fritting) at high temperatures ($T > 773$ K), which are required for high RWGS activity. For high temperature applications, iron can be added as a thermal stabilizer: Chen et al. [10] showed that adding small amounts of iron to 10% Cu/SiO₂ resulted in stable RWGS activity for 120 h at 873 K and atmospheric pressure, while non-promoted 10% Cu/SiO₂ deactivated rapidly.

Iron oxides (Fe_xO_y) are often used industrially for FT synthesis (473 K–623 K, 1 MPa) [18,19] and the high-temperature (623 K–723 K) WGS reaction [20–22]. In FT synthesis, alkali, iron-based catalysts are combined with Cu for reduction promotion. Schulz et al. [18,23] showed that the working FT catalysts contain several iron carbide phases and elemental carbon formed after the hydrogen reduction period. Iron oxides and the metallic iron are still present in the catalyst composition, but iron carbide phases are identified as active sites [23]. The RWGS and WGS reactions are often carried out in conjunction with FT synthesis at a higher temperature regime on iron catalysts, and iron oxide or oxidic amorphous iron phases are known as the active phases for WGS and RWGS [24–26].

Extensive research on iron-based catalysts has been reported mainly on the WGS reaction over decades [20]. Chromium is a structural promoter that helps prevent the iron from sintering at high temperature. A more recent survey on Cr-free, Fe-based WGS catalysts shows the current strong interest in this topic [27]. However, the studies on RWGS reactions over iron-based catalysts are much less frequent. Fishman et al. [28] synthesized hematite nano-sheets to obtain a 28% CO₂ conversion at 783 K, and hematite nanowires to obtain a 50% CO₂ conversion at a very high temperature of 1023 K. Hematite was reduced to magnetite during the reaction. The catalytic behavior over time on stream and the stability of the CO production were, however, not investigated. Fe nanoparticles have also shown good stability and activity (35% CO₂ conversion, > 85% CO selectivity) in RWGS by Kim et al. [29], yet no kinetic parameters were determined, and the mechanism was not discussed.

Two principal mechanisms of the WGS (or RWGS) reaction have been investigated extensively: The “redox mechanism” and the “associative” mechanism [30,31]. Different catalysts may lead to a different reaction pathway. The redox mechanism was suggested to be active for the WGS reaction over iron catalysts promoted with chromium [32]. A distinguishing feature of the redox mechanism is that products can be generated in the absence of both reactants. The catalyst is first reduced by the adsorbed H₂, and is subsequently oxidized by CO₂ (in RWGS) or H₂O (in WGS). The associative mechanism was proposed to be dominant in the WGS reaction over iron oxide catalysts [33]. In this mechanism, both reactants are adsorbed on the catalyst surface at the same time to create products. Several carbon-containing intermediates, including formate, carbonate, carbonyl and carboxyl species, have been proposed. In a previous report in alumina-supported iron catalysts [14], we showed that the redox mechanism is the only pathway for RWGS over Fe/ γ -Al₂O₃, and the predominant pathway over Fe-K/ γ -Al₂O₃. The addition of the potassium promoter activates a secondary pathway for CO formation, which is probably the associative pathway.

In the present report, unsupported Fe₃O₄-derived catalyst is identified as a highly active, selective and stable catalyst for the reverse water-gas shift reaction at temperatures between 723 K and 753 K. The characterization of surface composition, bulk properties, and the evaluation of the CO production specific rate showed that the working catalyst is constructed during the H₂-activation and the period of reaction conditions. Quantitative gas-switching experiments in combination with isotopic switching experiments allowed the redox and associative reaction pathway to be differentiated. The catalysts appear to be highly stable under the reaction conditions investigated.

2. Results and Discussion

The catalytic CO formation rates on the Fe₃O₄ catalyst with various H₂ to CO₂ ratios (Figure 1) show that after an induction period of ~120 min, the catalyst produced CO at a steady rate of 35.1 mmol h^{−1} g_{cat}^{−1} at 753 K with 12.5% CO₂ conversion. The selectivity to CO was greater than 99% under equimolar CO₂ and H₂. After 950 min, the partial pressure of CO₂ was raised to 60 kPa, while the partial pressure of H₂ was kept constant. The rate increased to 54.6 mmol h^{−1} g_{cat}^{−1} with 4.4% CO₂

conversion. Deactivation also occurred during this period: Starting at a deactivation rate of $3.71 \text{ mmol h}^{-1} \text{ g}_{\text{cat}}^{-1}$ per h, this rate gradually decreased to $0.23 \text{ mmol h}^{-1} \text{ g}_{\text{cat}}^{-1}$ per h. When the partial pressure of H_2 was 60 kPa, and the CO_2 was switched back to 15 kPa, the CO formation rate increased first to $91.3 \text{ mmol h}^{-1} \text{ g}_{\text{cat}}^{-1}$ and gradually stabilized to a value of $95.3 \text{ mmol h}^{-1} \text{ g}_{\text{cat}}^{-1}$ with 33.7% CO_2 conversion. The final rate of the catalyst reactivation was about $0.50 \text{ mmol h}^{-1} \text{ g}_{\text{cat}}^{-1}$ per h. It should be noted that the differential condition (see Equation (8)) was used to determine reaction rates, and preferred for the investigation of the kinetic properties of our materials. Under higher concentration of H_2 (15 kPa CO_2 + 60 kPa H_2), high CO_2 conversion (> 12%) could lead to small errors in the estimation of the reaction rate and the reaction order. The trend observed in Figure 1, however, should not be affected by this approximation.

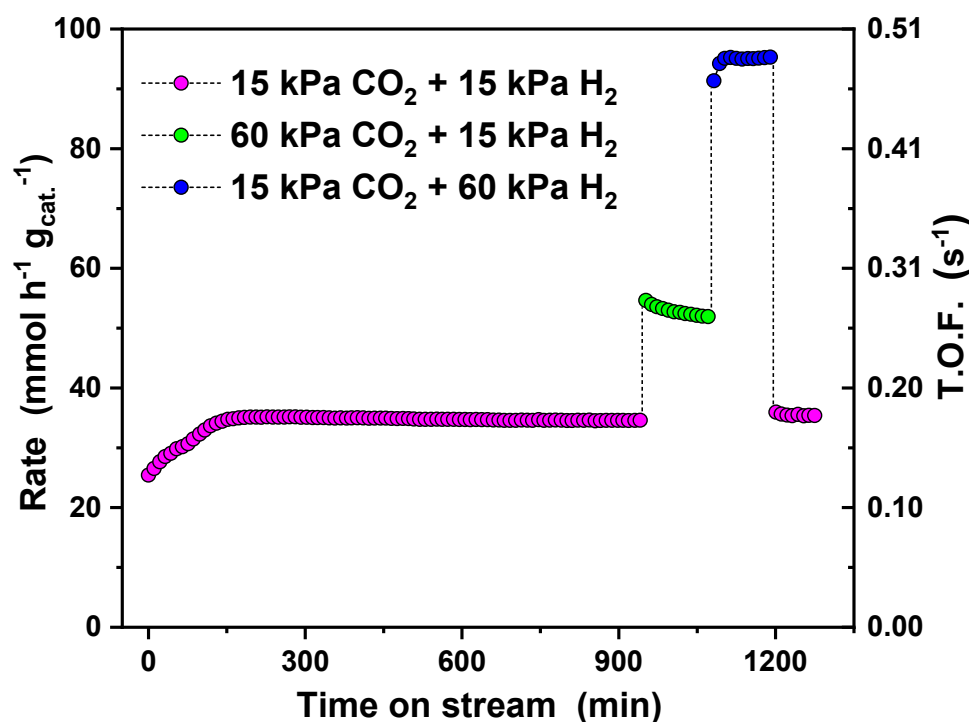


Figure 1. CO formation rates and their turnover frequencies (T.O.F.) on Fe_3O_4 at partial pressures of CO_2 and H_2 indicated in the legend. Other reaction conditions: $P_{\text{tot}} = 1 \text{ bar}$, $T = 753 \text{ K}$, $F_{\text{tot}} = 75 \text{ sccm}$, $\text{GHSV} = 4.5 \times 10^4 \text{ cm}^3 \text{ h}^{-1} \text{ g}_{\text{cat}}^{-1}$.

