Article

Flow Pd(II)-Catalysced Carbonylative Cyclisation in the Total Synthesis of Jaspine B

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Abstract: This work describes the total synthesis of jaspine B involving the highly diastereoselective Pd(II)-catalysed carbonylative cyclisation in the preparation of crucial intermediates. New conditions for this transformation were developed and involved the *p*BQ/LiCl as a reoxidation system and $Fe(CO)_5$ as an in situ source of stoichiometric amount of carbon monoxide (1.5 molar equivalent). In addition, we have demonstrated the use of a flow reactor adopting proposed conditions in the large-scale preparation of key lactones.

Keywords: Jaspine B; flow chemistry; palladium catalysis; cyclisation; carbonylation

1. Introduction

The examination of natural resources clearly remains the basis of the discovery of new bioactive substances. Since these newly discovered natural compounds become the inspiration for novel drug candidates, many groups in the scientific community create their research programs aiming at these novel structures. As a result, the newly developed transformations are then presented in terms of their applicability in the synthesis of such targets. However, in many cases such synthetic demonstrations do not provide accessibility to all derivatives and/or usable amounts of promising target molecule for further testing. In particular, progress in later stages of pharmaceutical/biomedical research might then be negatively affected. Although the synthetic optimisation is not so scientifically valued in the chemical community, it is still of great importance. This is especially so today when we are facing environmental and climate changes and need to be concerned about a sustainable future.

Since its discovery, jaspine B (pachastrissamine) **1** has drawn an immense attention from the scientific community (Figure 1).
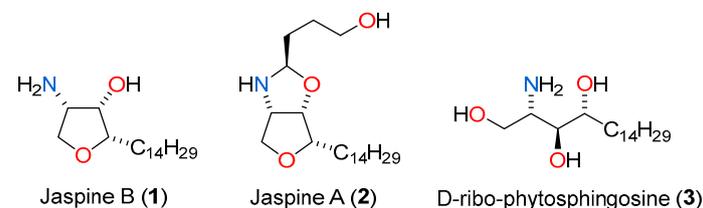

Figure 1. Structure of pachastrissamine (jaspine B) (**1**), jaspine A (**2**) a D-ribophytosphingosine (**3**).

This natural sphingolipid **1** was independently isolated in 2002 and 2003 by T. Higa et al. and by the C. Debitus group from marine sponges, *Pachastrissa* sp. (family Calthropellidae) and *Jaspis* sp., respectively [1,2]. Due to its similar structure to other bioactive sphingolipids, jaspine B **1** has been also tested for its pharmacological properties and it has shown in vitro cytotoxic activity against several types of cancer cell (A-549, P-388, HT-29,

MeL-28, MCF-7, KB, HCT-116, U2OS, MDA-231. HeLa, CNE, MGC-803, EC-9706, PC-3, A-375, WM-115, Caco-2, Jurkat, SNU-638 and Caki-1) in the micro and sub-micromolar range [1–15]. The group of Y. Salma described how the cytotoxic activity of jaspine B **1** is based on the inhibition of SMS (sphinghomyelin synthetase) enzyme activity, which is responsible for maintaining stable concentration levels of ceramides (Cer) in the cell. Thus, higher concentration of Cer induces the cell apoptosis by a caspase-dependent pathway.

To this date, an enormous effort has been made to prepare and study this natural compound 1. There are 35 known syntheses of jaspine B **1**, ten of which are based on an asymmetric step [12,16–24] and twenty-five are chiral pool approaches [4,8,9,25–45]. Moreover, the promising biological activity of this natural compound has resulted in the syntheses of various derivatives of this molecule for structure–activity relationship study purposes (Figure 2).
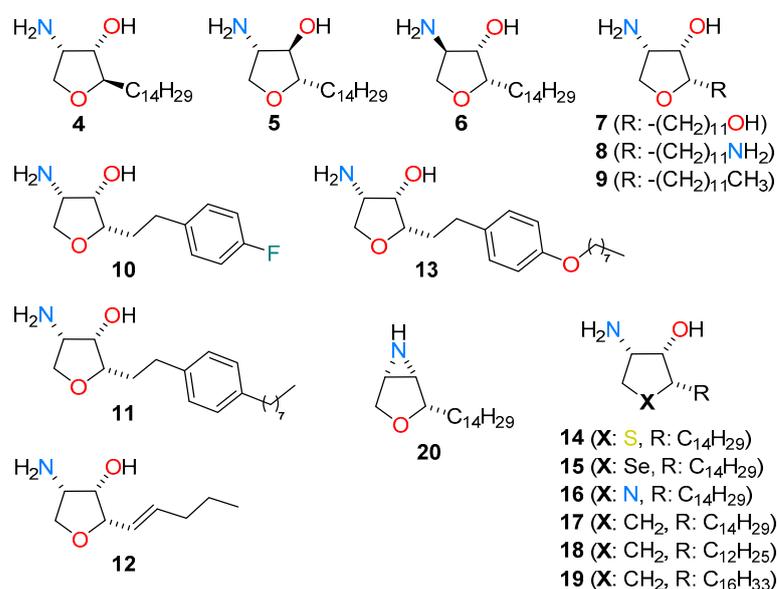

Figure 2. Synthetic derivatives of jaspine B **1**.

In summary, the biological activity of **1** has been found to be highly dependent on the stereo-configuration of the ring substituents and on the length of the aliphatic chain of the natural product [4,9]. The best bioactivity was observed while keeping the original configuration and the length of aliphatic chain [31]. However, the oxygen atom in the heterocycle of jaspine B **1** has not been found to be crucial for its cytotoxic properties [46].

2. Results and Discussion

In the course of our long-term research program directed towards CO gas-free carbonylative cyclisations, flow transformations and their synthetic applications, we have developed a new flow protocol for Pd-catalysed carbonylation reactions based on the use of iron pentacarbonyl [47]. To this date, only a few flow applications of this stereoselective reaction are reported in the literature. However, many total syntheses of natural products utilised this transformation as a batch process [48–50]. As a result, the reaction conditions have undergone many changes and the reoxidation system as one of the most modified parameters has been varied/adjusted from its original conditions to substrate specific requirements (pBQ/CuCl$_2$/O$_2$) [51,52].

