

Article

Sorption of 71 Pharmaceuticals to Powder Activated Carbon for Improved Wastewater Treatment

Maritha Hörsing ^{1,2}, Henrik Rasmus Andersen ², Roman Grabic ³, Jes la Cour Jansen ^{1,*} and Anna Ledin ¹

¹ Water and Environmental Engineering at Department of Chemical Engineering, Lund University, P.O. Box 124, SE-221 00 Lund, Sweden; maritha.horsing@mjolby.se (M.H.); anna.ledin@miljo.goteborg.se (A.L.)

² Department of Environmental Engineering, Technical University of Denmark, B113, DK-2800 Kgs Lyngby, Denmark; hran@env.dtu.dk

³ Department of Chemistry, Umeå University, SE-901 87 Umeå, Sweden; rgrabic@frov.jcu.cz

* Correspondence: jes.la_cour_jansen@chemeng.lth.se; Tel.: +45-45-812806

Abstract: In this study, sorption distribution coefficients were determined for 71 pharmaceuticals, aiming to describe their sorption behavior to powder activated carbon (PAC). The data are expected to be applied when designing and upgrading wastewater treatment plants (WWTP) for improved removal of pharmaceuticals by applying sorption to PAC as an additional removal technique. Sorption isotherms were determined for the pharmaceuticals over a concentration interval covering a wide range from 0.08 to 10 µg/L using PAC at a concentration of 10 mg/L. The best fitted sorption isotherms were used to calculate the distribution coefficients (K_d) and these were applied to estimate that the PAC doses needed to achieve a target concentration of 10 ng/L in the effluent. A target concentration was used since neither discharge limit values nor environmental quality standards in general have been defined for these compounds. Using a %-removal approach does not guarantee achievement of concentrations low enough to protect the water ecosystems. Some of the pharmaceuticals will be reduced by the addition of small amounts of PAC. Examples are atenolol, carbamazepine, citalopram, codeine, fluoxetine and ibuprofen. For others, e.g., oxazepam, an alternative treatment has to be considered since the requested dose is too high to be realistic for a target concentration of 10 ng/L.



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1. Introduction

The existing conventional wastewater treatment plants (WWTPs) are not designed for removal of anthropogenic organic micropollutants. Industrial chemicals and pharmaceuticals with endocrine disrupting effects and/or other unwanted, and even unknown, biological effects have been detected in bodies of water around the world (see, e.g., [1–5]). WWTPs with different types and combinations of treatment processes reduce pharmaceuticals to different extents. Some examples can be found in the literature, e.g., diclofenac, metoprolol and glibenclamide, where the removal efficiencies varied between 45–85, 75–100 and 40–90%, respectively [6]. Sorption to sludge during wastewater treatment has been shown to be important for some pharmaceuticals, such as clotrimazole and haloperidol, whereas the main part of the 75 pharmaceuticals investigated in that study remained in the water phase [7]. Hence, there is a need to upgrade WWTPs in order to minimize the release of organic micropollutants into the aquatic environment.

Numerous technologies based on biological, chemical and physical treatments have been developed and tested for the extended removal of organic micropollutants during recent years. Advanced biological treatments, i.e., moving bed biofilm reactors, have shown to be more efficient in removing the target compounds compared to active sludge systems [8]. However, not all compounds can be removed with the use of advanced