With 60 kPa of H_2 and 15 kPa of CO_2 in the feed, a small amount of CH_4 —the only side-product—was produced at the rate of $1.35 \text{ mmol h}^{-1} \text{ g}_{\text{cat}}^{-1}$, reducing the CO selectivity from near 100% to 98.6%. Methane production implies that C–H bond formation is facilitated at higher partial pressure of H_2 . There was no further C–C chain growth under this reaction condition, indicating that the FT synthesis was not active over the working catalyst. The effect of H_2 partial pressure on the CO formation rate was much higher than the effect of CO_2 , implying a higher reaction order on H_2 than CO_2 . The catalyst showed overall high stability in 1,300 min, and the final reactivation rate in excess H_2 was higher than the deactivation rate under the excess CO_2 condition. This indicates that this Fe_3O_4 -derived catalyst is easy to regenerate in a very short period (< 100 min), making the catalyst attractive in industrial use for long-term application.

The activation of the catalyst was carried out by a pretreatment under reducing conditions (H_2 gas). The bulk structure of the catalyst after the pretreatment can be identified. Based on the body-centered cubic (BCC) structure of $\alpha\text{-Fe}$ (JCPDS PDF 00-006-0696) after the pretreatment (Figure S1), the surface density of Fe atoms on the Fe(110) surface can be calculated as $1.297 \times 10^{19} \text{ Fe atoms m}^{-2}$. Assuming all Fe atoms on Fe(110) were active sites, the observed CO formation rates can be converted to turnover frequency (TOF). This is reported in Figure 1 based on the measured CO formation rates, atomic surface density, and BET surface area ($2.52 \text{ m}^2/\text{g}$ for Fe_3O_4) of the pristine catalyst. The

turnover frequency of this catalyst under the equimolar condition was as high as 0.18 s^{-1} ($P_{\text{tot}} = 1 \text{ bar}$, $T = 753 \text{ K}$, $F_{\text{tot.}} = 75 \text{ sccm}$, $\text{GHSV} = 4.5 \times 10^4 \text{ cm}^3 \text{ h}^{-1} \text{ g}_{\text{cat.}}^{-1}$).

The stable reaction rates observed after the initial break-in period at 753 K allow for the determination of kinetic parameters without having to model deactivation profiles. The kinetic parameters, including reaction orders with respect to CO_2 and H_2 , and measured activation energies (E_{meas}) over Fe_3O_4 under near equimolar CO_2 and H_2 (~1:1), and in H_2 excess (2:1, 4:1, and 9:1)—see Table 1— indicate that CO formation rates have a higher dependence on H_2 partial pressure (order of ~0.8) than CO_2 partial pressure (order of ~0.33) under equimolar composition. In general, rate orders depend on reaction conditions: Increasing the H_2 partial pressure increases the order on CO_2 to 0.39 and decreases the rate order on H_2 to 0.72. At a ratio of $\text{H}_2:\text{CO}_2$ near 4:1, the reaction orders still show the same trend: An increasing dependence on CO_2 (order of 0.43) and decreasing dependence on H_2 (order of 0.31). In a high excess of H_2 ($\text{H}_2:\text{CO}_2 = \sim 9:1$), the reaction rate over Fe_3O_4 was of the order 1.30 with respect to CO_2 , and was independent of H_2 pressure. The activation energies (E_{meas}) also depend on the $\text{H}_2:\text{CO}_2$ partial pressure ratios; that is, different reaction pathways may occur under these conditions. This behavior is not unique to iron catalysts. Similar reaction orders were also observed by Ginés et al. [34] in the same regime of $P_{\text{H}_2}/P_{\text{CO}_2} < 3$ (CO_2 order ≈ 0.3 , H_2 order ≈ 0.8) on the $\text{CuO}/\text{ZnO}/\text{Al}_2\text{O}_3$ catalyst, and by Kim et al. [3] on $\text{Pt}/\text{Al}_2\text{O}_3$ catalysts (CO_2 order = 0.32, H_2 order = 0.70). It was also suggested by Ginés et al. [34] that different reaction pathways should be existed for $P_{\text{H}_2}/P_{\text{CO}_2} < 3$ and $P_{\text{H}_2}/P_{\text{CO}_2} > 3$ regions.

Table 1. Measured reaction orders with respect to CO_2 and H_2 , and measured activation energies (E_{meas}) over Fe_3O_4 . Reaction conditions: 100 mg Fe_3O_4 , $F_{\text{tot}} = 75 \text{ sccm}$, $T = 723 \text{ K}$.

P_{H_2} (kPa)	P_{CO_2} (kPa)	$P_{\text{H}_2} : P_{\text{CO}_2}$	Reaction order in CO_2	Reaction order in H_2	E_{meas} (kJ/mol)
15	10–20	~ 1:1	0.33	-	28.9 ± 0.9
10–20	15		-	0.79	
30	10–20	~ 2:1	0.39	-	27.1 ± 0.5
25–35	15		-	0.72	
40	5–12.5	~ 4:1	0.43	-	34.2 ± 1.9
35–45	10		-	0.31	
85	5–12.5	~ 9:1	1.30	-	39.0 ± 3.4
70–90	10		-	0	

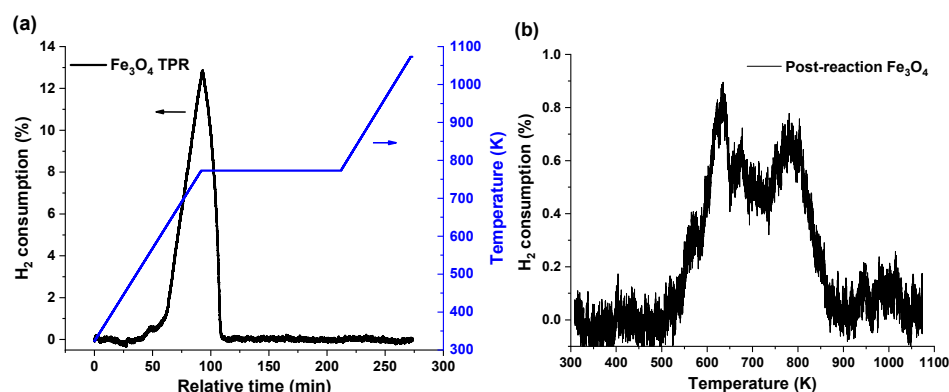


Figure 2. (a) H₂ consumption (%) of the reduction period during the pretreatment following the temperature-programmed reduction (TPR) of 100 mg Fe₃O₄. (b) TPR curve of the post-reaction Fe₃O₄ sample.

Figure 2 presents the temperature-programmed reduction (TPR) profiles of (a) the fresh Fe₃O₄ sample and (b) the post-reaction Fe₃O₄ sample. In Figure 2(a), the fresh Fe₃O₄ was heated to 753 K in a hydrogen atmosphere, kept for 2 h at these conditions, and then heated to 1,073 K at the rate of 5 K/min. The small peak observed in the TPR trace at about 563 K is assigned to an impurity of hematite present in the initial sample of magnetite (Fe₃O₄), but not detected in the XRD pattern, as shown in the report by Jozwiak et al. [35]. The following broader and asymmetric peak suggests a two-step reduction process that has been previously postulated in literature [36], as the following: (1) $Fe_3O_4 \xrightarrow{H_2} FeO$ and (2) $FeO \xrightarrow{H_2} Fe^0$. These two steps can be deconvoluted into two peaks located at ~688 K and 773 K in the TPR traces. After the 2 h reduction period at 773 K, there was no further H₂ consumption at higher temperatures. That is, the sample, after the reduction pretreatment used in our activation protocol, has been converted into metallic iron. This result is also consistent with the XRD pattern in Figure S1, which shows that α -Fe was the crystal formed after the reduction pretreatment of the Fe₃O₄ sample in the microreactor.