Based on the previous results and our experience with the Pd-catalysed carbonylation in the total synthesis of natural products, we have proposed a total synthesis of jaspine B **1** utilising the flow carbonylative step as a key transformation.

2.1. Total Synthesis of Jaspine B

The synthesis of jaspine B **1** was designed to build the chiral centres via the stereoselective Pd-catalysed carbonylation. In addition, the synthesis was optimised to reach one of the key aspects—the compatibility of batch reaction conditions for the following application in the flow system. Thus, this key transformation would provide *N*-protected lactone **21** with correct configuration at chiral centres. The substrate for this cyclisation—unsaturated *N*-protected amino diol can be easily accessible from L-serine (Scheme 1).
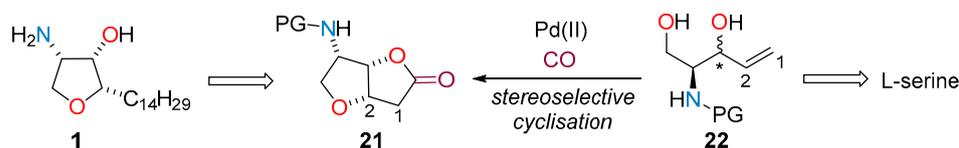
**Scheme 1.** Retrosynthetic analysis of jaspine B **1**.

As depicted in the retrosynthetic analysis, further transformation (chain elongation) of lactone **21** functional group would lead to the natural jaspine B.

Accordingly, the synthesis of **1** started from a commercially available *N*-Boc (*N-t*-butoxycarbonyl) protected Garner's aldehyde **26-Boc**. This aldehyde **26-Boc** can be easily prepared in few synthetic steps starting from L-serine. The whole sequence involving an esterification of L-serine, amino group protection of derivate **23**, the formation of oxazolidine **25** and the following reduction of the ester group is very well described in the literature [53] (Scheme 2).
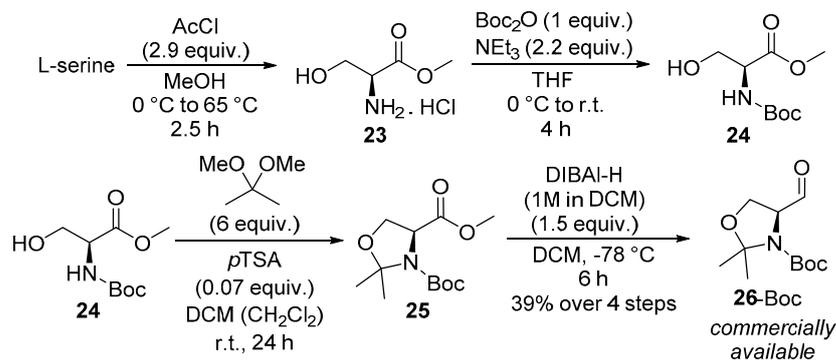

Scheme 2. Preparation of *N*-Boc protected Garner's aldehyde **27-Boc**.

At the beginning, the *N*-Boc protected Garner's aldehyde **26-Boc** was transformed to unsaturated *N*-Boc protected aminodiol **22-Boc** by a two step sequence (Scheme 3a) [54]. In detail, the addition of vinylmagnesium bromide to the starting aldehyde **26-Boc** in THF (tetrahydrofuran) provided a mixture of diastereomeric alcohols **27-Boc** in 91% yield. The selectivity of this reaction varies from 90:10 to 60:40 depending on the reaction temperature [54–56]. The major isomer, 2*S*,3*R*-alcohol **27-Boc** leads to a final product **1** with correct stereo configuration. The following selective deprotection of the acid labile oxazolidine group of **27-Boc** using *p*TSA (*p*-toluenesulfonic acid) provided *N*-Boc protected aminodiols **22-Boc** in 76% yield as an inseparable mixture [57]. Such a mixture of diastereomeric alcohols was then submitted to Pd-catalysed carbonylative cyclisation. This reaction was performed using well-established conditions with Fe(CO)$_5$ as a CO surrogate and the desired products-lactones **21-Boc** were obtained in 75% combined yield. At this stage, the lactone **21-Boc** with all *syn* configuration was separated using MPLC as a major substance from the diastereomeric mixture. Next, the reduction of lactone functional group using DIBAL-H (diisobutylaluminum hydride) provided lactol **28-Boc** in 88% yield (Scheme 3b).
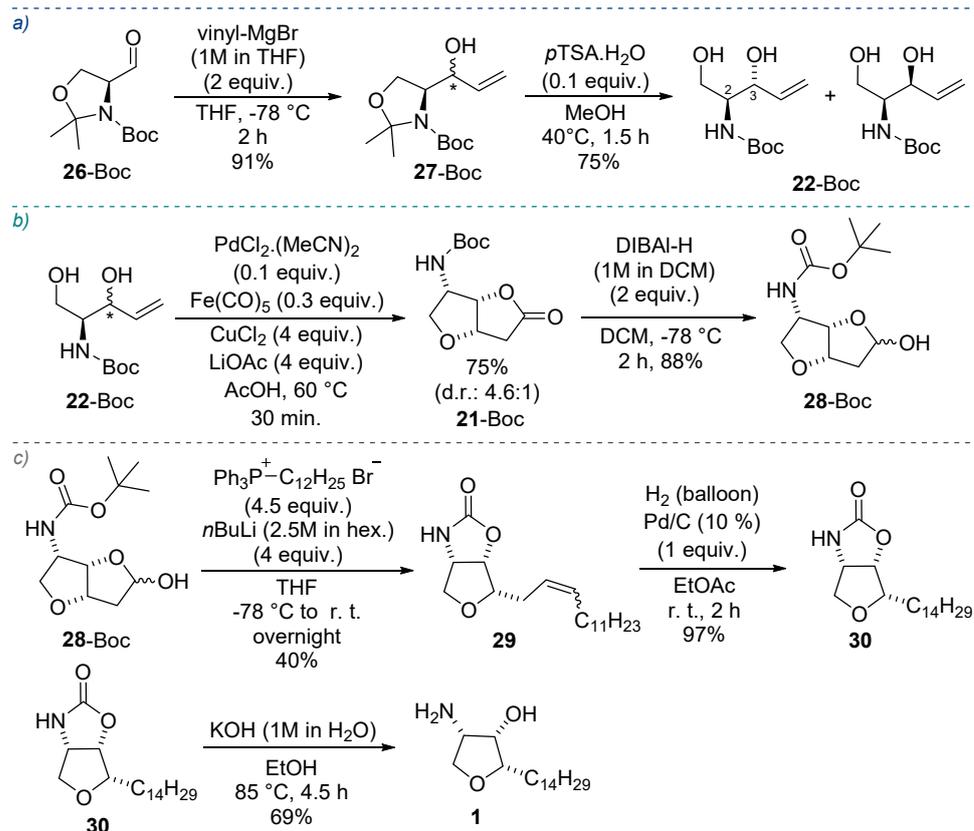
Scheme 3. Total synthesis of jaspine B **1**.

The final step sequence included a Wittig reaction, double bond reduction and oxazolidinone cleavage (Scheme 3c). These synthetic steps have already been described in the literature and the authors used them to furnish the final natural compound **1** by employing *N*-Cbz (*N*-benzyloxycarbonyl) protected lactone **21**-Cbz as a starting material [35]. However, based on the inspection of spectroscopic data, Davies et al. [58] later described the epimerization at C-2 carbon occurred during the Wittig reaction and the authors prepared 2-*epi*-jaspine B [35]. This discrepancy was accounted for by a retro-Michael/Michael epimerisation reaction pathway upon treatment of lactol **28** with excess Wittig reagent (Scheme 4b).
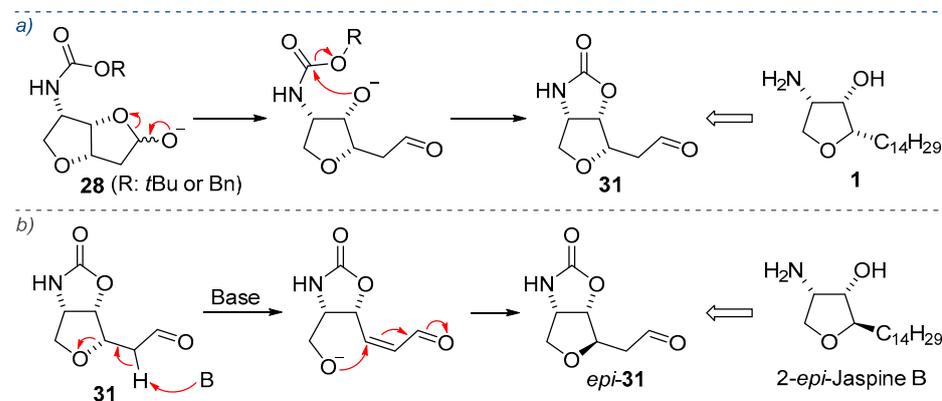

Scheme 4. Formation of oxazolidinone ring (**a**) and possible epimerisation at C-2 carbon in Wittig reaction (**b**).

The authors later described how this epimerisation occurred in the DIBAL-H reduction step using old reagent containing base via same reaction pathway [15].

In our case, by applying the described conditions we were able to prepare the chiral oxazolidinone **29**-Boc in 40% yield. The formation of oxazolidinone ring via intramolecular attack of the hydroxy anion to the carbamate group furnished aldehyde **31** (Scheme 4a). Following a reduction of the double bond using Pd/C and H_2 gave compound **30** in 97% yield. Finally, jaspine B **1** was provided by a cleavage of the oxazolidinone ring of **30** using aqueous KOH in 69% yield. The comparison of spectroscopic data of prepared jaspine B **1** to described data [34] revealed that the epimerisation of **31** during Wittig reaction or reduction has not occurred.

In summary, we have accomplished the total synthesis of jaspine B **1** in seven steps starting from *N*-Boc protected Garner's aldehyde. The stereoselective Pd(II)-catalysed carbonylative cyclisation was used in the preparation of key intermediate-lactone **21**-Boc. The yield of jaspine B was 10% over all synthetic steps.

In addition, the synthesis of jaspine B was also performed starting from the commercially available *N*-Cbz protected Garner's aldehyde **26**-Cbz. Following the same synthetic route, we were able to increase the overall yield of jaspine B up to 16% yield over seven reaction steps (Scheme 5).
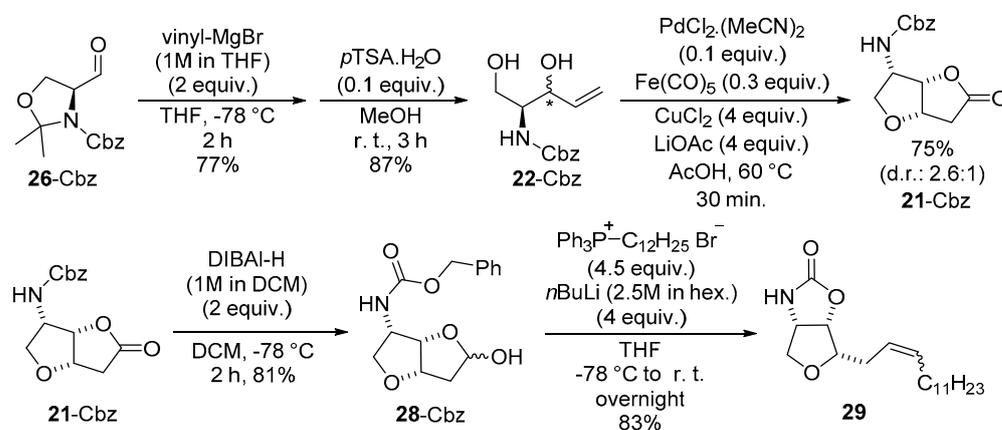
Scheme 5. Synthesis of jaspine B **1** via *N*-Cbz protected lactone.

Similarly, the Wittig reaction of lactol **28**-Cbz proceeded cleanly to oxazolidinone **29** without unwanted epimerisation at the C-2 carbon centre as in the previous case and the desired product **29** was isolated in 83% yield.

After successful optimisation of the total synthesis of jaspine B in batch, we focused our attention on the application of flow chemistry for the preparation of key intermediate-lactone **21**. Thus, the flow Pd(II)-catalysed carbonylative cyclisation of **22** was proposed.