As soon as CO₂ was fed into the reactor, the surface of the catalyst was partially oxidized. This is known from the results of Figure 2(b) that illustrates the presence of two significant peaks in the TPR profile for the post-reaction catalysts (at 630 K and 780 K, respectively). The location of these two predominant peaks shows good agreement with the results of Figure 2(a) and results reported elsewhere [35,37]. There is at least a two-step reduction at ~630 K and 780 K, implying the coexistence of different oxidation states of iron on the post-reaction sample due to the partial oxidation from CO₂. For this post-reaction sample, the H₂ concentration in the effluent stream decreased by only a small amount (less than 1%), suggesting that the consumption of the H₂ feed would not affect the reduction rate during the TPR reaction.

Figure 3 displays the diffraction pattern of fresh Fe₃O₄ and the catalyst after the RWGS reaction (post-reaction Fe₃O₄). The 2 θ degree peak positions in fresh Fe₃O₄ were 30.15°, 35.45°, 37.15°, 43.15°, 53.50°, 56.95° and 62.55°, which are all consistent with magnetite (JCPDS PDF 01-071-6336). The post-reaction Fe₃O₄ shows a very different XRD pattern: This pattern was composed of metallic iron (α -Fe, 44.67°, shown in the inset of Figure 3), iron carbide (Fe₃C), and a small peak of FeO_x (35.47°).

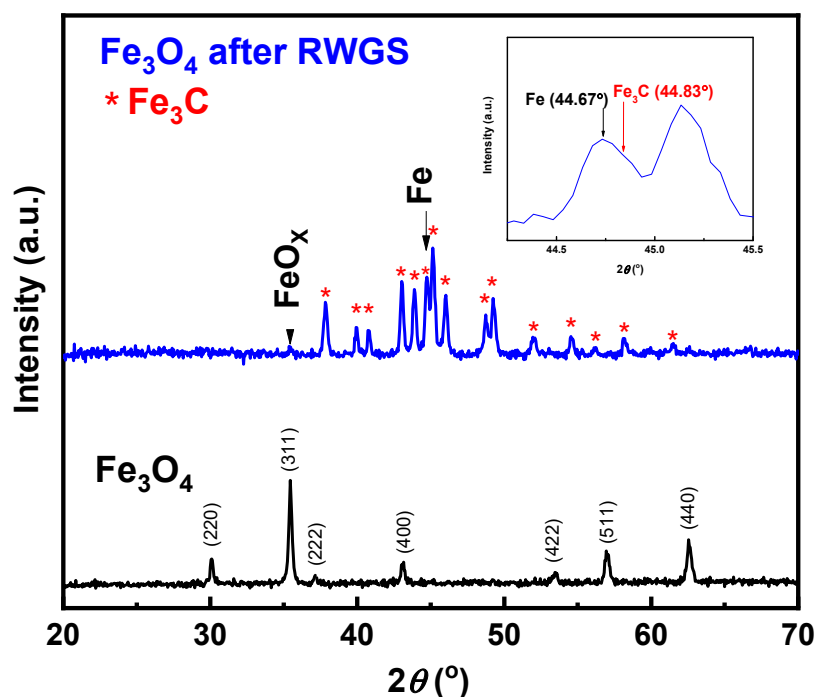


Figure 3. XRD patterns of fresh Fe_3O_4 (down) and post-reaction Fe_3O_4 (up); inset is the magnification of post-reaction Fe_3O_4 from 44° to 45.5° .

Iron oxides can be converted directly into carbides in a reducing and carburizing atmosphere [38], and the carbon source of the Fe_3C production can be either from impurities in the fresh Fe_3O_4 sample or due to reaction with the product CO , after the RWGS reaction as indicated by Equation 2[39]:



The bulk composition of the catalyst after the reaction is also consistent with the TPR results in Figure 2 (a) and (b). During TPR, the amount of H_2 consumption of magnetite relative to the amount of H_2 consumption after the reaction was 12:1, therefore the iron species in the catalyst has been changed into a more reduced chemical state after the pretreatment and RWGS reaction. The reduction was mainly caused by the pretreatment, while the following CO_2/H_2 reaction shifted the metallic iron back to a slightly more oxidized state; a combination of iron carbide, metallic iron and some iron oxides.

Besides bulk property information obtained from XRD, XPS analyses were conducted to characterize the surface composition of the initial fresh Fe_3O_4 and the change of the catalyst after the RWGS reaction. Figure 4 shows the XPS spectra, peak deconvolutions and the fitting envelopes for the $\text{Fe } 2p_{3/2}$ spectra of Fe_3O_4 and post-reaction Fe_3O_4 .

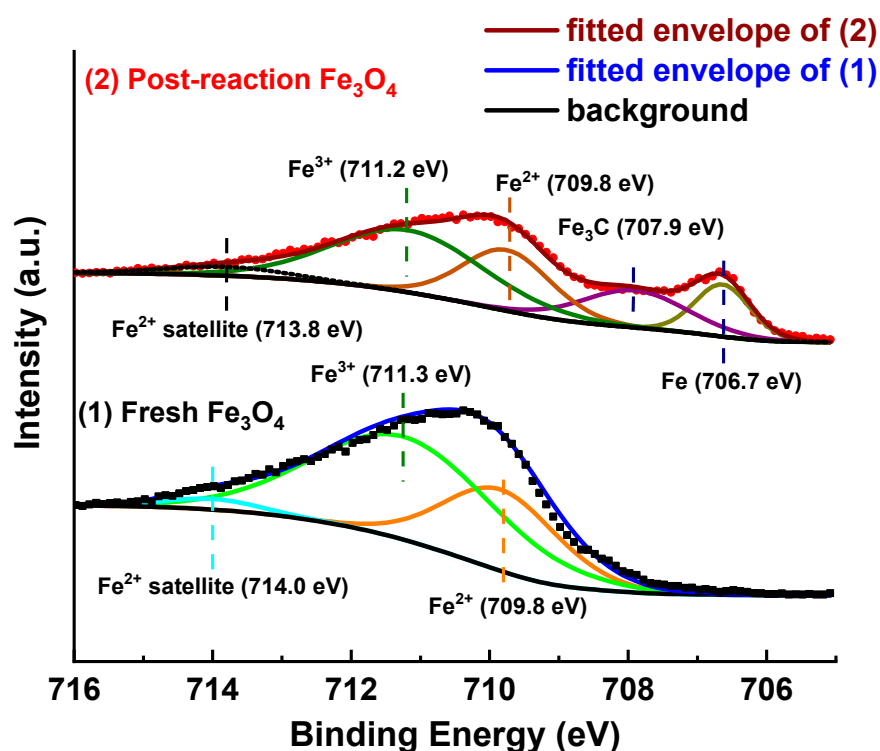


Figure 4. XPS Fe $2p_{3/2}$ spectra of Fe_3O_4 and post-reaction Fe_3O_4 . The curves under the fitted envelope and above the background are contributions of estimated components from peak fitting.