2.2. Flow Synthesis of the Key Intermediate **21** for the Preparation of Jaspine B **1**

Over the last few decades, the flow chemistry has shown many advantages in organic synthesis, and it has grown into a modern and enabling tool for new synthetic methods utilising dangerous and/or toxic chemicals [59,60]. Moreover, many total syntheses of various biorelevant compounds have utilised this technique as a fundamental instrument in the preparation of key intermediates [61–63] or as a multiple step telescoped system [64–66]. At present, the flow chemistry has become an integral part of scientific research and it is commonly used in synthetic laboratories at universities and in pharmaceutical companies.

The flow chemistry technique as a part of our research program has been used in the application of CO surrogates in the carbonylative transformations. We have previously demonstrated that $Fe(CO)_5$ can be utilised as a CO donor in Pd(II)-catalysed carbonylative cyclisation [47]. In the continuation of our research, we have focused on the development of new conditions for this flow transformation and on its application in the flow synthesis of bioactive compounds. Thus, we have proposed a new flow system for the preparation of the key intermediate **21** in the jaspine B **1** synthesis (Figure 3).
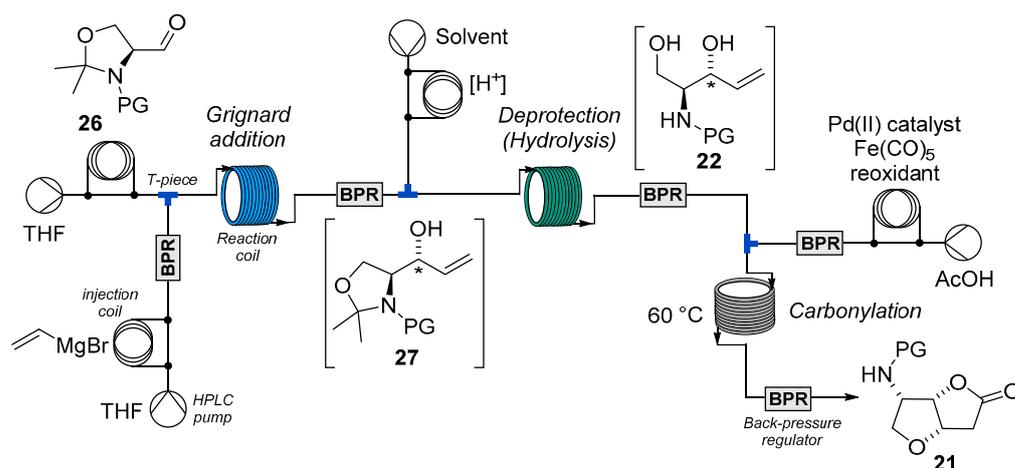
Figure 3. Proposed telescoped flow system for the synthesis of bicyclic lactone **21**.

The proposed telescoped flow system consists of three parts involving the Grignard addition, selective deprotection and crucial cyclisation. The aim of the design was to perform these steps in a one-telescoped system without executing any isolation procedure. Consequently, the flow system would provide the crude final lactone **21** starting from commercially available substrates.

Our investigation started with a series of batch experiments aimed to address the minimal requirements and compatibility of reaction conditions for flow procedure. At first, we examined various reaction conditions of the first two steps sequence of the total synthesis—addition of vinyl magnesium bromide to *N*-protected Garner's aldehyde **26** and selective cleavage of oxazolidine **27** without the isolation after the first step (Scheme 6).
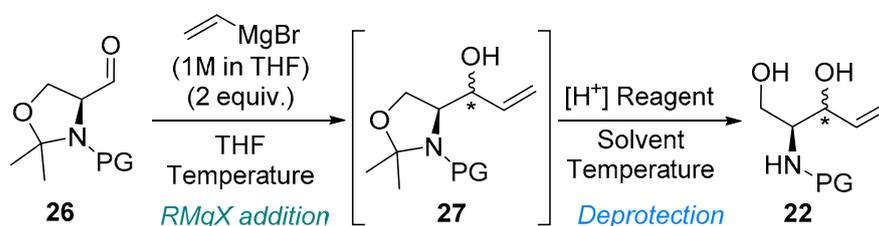
Scheme 6. Optimisation of the RMgX addition and deprotection reaction sequence.

Compared to the previously described batch conditions (Scheme 3a), we tried and modified mainly the cleavage of 2,2-dimethyl oxazolidine **27** using different acidic conditions (Table 1). The best results were achieved using *p*TSA.H$_2$O as a H$^+$ source in MeOH in the second step (Table 1, Entry 1 and 5). Following products **22**-Cbz and **22**-Boc were isolated in 87% and 75% yield over two steps, respectively. In general, altering the temperature of RMgX addition did not affect the yield of this sequence and only the difference in the diastereoselectivity outcome was observed. The addition step at 0 °C of this two-step procedures provided in all cases a 1:1 mixture of diastereomeric alcohols **22**. In addition, the SO$_3$H polymer supported resin, Amberlyst 15 was also tried for the deprotection step as the implementation of polymer supported reagents in flow reactions is described very well [64,67]. In this case, the yield of product **22**-Boc was decreased due to the partial cleavage of an acid labile *N*-Boc protecting group of substrate **26**-Boc. The formation of completely deprotected aminodiol **22** was confirmed by LC-MS analysis and the full cleavage of protecting groups of **26**-Boc was also observed in the case of the reaction performed in AcOH (Table 1, entry 3).

Table 1. Optimisation of the RMgX addition and deprotection reaction sequence in batch.

| Entry | Substrate | RMgX Addition | | Deprotection | | | | Product |
		T (°C)	Rxn Time	[H⁺] Reagent (Equivalent)	Solvent	T (°C)	Rxn Time	Yield (%) [a]
1	**26**-Boc	−78	2 h	pTSA.H$_2$O (0.1)	MeOH	40 °C	1.5 h	75
2	**26**-Boc	0	2 h	Amberlyst 15 (3.2) [b]	MeOH	40 °C	0.5 h	46 [c]
3	**26**-Boc	0	2 h	-	AcOH	70 °C	0.5 h	35 [c]
4	**26**-Cbz	−78	1.5 h	-	AcOH/H$_2$O (4/1)	r.t.	3 h	59
5	**26**-Cbz	−78	1.5 h	pTSA.H$_2$O (0.1)	MeOH	r.t.	3 h	87
6	**26**-Cbz	0	1.5 h	Amberlyst 15 (3.2) [b]	MeOH	40 °C	0.5 h	73

[a] Yield based on the amount of isolated product **22**. [b] The capacity of Amberlyst 15 is 4.7 m equivalents per 1g by dry weight. [c] Partial cleavage of *N*-Boc protecting group was observed by LC-MS analysis.