Atomic percent contributions are calculated from the fitted peaks of Fe $2p_{3/2}$ due to its larger intensity (Area of Fe $2p_{3/2}$: Fe $2p_{1/2}$ = 2:1). The Fe $2p_{3/2}$ spectra were fitted over the range of 705–722 eV. The spectra between 716–722 eV were not shown in the figure for clarity. In this range, there were only small Fe^{3+} satellite peaks located at 719.2 eV and 719.4 eV for both the fresh and post-reaction Fe_3O_4 samples, respectively, although the area of the satellite peaks was still included in the corresponding components when calculating the relative atomic percentage. The fits, including the binding energy, full width at half maximum (FWHM), and the relative iron composition, are summarized in Table 2. The fitted XPS spectrum of fresh Fe_3O_4 was composed of doublets for Fe^{2+} at 709.8 eV and Fe^{3+} at 711.3 eV. Fe_3O_4 has an inverse spinel structure which can be written as $\text{Fe}^{3+}_{\text{TET}}[\text{Fe}^{2+}\text{Fe}^{3+}]_{\text{OCT}}\text{O}_4$, with one Fe^{3+} on a tetrahedral site, and Fe^{2+} and the other Fe^{3+} distributed on octahedral sites. Therefore, the theoretical relative composition of $\text{Fe}^{2+}/\text{Fe}^{3+}$ is 0.5, which is close to the area fitted and the calculated relative composition in our fresh Fe_3O_4 (Fe^{2+} : Fe^{3+} = 34.8/65.2 = 0.53). The Fe^{3+} peak has a larger FWHM than Fe^{2+} . This is as expected because the electronic configuration of Fe^{2+} is $3d^6$, while that of Fe^{3+} is $3d^5$, that is, Fe^{2+} will have a longer life time compared to Fe^{3+} ; and therefore the FWHM of the Fe^{2+} peak should be smaller than the Fe^{3+} peak [40]. Additionally, the Fe^{3+} peaks can be attributed to two different structures, octahedral Fe^{3+} and tetrahedral Fe^{3+} , a factor that will also lead to broader Fe^{3+} peaks.

Table 2. XPS peak fittings for Fe 2p_{3/2} spectra for Fe₃O₄ and post-reaction Fe₃O₄.

Sample	Peak Deconvolution	Binding Energy (eV)	FWHM (eV)	Atomic %
Fe ₃ O ₄	Fe ³⁺	711.3	3.08	65.2
	Fe ²⁺	709.8	1.95	34.8
post-reaction Fe ₃ O ₄	Fe ³⁺	711.2	2.58	43.9
	Fe ²⁺	709.8	1.51	27.5
	Fe ₃ C	707.9	1.78	16.4
	Metallic Fe	706.7	0.94	12.2

After the RWGS reaction, the spectrum was fitted using four different components corresponding to metallic Fe (706.7 eV), Fe₃C (707.9 eV), Fe²⁺ (709.8 eV) and Fe³⁺ (711.2 eV). The peak locations of Fe²⁺ and Fe³⁺ were the same or very close to the fresh sample, indicating that there was only a small surface charging effect with the flood gun on. The binding energies of the components are in agreement with literature results [38,40–42]. In terms of the atomic percentages, the overall peak area was re-allocated to a more reduced regime after the RWGS reaction. The Fe²⁺ decreased from 34.8% to 27.5%, the Fe³⁺ decreased from 65.2% to 43.9%, while there were two components formed: Fe (12.2%) and Fe₃C (16.4%). The shift of the spectra was due to the H₂ reduction pretreatment before operating the RWGS reaction, and the flow of H₂/CO₂ reactants through the system would balance each other to make the catalyst partially oxidized or reduced. Though the sample surface could be oxidized by the air during the transportation from the reactor to the XPS analysis chamber, the result from XPS still can confirm the reduction of the surface during the reaction, since new crystal structures such as Fe and Fe₃C are detected by XRD.

The XPS analyses indicate that the active catalyst consisted of a mixture of metallic Fe, Fe₃C, Fe²⁺ and Fe³⁺; however, it cannot establish the relative contributions of these components to the observed rate of the RWGS reaction. To determine if the iron carbide formed in our reaction can catalyze the RWGS reaction, reaction rates over pure Fe₃C were measured (Figure 5). In Figure 5(a), Fe₃C showed an initial CO formation rate of 26.0 mmol h^{−1} g^{−1}, but dropped 48% to near 13.5 mmol h^{−1} g^{−1} in 10 min, and then further down to 5.7 mmol h^{−1} g^{−1} in 160 min at 753 K. This is clearly different from the properties of the Fe₃O₄-derived catalyst in Figure 1, since the Fe₃O₄-derived catalyst displayed high stability for at least 1,300 min. To evaluate the fast deactivation shown in Figure 5(a) and remove the initial reduction effect during the ramping by hydrogen, another measurement was carried out with respect to temperature, (see Figure 5(b)). This experiment was conducted flowing a CO₂/H₂/He gas mixture in the same relative concentration used in the standard activity test during the ramping procedure from room temperature to 773 K. At 573 K, the material did not catalyze the formation of CO; however, when the temperature was increased to 623 K, the catalyst immediately showed catalytic rates in the range of 2.60 mmol h^{−1} g^{−1} to 2.99 mmol h^{−1} g^{−1}. After 1 h of the reaction, the rate remained at quasi-steady state at this low temperature (623 K).

The CO formation rates were $6.60 \text{ mmol h}^{-1} \text{ g}^{-1}$, $9.80 \text{ mmol h}^{-1} \text{ g}^{-1}$, and $9.16 \text{ mmol h}^{-1} \text{ g}^{-1}$, as the temperature was increased to 673 K, 723 K and 773 K, respectively. The formation rate at 773 K was not higher than that at the lower temperature because of rapid deactivation at this temperature. Faster deactivation rates were observed at higher temperatures: The average deactivation rates were $1.36 \text{ mmol h}^{-1} \text{ g}^{-1} \text{ per h}$, $2.57 \text{ mmol h}^{-1} \text{ g}^{-1} \text{ per h}$ and $3.50 \text{ mmol h}^{-1} \text{ g}^{-1} \text{ per h}$.

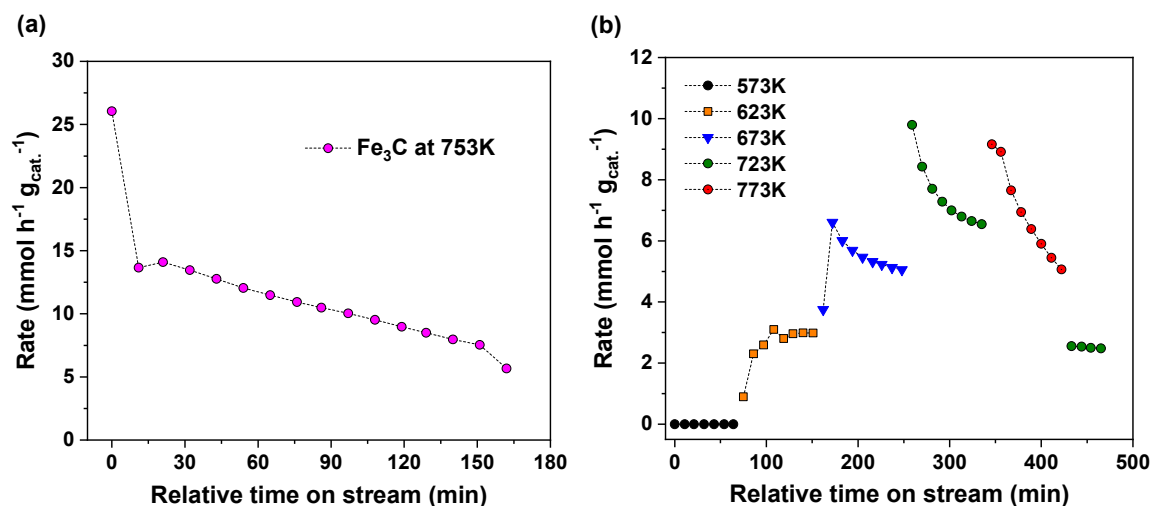


Figure 5. (a) CO formation rate on 100 mg Fe₃C. Reaction conditions: $F_{\text{tot}} = 75 \text{ sccm}$; the reactor was ramped to 753 K with $P_{\text{H}_2} = 15 \text{ kPa}$ and He as remainder. No further reduction was applied after the ramping. During the reaction, $T = 753 \text{ K}$, $P_{\text{tot}} = 1 \text{ bar}$, $P_{\text{H}_2} = P_{\text{CO}_2} = 15 \text{ kPa}$. (b) CO formation rate on 100 mg Fe₃C. The temperature was directly ramped from room temperature to 773 K as shown in the figure with $P_{\text{tot}} = 1 \text{ bar}$, $P_{\text{H}_2} = P_{\text{CO}_2} = 15 \text{ kPa}$, and the remainder is He.