Based on the optimisation of reaction sequence under batch conditions, we performed a series of experiments using a flow system as depicted in Scheme 7. At first, only nucleophilic addition of RMgX was examined. In this case, the second stage of the flow setup was omitted, and the Grignard reaction was performed at 0 °C to ensure the homogeneity of the reaction stream (the reaction at −78 °C is not homogeneous). Thus, the flow reaction using a 9 mL reactor coil provided products **27** with full conversion of substrates **26** in acceptable yields with lower stereoselectivity (Table 2, entry 1 and 2).
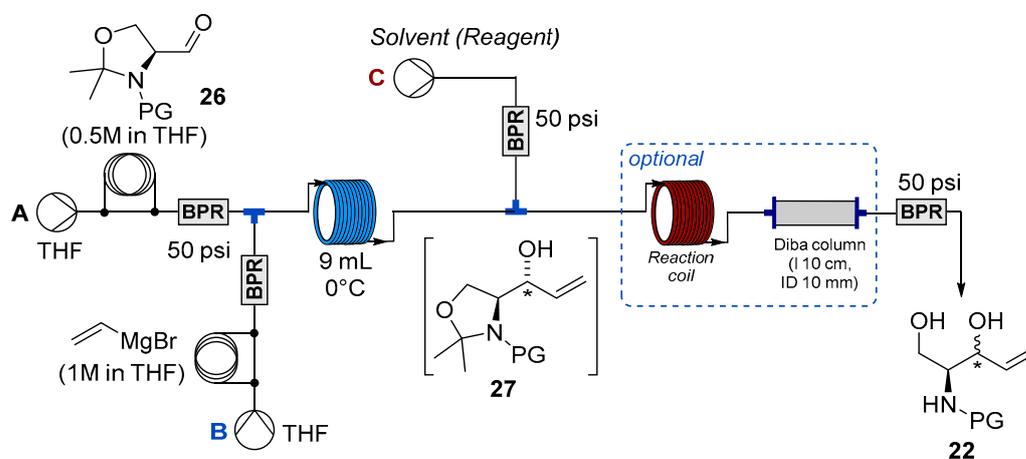
Scheme 7. Optimisation of the flow addition/deprotection reaction sequence.

The following flow experiments employing the second stage of the system were performed using a reaction coil or Diba column (optional) depending on the use of H⁺ donor in the acetonide deprotection step. In the case of the reaction using an excess of Amberlyst 15 (1.7 g, 8 equivalents) in the Diba column, the reagent also secured the filtration of reaction stream and Mg(II) salts formed after mixing (quenching) the Grignard reaction stream with MeOH were caught on the polymer resin. However, the larger excess of Amberlyst 15 also caused a parallel carbamate cleavage and decreased the yield of products. Thus, the flow system using Amberlyst 15 provided products **22**-Boc and **22**-Cbz in 34 and 49% yield, respectively (Table 2, entry 3 and 4).

The best results were achieved using 1.1 M solution of pTSA in MeOH in the second step and the products were isolated in similar yields to batch (Table 2, entry 5 and 6). In this case, the concentration and flow rate of *para*-toluenesulfonic acid stream were adjusted to ensure the catalytic amount of H⁺ necessary for the deprotection of acetonide group.

Since, the 0.25 of 0.275 mmol/min amount of this acid was immediately quenched in the reactor by the excess of Mg(II) salts, the 0.275 mmol/min amount really represents only the catalytic amount of H^+. Thus, the flow reactions using 8.65 mmol of substrates **27**-Cbz or **27**-Boc led to the formation of desired *N*-protected unsaturated aminodiols **22** in 82 and 62% yields, respectively (Table 2, entry 5 and 6). With optimised conditions for this addition/deprotection sequence in hand, we turned our attention to the continuous carbonylative cyclisation step.

Table 2. Optimisation of the flow addition/deprotection reaction sequence.

Entry	Substrate 26-PG	STREAM						Optional Equipment	Yield [b] (%)
		A [a]		B		C			
		Inj. Coil (mL)	Flow Rate (mL/min.)	Inj. Coil (mL)	Flow Rate (mL/min.)	Solvent	Flow Rate (mL/min.)		
1	Boc	2	0.3	2.3	0.3	-	-		84 [c]
2	Cbz	2	0.25	2.3	0.25	-	-		66 [c]
3	Boc	2	0.3	2.3	0.3	MeOH	0.6	1.7g (Amberlyst)	34 [d]
4	Cbz	2	0.25	2.3	0.25	MeOH	0.5	1.7g (Amberlyst)	49
5	Boc	17.3	0.25	18.4	0.25	*p*TSA in MeOH (1.1M)	0.25	reaction coil (10 mL, 50 °C)	62
6	Cbz	17.3	0.25	18.4	0.25	*p*TSA in MeOH (1.1M)	0.25	reaction coil (10 mL, 50 °C)	82

[a] 0.5 M solution of substrate in THF (tetrahydrofuran) was used. [b] Yield based on the amount of isolated product **22**. [c] Only addition step was performed in the flow system, the yield corresponds to the addition product **27**. [d] Deprotection of *N*-Boc group was also observed.

In 2018, we reported on pros and cons of the flow and batch stereoselective Pd-catalysed carbonylative cyclisation of unsaturated polyols/aminoalcohols using known conditions [68] and $Fe(CO)_5$ as an in situ donor of carbon monoxide [47]. By adjusting the concentration of reaction streams and the amount of Cu^{2+}/Li^+ inorganic salts required for the reoxidation Pd^0, we were able to prepare a series of various cyclisation products in a flow system (Scheme 8).
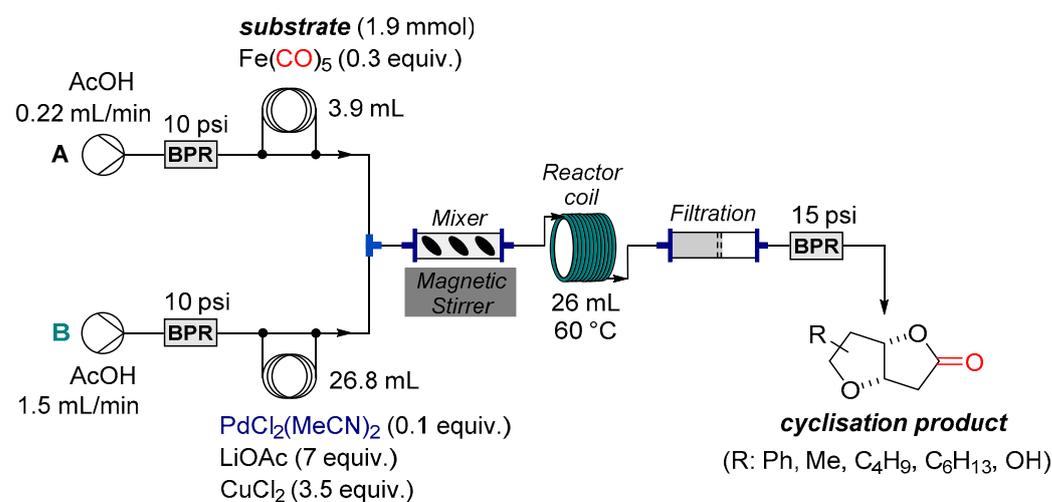
Scheme 8. Previously described continuous Pd(II)-catalysed carbonylation of unsaturated polyols and aminoalcohols.

Even though aforementioned continuous flow system was successfully applied in the large-scale preparation of desired bicyclic lactones, there are still limitations of the

system regarding the formation of insoluble copper salts in the reactor. Also, an active mixer and interchangeable filtration unit were necessary to perform the transformation over longer periods.

With the aim to improve the conditions for continuous flow Pd-catalysed oxy/aminocarbonylation, we adopted the use of *p*BQ (*p*-benzoquinone) instead of Cu²⁺ as a reoxidant.

At first, we performed a batch reaction using 2 equivalents of *p*BQ, 0.6 equivalent of Fe(CO)₅ and 0.1 equivalent PdCl₂(MeCN)₂ using diastereomeric mixture **22**-Boc (0.23 mmol) in acetic acid (0.9 mL, 0.25 M reaction). The reaction at 60 °C proceeded with full conversion of starting material after 1 h, however noticeable amounts of insoluble material were observed. The homogeneity of the reaction mixture over the whole course of reaction was achieved by the addition of 1 equivalent of LiCl. The reaction proceeded smoothly with full conversion of **22**-Boc in 1 h at 60 °C. A comparison of newly optimised and previously described conditions is shown in Figure 4.
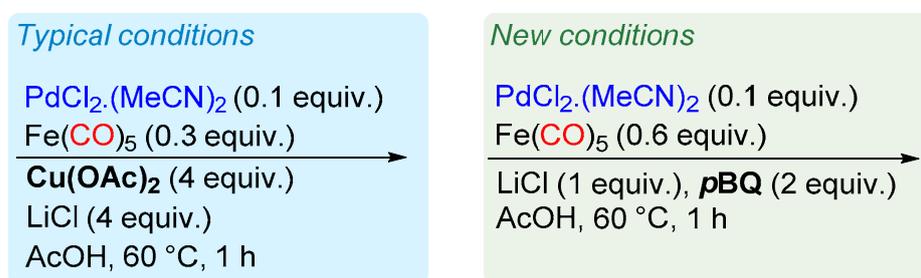

Figure 4. Comparison of known and new conditions for Pd-catalysed carbonylative cyclisation.

The new reaction conditions were then tested in the preparation of key intermediate-lactone **21** for the synthesis of jaspine B **1** in continuous flow mode (Scheme 9). The flow setup consisted of two reaction streams which were pumped using HPLC Azura pumps via injection coils to a preheated reactor coil. The composition of stock solutions were adjusted to avoid the decomposition of Fe(CO)₅ in the presence of oxidation reagents (*p*BQ). The following continuous reaction of **22** on 0.5 mmol scale provided the desired *N*-protected bicyclic lactones **21** in comparable yields to standard batch and flow conditions (Table 3).
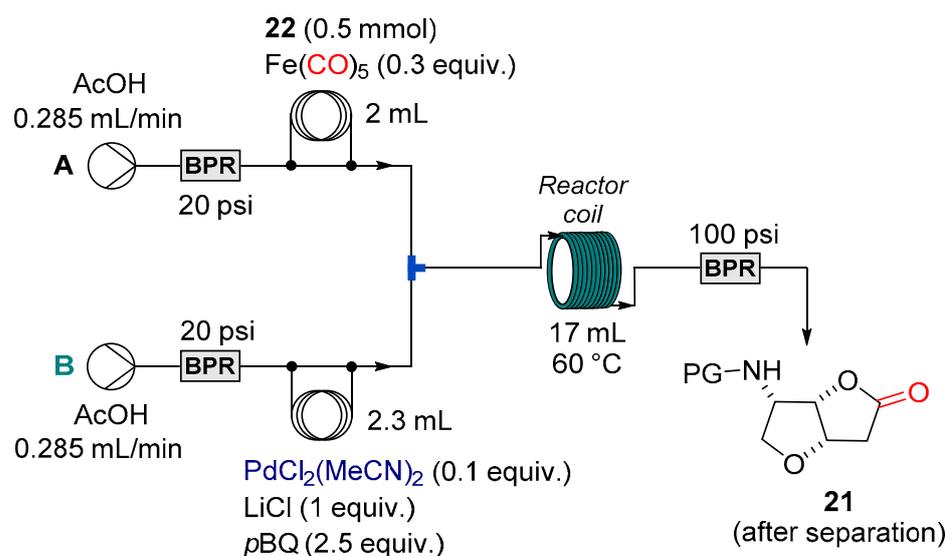
Scheme 9. Continuous Pd(II)-catalysed carbonylations of unsaturated *N*-protected aminodiols **22**.