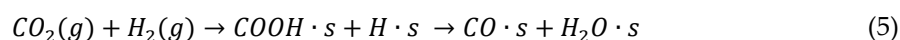
After reacting at 773 K, the temperature was reduced to 723 K to monitor the reaction rate and compare to the previous value. Much lower rates ($2.55 \text{ mmol h}^{-1} \text{ g}^{-1}$) were observed than in the previous measurement at the same temperature (723 K), indicating that there was an irreversible change in the catalyst structure or composition. At higher temperatures, the reverse reaction of Equation 2, where Fe₃C reacts with CO₂ and forms Fe and CO, is more favorable than the Fe₃C formation [39]. Therefore, the initial CO formation rate was probably due to the formation of CO from decomposition, but quickly dropped since it is harder to convert the metallic iron back to Fe₃C at higher temperatures. The iron carbide catalyst only showed steady CO production at 623 K. This explains why the deactivation at 723 K over Fe₃C is very different from the steady-state magnetite catalyst reported in Figure 1, which showed a very stable CO formation rate at 753 K. This observation suggests that the operating temperature of RWGS in this study was not an environment conducive for a stable iron carbide for CO production. In addition, the iron carbide (Fe₅C₂ or Fe₃C) is normally considered to be the active phase of iron for hydrocarbon production [43,44], and iron oxide is the active phase for WGS and RWGS [25]. Several reports have suggested that the stability of the iron catalyst in either FT synthesis [45] or RWGS [29] can be related to an iron carbide layer. Davis [45] suggested that catalyst composition and reaction condition will define the existence of the pseudo-equilibrium layer of iron carbide to ensure a very slow deactivation condition. Kim et al. [29] concluded that the stability of the catalyst could have originated from migration of C and O into the catalyst bulk, forming iron oxide and iron carbide, which likely prevented the nanoparticles on the surface from agglomerating. Based on the XPS results and Fe₃C catalytic tests, the iron carbide of the working catalyst is less likely to be the main active site for CO production, but is an important species to provide stability in the overall catalytic performance.

Gas-switching experiments, in which H₂ and CO₂ are flown on and off, were used to distinguish and quantify contributions from redox and associative reaction pathways [3,14,46]. In the simplest form of the redox mechanism, gas-phase CO₂ adsorbs on a reduced site to form CO and an oxidized

site (Equation 3), which can then be reduced by gas phase H_2 to reform the reduced site (Equation (4)). The simplest redox cycle can be described as follows:



A simplified associative pathway can be described generally by Equation 5. CO_2 and H_2 adsorb on the catalyst surface to form a carbon-containing intermediate (i.e. formate, carbonate, or bicarbonate), which then decomposes in the presence of H_2 to form CO and H_2O .



CO and H_2O were the main products formed during gas-switching experiment (Figure 6). In the first three cycles, CO was formed when switching from H_2 to CO_2 , and a very small amount of CO was formed when switching from CO_2 to H_2 at 30 min, 70 min and 110 min, respectively. When the catalyst was purged 20 min with helium before switching from CO_2 to H_2 , CO was not formed, and H_2O was produced at 195 min. Water was formed when switching from H_2 to CO_2 and when switching from CO_2 to H_2 . After flowing H_2 and purging the reactor with He for 20 min, only a negligible amount of H_2O was formed upon the admission of CO_2 (at 150 min).

In Figure 6, the fact that CO was formed when the reduced form of the Fe_3O_4 catalyst was contacted with CO_2 , (even after the purge with He to decrease the concentration of any surface H_2), is evidence of a redox pathway. During the first 125 min of gas-switching experiments, H_2O was produced during flows of only CO_2 or only H_2 . This differs from what is expected in the traditional redox cycle, in which H_2O is only produced during the H_2 feeding period (see Equation 4). However, after flowing H_2 and purging the reactor with He for 20 min, the admission of CO_2 only produced negligible amounts of water. Table 3 summarizes the estimated initial rates of CO production on the Fe_3O_4 catalyst during each segment of the gas-switching experiments. The CO production rates were calculated from the initial slopes of the concentration vs. time data in Figure 6, essentially modeling the system as a batch reactor (Equation. 6).

$$\frac{dC_A}{dt} = r_A \quad (6)$$

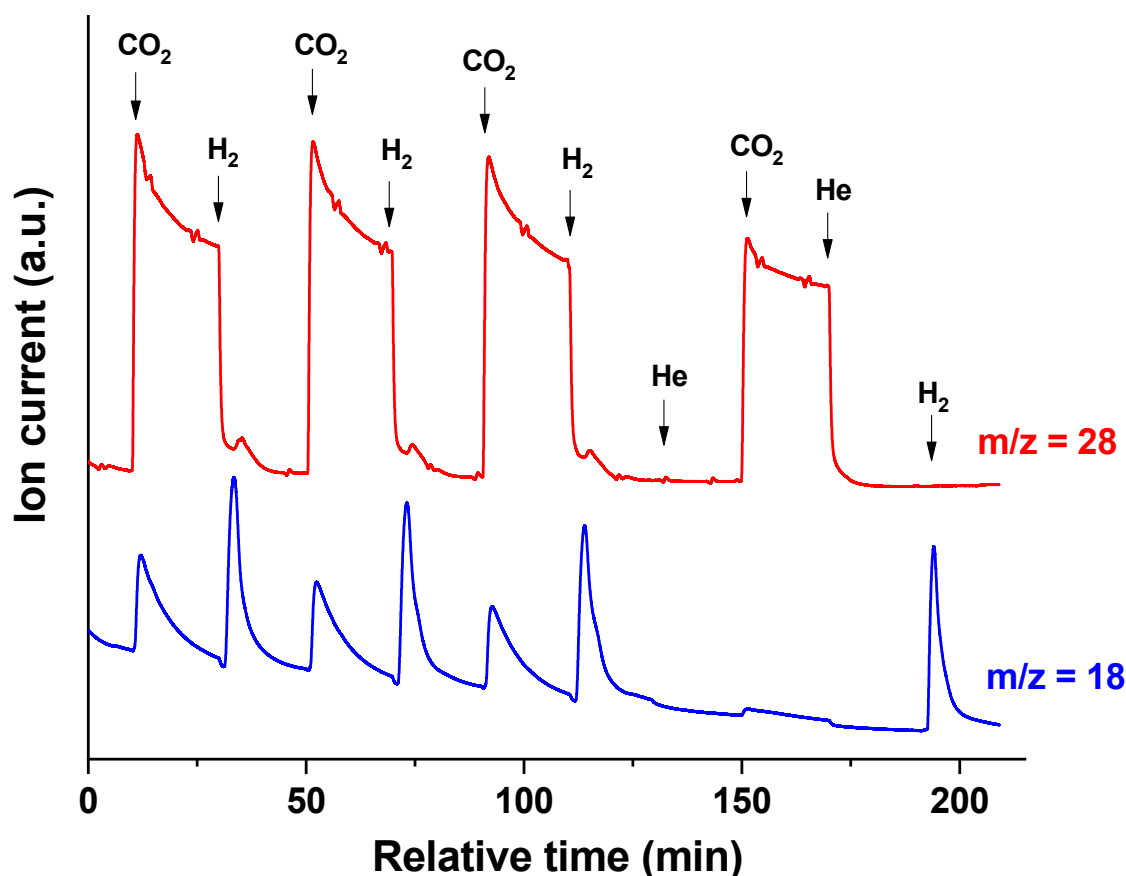


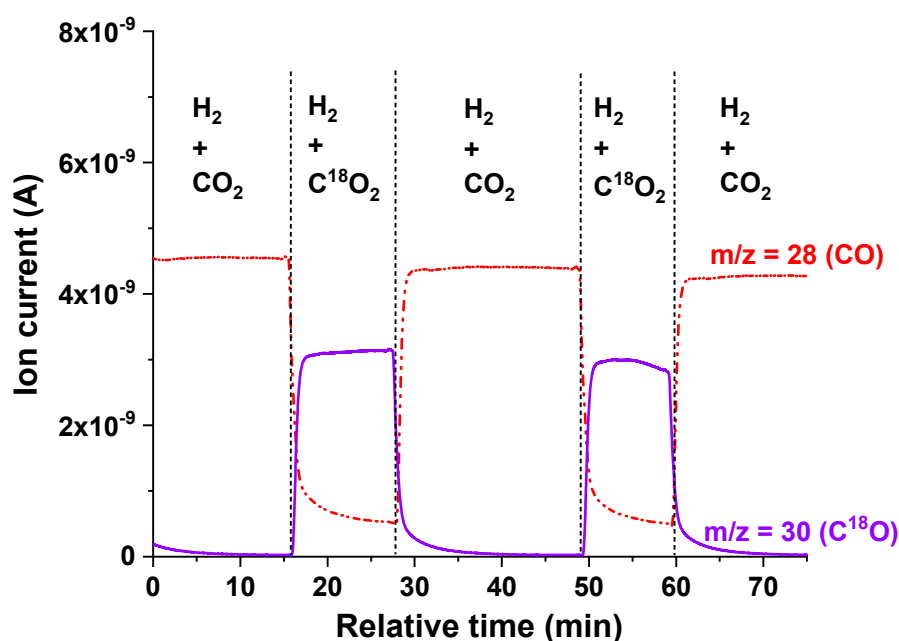
Figure 6. Ion current at $m/z = 18$ (H_2O) and 28 (CO) during H_2/CO_2 switching experiments on Fe_3O_4 . Arrows with a label indicate a change in gas composition to the indicated gas. The catalyst first was reduced in flowing H_2 for 2 h, following the reaction in H_2 and CO_2 for 2 h, and H_2/He in 20 min before the first admission of CO_2 . Reaction conditions: $T = 773 \text{ K}$, $F_{\text{He}} = 36 \text{ sccm}$, F_{H_2} or $F_{\text{CO}_2} = 4 \text{ sccm}$.

It is observed (Table 3) that the rate after switch from H_2 to CO_2 fluctuated between $2.74 \mu\text{mol L}^{-1} \text{ s}^{-1} \text{ g}_{\text{cat}}^{-1}$ and $2.98 \mu\text{mol L}^{-1} \text{ s}^{-1} \text{ g}_{\text{cat}}^{-1}$ in the first three periods of CO_2 admission, and it decreased after the He purge. The rate after switching from CO_2 to H_2 decreased in the first three periods, and it was zero (with no CO produced) during the last admission of CO_2 after the He purge. The decrease of the CO initial rate after switching from CO_2 to H_2 , especially when equal to zero after the purge, raises doubts about the existence of residual CO_2 during the first three admissions of H_2 in the switching experiment. As a control, when the gas was switched from CO_2 to H_2 , the CO_2 gas did not exit from the surface very quickly (see Figure S2). Therefore, a small amount of CO can be produced by the residual CO_2 with the available reduced sites; evidence of this interpretation in the detection of very small peaks after the H_2 admissions (Figure 6). The negligible CO production (relative time = 34 min, 74 min, and 114 min, respectively) after the H_2 admissions should not be considered evidence of the associative mechanism. In summary, the CO formation upon switching from H_2 to CO_2 is evidence consistent with the redox mechanism, while the small contribution of CO production upon switching from CO_2 to H_2 was suppressed by the confirmation of the helium purge. Thus, from the gas-switching experiment, only the redox pathway is active on our Fe_3O_4 -derived catalyst.

Table 3. Estimated initial rates of CO production after gas switches from H₂ to CO₂ and from CO₂ to H₂ during gas-switching experiment on Fe₃O₄ in Figure 6.

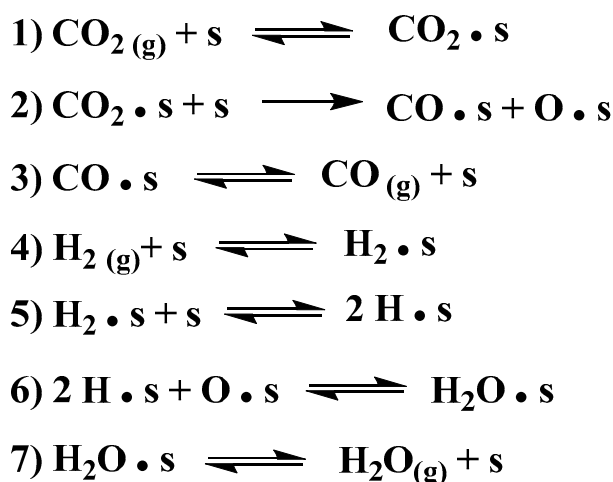
Period	Rate after H ₂ to CO ₂ gas switch ($\mu\text{mol L}^{-1} \text{s}^{-1} \text{g}_{\text{cat}}^{-1}$)	Rate after CO ₂ to H ₂ gas switch ($\mu\text{mol L}^{-1} \text{s}^{-1} \text{g}_{\text{cat}}^{-1}$)	(H ₂ to CO ₂ rate)/(CO ₂ to H ₂ rate) ratio
1 st CO ₂	2.78	1.64	1.70
2 nd CO ₂	2.98	1.00	2.98
3 rd CO ₂	2.74	0.91	3.01
4 th CO ₂ (after He purge)	1.94	0	-

Isotopic experiments were conducted to gain insight into the mechanism of the reaction. The isotopic C¹⁸O₂ to the CO₂ switching experiment is shown in Figure 7. Here it can be seen that C¹⁸O ($m/z = 30$) formed and CO ($m/z = 28$) decreased when the gas (CO₂/H₂) was switched to C¹⁸O₂/H₂. CO can be only formed from CO₂, and not from the lattice oxygen.

**Figure 7.** Ion current at $m/z = 28$ (CO) and 30 (C¹⁸O) during CO₂/C¹⁸O₂ switching experiments on Fe₃O₄ (100 mg). Labels in each region indicate a change in gas composition. A standard pretreatment (reduced in flowing H₂ for 2 h) and RWGS reaction (> 2 h) had been done before the switching experiment. Switching experiment conditions: $T = 753 \text{ K}$, $F_{\text{tot}} = 40 \text{ sccm}$, $F_{\text{H}_2} = 4 \text{ sccm}$, F_{CO_2} or $F_{\text{C}^{18}\text{O}_2} = 4 \text{ sccm}$.

The gas-switching experiments with CO₂ and H₂ led us to conclude that a redox pathway is active on the Fe₃O₄-derived catalyst. A model that can present a redox reaction pathway for this catalyst is given in Scheme 1. It includes the adsorption of both of the reactants, CO₂ and H₂. In the surface redox mechanism, the dissociation of CO₂ at the catalyst surface (step 2 in Scheme 1) is known to be the RDS [8,30,34]. Evidence for H₂ dissociation (step 5 in Scheme 1) was observed when H₂/D₂ mixtures were fed to the catalyst in the presence of CO₂ (see Figure S3).

HD formation was observed to occur quickly, since the amount of CO₂ to CO conversion decreased on the same time scale when switching the concentration from H₂/D₂ (7.5kPa/7.5kPa) to H₂ (7.5 kPa), indicating that H₂ dissociation is reversible and not rate limiting.



Scheme 1. Redox reaction pathway for CO formation.

An additional gas switching experiment was conducted to monitor the H₂O production (Figure S4). The amount of H₂O produced during H₂ flow periods was consistent between each cycle (Figure S4(a)), that is, the adsorbed O·s species formed upon CO₂ reduction are stable at these reaction conditions. However, the amount of H₂O produced during the period of CO₂ flow decreased as the purge time in helium increased. After only a five min purge, the amount of H₂O produced during the period of CO₂ flow was much greater than that produced following a 20 min purge in helium, and the rate fitted from the initial slope of this region dropped dramatically (see Table S1). This suggests that H* atoms from the catalyst surface appeared to desorb (as H₂) during the He purge. This was a slow process, because even following a 20 min purge, there were enough H* atoms on the sample to form small amounts of H₂O when CO₂ was administered. Both gas-switching experiments (Figure 6 and Figure S4) suggest that the redox mechanism should be the dominant reaction pathway for this Fe₃O₄-derived catalyst during the CO₂ hydrogenation at our reaction conditions (753 K, 1 atm).