**Table 3.** Comparison of Pd(II)-catalysed carbonylation of **22** employing batch and flow conditions.

Entry	Product	Typical Conditions		New Conditions
		Batch Yield [a,b] (%)	Flow Yield [a,c] (%)	Flow Yield [a,d] (%)
1	**21**-Cbz	75	76	71
2	**21**-Boc	75	64	72

[a] Combined yield of both diastereomers based on the isolated amounts of products **21**. [b] Batch reaction of **22** (0.5 mmol) using $PdCl_2$. $2CH_3CN$ (0.048 mmol, 0.1 equivalent), $CuCl_2$ (1.9 mmol, 4 equivalents), LiOAc (1.9 mmol, 4 equivalents) and $Fe(CO)_5$ (0.15 mmol, 0.3 equivalent) in 1.9 mL of AcOH [68]. [c] Reaction was performed on 1.22 mmol scale (substrate **22**) using the conditions and flow system as described in the literature [47]. [d] Reaction was performed using flow system as depicted in Scheme 9.

In detail, flow transformation using new conditions as depicted in Scheme 9 provided both lactones **21** in comparable yields to reactions performed under typical conditions (Table 3, flow yield column). The new reoxidation system for Pd^0-Pd^{II} cycle ensures homogeneity of the reaction stream thus enabling better scaling of this flow transformation. Compared to the batch reaction (Table 3, typical conditions, batch yield column), the designed flow transformation (under new conditions) has several advantages. The batch reaction using typical conditions [47] can be undertaken only on a small scale due to the excessive pressure in the glass reaction tube. Upscaling the batch reaction 20 mmol may cause a few problems. As $Fe(CO)_5$ immediately decomposes after contact with the reaction mixture, it releases 1 equivalent of CO resulting in foaming and problematic stirring of heterogenous reaction mixture. Also, the pressure in a 120 mL reaction tube can raise up to 95 psi after few minutes.

To prove the robustness of the described flow setup, a six-hour long experiment was performed. Based on our previous experience with this type of transformation, we lowered the reaction stream concentration (0.25 M down to 0.125 M) to avoid the gas-liquid segment formation in the reaction coil. Continuous flow transformation of diastereomeric mixture **22**-Boc (5.57 g) using such minimally modified conditions provided the desired lactones **21**-Boc in 71% (4.5 g) combined yield (using the same flow setup as depicted in Scheme 10). However, a formation of precipitate at the exit of the reactor after cooling the reaction stream was observed. To prevent the potential clogging of the tubing, THF was employed as co-solvent in the case of a large-scale continuous reaction using **22**-Cbz (Scheme 10). In this case, the prepared stock solutions of substrate **22**-Cbz and reagents were pumped directly through the HPLC pumps into the larger reactor (47 mL) therefore allowing us to use higher flow rates (0.785 mL/min) and transform a larger amount of starting material **22**-Cbz in shorter time. In detail, the diastereomeric mixture *N*-Cbz protected aminodiols **22**-Cbz (7.6 g) was easily transformed over 2.5 h into bicyclic lactones **21**-Cbz (d.r.: 2.6:1, 6.3 g) in 75% combined yield. The pure diastereomer **21**-Cbz with all *syn*-configuration was obtained after MPLC purification in 54% yield (4.5 g).

In conclusion, we have designed and optimised an enhanced synthesis of the key intermediate-lactones **21**-Cbz and **21**-Boc utilising the stereoselective Pd-catalysed cyclo-carbonylation of corresponding unsaturated aminodiols **22**. The key lactones **21** were then successfully transformed into natural jaspine B **1** over a four-step sequence in batch. Also, we have demonstrated the applicability of the flow reactor in two steps preparation of *N*-protected aminodiols **22** in comparable yields to the batch process. Importantly, new conditions for Pd-catalysed cyclocarbonylation of unsaturated polyols/aminoacohols were developed involving *p*BQ/LiCl as a reoxidation system and $Fe(CO)_5$ as an in situ source of stochiometric amount of carbon monoxide (only 1.5 molar equivalents). Such conditions were easily applied to continuous flow mode allowing us to prepare gram quantities of intermediates **21** for jaspine B **1** synthesis. This flow setup has shown several advantages compared to previous versions of the flow reaction system and the homogeneity of the reaction stream facilitated the use of a common flow system without the implementation of any other special devices.
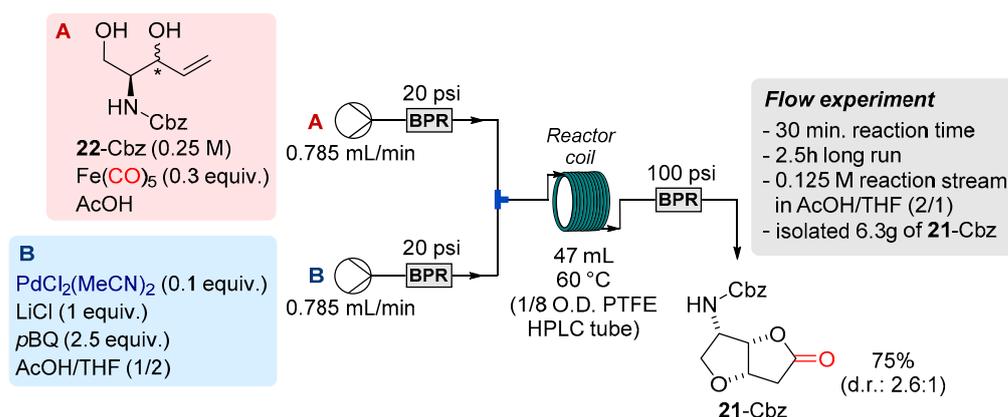
Scheme 10. Large-scale continuous synthesis of *N*-Cbz protected lactone **21**-Cbz.