3. Materials and Methods

3.1. Materials

Magnetite (Fe₃O₄, 99.99%, 50–100 nm particle size, Sigma-Aldrich, St. Louis, MO, USA) powder was pressed by hydraulic press and sieved (mesh 40 to mesh 60) to obtain particle sizes within the range of 250–425 μm before the reaction. Iron carbide (Fe₃C, 99.5%, American Element, Los Angeles, CA, USA) granules were crushed to a powder using a ball-mill, pressed using a hydraulic press, and sieved within the range of 250–425 μm. The gases used were CO₂ (Grade 5.0, Keen, Wilmington, DE, USA), H₂ (UHP, Matheson, Basking Ridge, NJ, USA), Helium (Grade 5.0, Keen, Wilmington, DE, USA), C¹⁸O₂ (95 atom% ¹⁸O, Sigma-Aldrich, St. Louis, MO, USA), and D₂ (99.6% gas purity, 99.8% isotope purity, Cambridge Isotopes, Tewksbury, MA, USA).

3.2. Reactor setup for kinetics and gas-switching experiments

The reaction rates and other kinetic parameters were measured using a packed-bed microreactor operated in a down-flow mode at atmospheric pressure. The catalyst particles were supported on a plug of quartz wool within a 7 mm I.D. quartz tube reactor. The quartz tube was positioned inside an Omega CRFC-26/120-A ceramic radiant full cylinder heater. The temperature was controlled by an Omega CN/74000 temperature controller using the input from a K-type, 1/16 in. diameter thermocouple (Omega Engineering, Inc., Norwalk, CT, USA) placed around the outside of the quartz

tube at the center of the catalyst bed. Gas flows were controlled by mass flow controllers (Brooks Instruments) through the reactor or the other instruments.

Gas transfer lines were heated to a temperature above 373 K at all times to avoid water condensation. The composition of the effluent stream was analyzed online by a gas chromatograph (GC, 7890A, Agilent, Santa Clara, CA, USA) during continuous flow experiments or by a mass spectrometer (MS, GSD320, Pfeiffer Vacuum Technology AG, Aßlar, Germany) during gas-switching experiments or isotopic experiments. The GC was equipped with both a thermal conductivity detector (TCD) and a flame-ionization detector (FID). The TCD was used to quantify CO₂, CO and H₂ concentrations, while the FID was used to quantify hydrocarbon concentrations. An Agilent 2 mm ID × 12 ft Haysep Q column was used in the GC to separate products quantified with the TCD, and an Agilent 0.32 mm ID × 30 m HP-Plot Q column was used to separate products quantified with the FID.

3.3. Catalyst Characterization

Temperature-programmed reduction (TPR) was performed by using a MS including the reduction period (773 K, P_{tot} = 1 bar, P_{H₂} = 15 kPa in He for 2 h), and then the temperature was ramped up to 1,073 K. The ramping rate of each step was 5 K min^{−1}. Another TPR experiment was performed after the reverse water-gas shift (RWGS) reaction (553 K, P_{tot} = 1 bar, GHSV = 4.5 × 10⁴ cm³ h^{−1} g_{cat.}^{−1}, P_{CO₂} = P_{H₂} = 15 kPa with He as an inert balance gas). The post-reaction sample was cooled down to room temperature in He flow inside the microreactor. The TPR was then continued in 15 kPa H₂ and 86.3 kPa He from room temperature to 1073 K at the rate of 5 K min^{−1}. The H₂ consumption was converted from the ion current (m/z = 2) after the calibration of the H₂ signal each time before the experiment using a mass spectrometer.

X-Ray Diffraction (XRD) patterns of catalyst powders were collected at room temperature on a Bruker diffractometer using Cu Kα radiation (λ = 1.5418 Å). Measurements were taken over the range of 5° < 2θ < 70°, with a step size of 0.02° before and after the RWGS reaction. X-ray photoelectron spectroscopy (XPS) measurements were performed on a K-alpha Thermo Fisher Scientific spectrometer using a monochromated Al Kα X-ray source. The measurements of iron oxide samples (pre- and post-reaction) were done with a spot size of 50 μm at ambient temperature and a chamber pressure of ~10^{−7} mbar. A flood gun was used for charge compensation. All the spectra measured were calibrated by setting the reference binding energy of carbon 1s at 284.8 eV. The spectra were analyzed by Thermo Fisher Scientific (Waltham, MA, USA) Advantage® commercial software (v5.986). For the fitting, each component consists of a linear combination of Gaussian and Lorentzian product functions, and the full width at half maximum (FWHM) and differences in binding energy of the same species between the Fe2p_{3/2} and Fe2p_{1/2} scan were kept constant. SMART background in Advantage® was used over the region to define the peaks.

3.4. Measurement of product formation rates and reaction rates with gas-switching or isotopic experiments

Most of the procedures in the measurement of the reaction rates, gas-switching, or isotopic experiments are identical to the ones described in our previous report [14]. Fe₃O₄ samples were pretreated before all experiments by increasing the reactor temperature at a rate of 5 K min^{−1} to 773 K under a gas flow of 15 kPa H₂. After the pretreatment at 773 K for 2 h, the temperature was lowered to the initial reaction temperature of 753 K. During the measurement of the reaction rates, the partial pressures of the reactants were P_{CO₂} = P_{H₂} = 15 kPa. A constant total flow rate of 75 cm³ min^{−1} (sccm) was maintained with He as an inert balance gas.

Gas hourly space velocity (GHSV) in cm³ h^{−1} g_{cat.}^{−1} was calculated under STP condition (273 K and 1 atm) according to the equation below:

$$GHSV = \frac{F_{tot}}{m_{cat.}} \quad (7)$$

where $m_{cat.}$ is the mass of the catalyst and F_{tot} is the total flow rate.

CO₂ and H₂ reaction orders were measured by independently varying the inlet CO₂ and H₂ partial pressures. The total pressure remained at 1 bar. The activation energy was estimated by using the Arrhenius plot with the temperature varied between 723 K and 773 K while monitoring the CO formation rate.

Rates of CO formation were calculated assuming differential reactor operation according to Equation 8:

$$r_{CO} = \frac{\dot{V} \Delta C_{CO}}{m_{cat.}} \quad (8)$$

where $\dot{V}$ is the total volumetric flow rate, ΔC_{CO} is the change in CO concentration. Measured reaction rates are the net rate of the forward and reverse reactions; therefore, the observed rate must be transformed into the reaction rate for the forward reaction by using Equations 9–11. The equilibrium constant (K_C) is low (< 1) for the RWGS at the temperatures investigated, although the reverse reaction had a negligible contribution to the observed rates because of the low conversion ($< 12\%$) under conditions at which the reactor was operated. Note that C_o (Equation 11) represents the standard state (1 mol L⁻¹) and equals 1, since the reaction is equimolar.

$$r_{obs.} = r_+ - r_- = r_+(1 - \eta) \quad (9)$$

$$\eta = \frac{[CO][H_2O]}{K_C[CO_2][H_2]} \quad (10)$$

$$K_C = \left(\prod_i C_{i_{eq.}}^\gamma \right) \frac{1}{C_o} \quad (11)$$

where $r_{obs.}$ is the observed rate, r_+ and r_- are the rate of forward and reverse reactions, η is the ratio of the rate of the reverse and forward reactions and K_C is the equilibrium constant.

Experiments were also conducted to *i*) determine reaction rates in excess (i.e. non-equimolar) CO₂ or H₂, and *ii*) to determine apparent kinetic parameters. In the first case, CO₂ and H₂ were fed with the catalyst—Fe₃O₄ (100 mg)—held at a temperature of 753 K. The initial partial pressure of both CO₂ and H₂ was 15 kPa. After a period of 16 h, the partial pressure of CO₂ was increased to 60 kPa, while the partial pressure of H₂ was held at 15 kPa. After another period of 2 h, the partial pressure of CO₂ was decreased to 15 kPa and the partial pressure of H₂ was increased to 60 kPa. Finally, both partial pressures were returned to 15 kPa. CO₂ conversion was quantified under the same conditions.

For the second case, apparent kinetic parameters (activation energy and reaction orders) were determined with near equimolar concentrations of CO₂ and H₂ on Fe₃O₄, and under large H₂ excess on Fe₃O₄ as well. With near equimolar concentrations of CO₂ and H₂, the reaction was first performed for 15–16 h at a temperature of 753 K with reactant partial pressures of 15 kPa. The temperature was then lowered in 10 K increments to 723 K, with 5–6 GC injections (a period of about 60 min) taken at each temperature. After the period at 723 K, the CO₂ partial pressure was reduced to 10 kPa and increased in 2.5 kPa increments to a final partial pressure of 20 kPa. Finally, the CO₂ partial pressure was returned to 15 kPa and the H₂ partial pressure was lowered to 10 kPa and increased in 2.5 kPa increments. The basic outline of experiments conducted with excess H₂ was the same as that used for near equimolar reactant concentrations (see also our previous report) [14]. Reactant partial pressures during the initial period were 90 kPa H₂ and 10 kPa CO₂. During the variable CO₂ partial pressure period, the H₂ partial pressure was 85 kPa, and the CO₂ partial pressure was varied between 5 and 12.5 kPa in 2.5 kPa increments. To investigate the effect of H₂ partial pressure, the CO₂ partial pressure was kept at 10 kPa and the H₂ partial pressure was varied between 70–90 kPa in 5 kPa increments.

The measurement of the CO formation rate over Fe₃C has been performed in two different manners. First, the temperature was ramped under a flow of H₂ (15 kPa) and He at the rate of 5 K min⁻¹ up to 753 K. 15 kPa CO₂ was then added into the flow while monitoring the CO formation rate. The second part of the Fe₃C activity test was done by ramping the temperature to 573 K, 623 K, 673 K, 723 K and then cooling back to 673 K again at the rate of 5 K min⁻¹ under the flow of H₂ (15 kPa),

CO₂ (15 kPa), and He (remainder). Each temperature was held for 80 min respectively for GC injection.

Gas-switching experiments were done by measuring CO formation rates while alternating between CO₂ and H₂ gas flows. Catalysts were pretreated as described above, and after pretreatment, CO₂ was added into the reactor to allow the RWGS reaction to proceed for 2 h.

After the reaction, the gas flow rates were changed to 36 sccm helium and 4 sccm H₂. After 20 min, H₂ flow was stopped and was replaced by 4 sccm of CO₂. After 20 min, CO₂ in the gas stream was replaced by H₂. This CO₂→H₂ sequence was repeated three times. The reactor was then purged with helium for 20 min before CO₂ was readmitted into the gas stream. After 20 min, the reactor was again purged with helium before H₂ was readmitted to the gas stream. All sequences with a given gas composition lasted for 20 min, and the temperature of the reactor was 773 K throughout the duration of the gas switching portion of the experiment.

Additional gas-switching experiments involving purge times of varying length with an inert gas were carried out at 753 K. Following the same pretreatment and the reaction in 15 kPa H₂ and 15 kPa for 2 h at 773 K, 15 kPa H₂ was admitted to the reactor. After 15 min, H₂ was replaced by 15 kPa CO₂ for 15 min, and CO₂ was then replaced by H₂ for another 15 min. Then the reactor was purged with helium for 5 min. This sequence (CO₂ → H₂ → He) was repeated several times, but each time the length of the inert purge was increased by 5 min.

An isotopic experiment for the CO formation rate was monitored by MS on Fe₃O₄ (100 mg) while alternating between CO₂ (4 sccm) and C¹⁸O₂ (4 sccm) after the RWGS reaction for 2 h. The temperature was kept constant at 753 K. The total flow rate was 40 sccm with H₂ maintained at 4 sccm. The kinetic isotope effect (KIE) of H₂/D₂ was investigated on Fe₃O₄ (100 mg) for various H₂:CO₂ ratios. After pretreatment, the reaction began at a temperature of 753 K with CO₂ and H₂ partial pressures of 15 kPa. After 16 h, the temperature was lowered to 723 K, and after 1.5 h, H₂ in the feed was replaced by D₂.

4. Conclusions

An unsupported Fe₃O₄-derived catalyst showed very promising activity toward CO formation via CO₂ hydrogenation. The high selectivity (~100% under H₂: CO₂ = 1:1) and great stability make the catalyst feasible to consider in extensive use. The catalyst exhibited only slight deactivation under conditions of excess CO₂, but it can be quickly regenerated under excess H₂. Reaction rates depended more strongly on H₂ (0.8 in reaction order) compared to CO₂ (0.33 in reaction order) under a near equimolar gas-phase composition. The post-reaction analyses of the catalyst indicated that the catalyst was reduced to metallic iron first in the pretreatment of H₂, but the working catalyst remained partially oxidized with the composition of Fe²⁺, Fe³⁺, Fe⁰ and Fe₃C. The main active sites are believed to be the combination of the above species, except that Fe₃C is unlikely to directly contribute to the very steady CO formation at our reaction conditions (1 atm, 723–773 K). Gas-switching experiments revealed that CO was formed only when switching from H₂ to CO₂, and H₂O was formed when switching from CO₂ to H₂, but not when switching from H₂ to CO₂ if purging of helium was in between with the gas admission. The redox mechanism is identified as the dominant reaction pathway for the unsupported iron catalyst.

Supplementary Materials: The following are available online at www.mdpi.com/2073-4344/9/9/773/s1, Figure S1. XRD pattern of Fe₃O₄ after the reduction in H₂, Figure S2. Ion current at m/z = 18 (H₂O), 28 (CO), and 44 (CO₂) during H₂/CO₂ switching experiments on Fe₃O₄. Arrows with a label indicate a change in gas composition to the indicated gas. Reaction conditions: T = 773 K, F_{He} = 36 sccm, F_{H2} or F_{CO2} = 4 sccm. The figure is a modification of Figure 6, Figure S3. Ion current at m/z = 2 (H₂), 3 (HD), 4 (D₂), and 28 (CO) during flow of 7.5 kPa H₂ + 7.5 kPa D₂ + 15 kPa CO₂ and 7.5 kPa H₂ + 15 kPa CO₂ on Fe₃O₄. Reaction conditions: T = 753 K, F_{tot} = 75 sccm, Figure S4. (a) Ion current at m/z = 28 (CO) and m/z = 18 (H₂O) during H₂/CO₂ switching experiments on Fe₃O₄. Arrows with a label indicate a change in gas composition to the indicated gas. The catalysts were in flowing H₂ for 2 h followed by the reaction in CO₂+H₂ for 2 h before the first admission of H₂ (relative time: 31 min) and CO₂ (relative time: 46 min). Reaction conditions: T = 753 K, F_{tot} = 75 sccm, P_{H2} or P_{CO2} = 15 kPa. (b) is the modification of (a), Figure S5. XPS O1s spectra of Fe₃O₄ and post-reaction Fe₃O₄. The curves under the fitted envelope and above the

background are contributions of estimated components from peak fitting. The peak deconvolution and their atomic % are listed on the right of the spectra for each sample, Table S1 Fitted initial slopes and area of H₂O in H₂/CO₂ switching experiment with different He purging time in Figure S4

Author Contributions: conceptualization, C-Y.C. and R.F.L.; methodology, C-Y.C., J.A.L., and R.F.L.; investigation, C-Y.C. and R.F.L.; resources, R.F.L.; data curation, C-Y.C.; writing—original draft preparation, C-Y.C.; writing—review and editing, C-Y.C., J.A.L., and R.F.L.; supervision, R.F.L.; project administration, R.F.L.; funding acquisition, R.F.L.”

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