3. Experimental Section

3.1. Material and Methods

Commercial materials which were obtained from Sigma-Aldrich, Acros Organics, Alfa Aesar or Fisher Scientific were used without further purification. Reactions were monitored using TLC on silica gel. Compound purification was undertaken by flash chromatography. All solvents were distilled before use. Hexanes refer to the fraction boiling at 60–65 °C. Flash column liquid chromatography (FLC) was performed on silica gel Kieselgel 60 (15–40 μm, 230–400 mesh) and analytical thin-layer chromatography (TLC) was performed on aluminium plates pre-coated with either 0.2 mm (DC-Alufolien, Merck) or 0.25 mm silica gel 60 F254 (ALUGRAM® SIL G/UV254, Macherey–Nagel). Analysed compounds were visualized by UV fluorescence and by dipping the plates in an aqueous H_2SO_4 solution of cerium sulphate/ammonium molybdate followed by charring with a heat gun. Melting points were obtained using a Boecius apparatus and are uncorrected. ^1H and ^{13}C NMR spectra were recorded on either 300 (75) MHz MercuryPlus or 600 (151) MHz Unity Inova spectrometers from Varian (Supplementary Materials). Chemical shifts (δ) are quoted in ppm and are referenced to the tetramethylsilane (TMS), $CDCl_3$ or DMSO-d_6 as internal standard. FTIR spectra were obtained on a Nicolet 5700 spectrometer (Thermo Electron) equipped with a Smart Orbit (diamond crystal ATR) accessory, using the reflectance technique (400–4000 cm^{-1}). High-resolution mass spectra (HRMS) were recorded on an OrbitrapVelos mass spectrometer (Thermo Scientific, Waltham, MA, USA; Bremen, Germany) with a heated electrospray ionization (HESI) source. The mass spectrometer was operated with a full scan (50–2000 amu) in positive or negative FT mode (at a resolution of 100,000). The sample was dissolved in methanol and infused via syringe pump at a rate of 5 mL/min. The heated capillary was maintained at 275 °C with a source heater temperature of 50 °C and the sheath, auxiliary and sweep gases were at 10, 5 and 0 units, respectively. Source voltage was set to 3.5 kV.

3.2. Representative Flow Procedures

3.2.1. Grignard Reaction

The flow setup consisted of three HPLC pumps (Knauer Azura 4.1S with 10 mL pump head). The pumps were used to introduce a solution of substrate **26** (1 mmol, 0.5 M) in anhydrous THF (Feed A), a commercial solution of vinylmagnesium bromide (1.0 M in THF, Sigma-Aldrich, Feed B), and MeOH (Feed C). Injection loops (PTFE, 0.8 mm i.d., 1.6 mm o.d.; internal volume: 2.0 mL, Feed A, and 2.3 mL, Feed B) were used to deliver the two starting feeds. At start of the experiment, the whole reactor was flushed with an anhydrous THF (Feed A and Feed B) and MeOH (Feed C). Both solutions were loaded into their corresponding injection loops. Feed A and feed B were pumped from the injection loops and mixed in a T-shaped connector (PEEK) in a cooling bath (0 °C). The combined mixture passed through a coil reactor (PTFE, 0.8 mm i.d., 1.6 mm o.d.; internal volume: 9.0 mL) at 0 °C before the mixture was combined with MeOH (Feed C) in a T-shaped

connector (PEEK) at the same temperature. Final reaction mixture left the system through Upchurch BPR (15 psi). The mixture was then collected in the flask, and evaporated in vacuo. The residue was purified by MPLC (mixture of hexanes and EtOAc) providing the desired alcohols **27**.

3.2.2. Preparation of Unsaturated Aminodiols

The flow setup consisted of three HPLC pumps (Knauer Azura 4.1S with 10 mL pump head). The pumps were used to introduce a solution of substrate **26** (0.5 M) into anhydrous THF (Feed A), a commercial solution of vinylmagnesium bromide (1.0 M in THF, Sigma-Aldrich, Feed B), and quenching solvent/mixture (MeOH, AcOH, mixture AcOH/H_2O or 1.1 M solution of pTSA in MeOH), Feed C). Injection loops (PTFE, 0.8 mm i.d., 1.6 mm o.d.; internal volume: 2.0 mL, Feed A, and 2.3 mL, Feed A) were used to deliver the starting two feeds. At the beginning of the experiment, the complete reactor setup was flushed with anhydrous THF (Feed A and Feed B) and corresponding solvent/mixture (according to the conditions in Table 2, Feed C). Both solutions were loaded into their corresponding injection loops. Feed A and feed B were pumped from the injection loops and mixed in a T-shaped connector (PEEK) in a cooling bath (0 °C). The combined mixture passed through a coil reactor (PTFE, 0.8 mm i.d., 1.6 mm o.d.; internal volume: 9.0 mL) at 0 °C before the mixture was combined with Feed C (corresponding solvent or mixture) in a T-shaped connector (PEEK) at the same temperature. The mixture was then pumped through a second coil reactor at 50 or 70 °C (PTFE, 1.5 mm i.d., 3.2 mm o.d.; internal volume: 4.0 or 10.0 mL) or glass Omnifit column at 40 °C (10 mm i.d. × 100 mm length) filled with corresponding amount of Amberlyst 15. At the end, the reaction mixture left the system through Upchurch BPR and it was collected in the flask. The solvent from collected crude material was concentrated in vacuo (if the pTSA was used, collected stream was at first quenched with saturated water solution of $NaHCO_3$ and extracted with EtOAc). The residue was purified by MPLC (mixture of hexanes and EtOAc) providing the desired alcohol **22**.

3.2.3. Carbonylative Cyclisation Using pBQ/LiCl Reoxidation System

The flow setup consisted of two HPLC pumps (Knauer Azura 4.1S with 10 mL pump head). These pumps were used to introduce a solution of substrate **22** (0.25 M) and iron pentacarbonyl (0.3 equivalent) in glacial AcOH (Feed A), and solution of pBQ (2.5 equivalents), LiCl (1 equivalent) and $PdCl_2(MeCN)_2$ (0.1 equivalent) in the solvent (glacial AcOH or THF/AcOH = 2:1, Feed B). Injection loops (PTFE, 0.8 mm i.d., 1.6 mm o.d.; internal volume: 2.0 mL, Feed A, and 2.3 mL, Feed B) were used to deliver the two feeds. At the beginning of the experiment, the complete reactor setup was flushed with glacial AcOH (Feed A) and corresponding solvent/mixture (Feed B). Both solutions were loaded into their corresponding injection loops. (Stock solutions were pumped directly via HPLC pumps in the case of long runs). Feed A and feed B were pumped from the injection loops and mixed in a T-shaped connector (PEEK). The combined mixture went through a reactor coil (PTFE, 0.8 mm i.d., 1.6 mm o.d.; internal volume: 17.1 or 47.1 mL) at 60 °C before the flow stream left the system through Upchurch BPR (100 psi). The whole reaction stream was collected in the flask, and evaporated in vacuo. The residue was purified by MPLC (mixture of hexanes and EtOAc) providing the appropriate bicyclic lactones **21**.

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