biological treatment. Chemical treatment has also been investigated for the removal of unwanted compounds. In [9], it is shown that ozone selectively could oxidize and remove estrogens. Another oxidant, chlorine dioxide, has been demonstrated to be a promising oxidant for removal of pharmaceuticals [10,11]. However, by applying chemical treatments, there is a risk that unwanted transformation products are formed, as well as by-products from the oxidation process. Both granular activated carbon (GAC) and powder activated carbon (PAC) have been investigated as sorbents for organic micropollutants. In [12] it was found that GAC was better suited as sorbent for nonylphenol compared to naproxen in a drinking water treatment plant in a pilot scale. Further, the authors showed that the need of PAC was less in order to achieve 90% removal of naproxen, while more PAC was needed to achieve 90% removal of nonylphenol compared to the use of GAC. PAC was shown to be an efficient method for removal of some endocrine disrupting compounds (EDCs) in a bench-scale study including 23 pharmaceuticals [13]. Here, it was found that >90% of the EDCs were removed by applying PAC at a dose of 5 mg/L. For ibuprofen, sulfamethoxazole and meprobamate the removal was lower, between 40% and 60%. In a review [14], it was summarized that PAC was shown to be the most efficient sorbent, especially for refractory nonbiodegradable compounds. However, the present knowledge regarding the removal efficiency for many pharmaceuticals is still scarce. Furthermore, sorption isotherms for different organic micropollutants than PAC are rare, although some can be found, e.g., perfluorooctane sulfonate (PFOS) and perfluorooctanoate (PFOA) [15], and some estrogens [16].

Other researchers have studied some of the pharmaceuticals investigated in the present study. In [17], a 69% reduction for both diclofenac and oxazepam by 12 g/m³ PAC is reported. Diclofenac in concentrations from 2600 to 5800 ng/L was reduced by 80% by applying 10 g/m³ PAC [18]. PAH, pharmaceuticals and pesticides were included in [13]. It was shown that PAH were reduced to a greater extent than the pharmaceuticals studied. Evaluation of the removal of endocrine disrupting compounds by use of PAC (3 g/m³) revealed a removal efficiency of 2–35% for bisphenol A during 15 min of contact time [19]. Further, the author found that at a PAC dose of 30 g/m³, nonylphenol and octylphenol were removed by 100% and 60%, respectively.

The objectives of this study were to experimentally determine the sorption isotherms and sorption coefficients for 120 pharmaceuticals to PAC. Further, based on the obtained coefficients and based on observed concentrations in Swedish wastewater effluents [4], this study estimates the quantity of PAC needed in order to reduce the pharmaceuticals from WWTPs' effluents substantially. The observed concentrations in Swedish WWTPs were supplemented with corresponding, worldwide observations in cases where the Swedish values deviated substantially from data found in the published literature. The obtained results are expected to be useful information when determining for which pharmaceuticals the application of PAC could be a realistic option and when WWTPs are going to be upgraded to remove organic micropollutants.

2. Materials and Methods

The methodology and design applied for determining the sorption isotherms for a large number of pharmaceuticals have been published earlier in a study by the authors [7]. The aim in that study was to determine sorption isotherms for pharmaceuticals to primary and secondary sludge. Shortly, a stock solution including all the pharmaceuticals with the concentration of 100×10^{-3} g/L was prepared in methanol. From this, four methanol stock solutions with the concentrations of 0.4×10^{-3} , 2.0×10^{-3} , 10.0×10^{-3} and 50.0×10^{-3} g/L, respectively, were prepared. Earlier studies have shown that there is no significant difference when the distribution coefficients are determined for single compounds or mixtures (see [7] and references therein). Furthermore, in the present study it was important to mimic a wastewater where the compounds are all present together. As in the previous study [7], 1 L artificial wastewater was used. It consisted of a phosphate-buffered mineral medium containing Ca^{2+} , K^+ , Mg^{2+} , Na^+ , Cl^- and SO_4^{2-} , to which PAC

0.01 g was added in 1 L Schott Duran® bottles. In order to inhibit microbial growth, the bottles were flushed with N₂(g) for 1 min, and Na₂SO₃ was added to a final concentration of 50 mg/L. The bottles were left at +4 °C in the dark and stirred for 12 h before the addition of the pharmaceutical mixture. By adding 200 µL of the different stock solutions, using a Hamilton syringe, the final concentrations given in Table 1 were reached. The sorption and equilibrium processes were set to 12 h, during which the bottles were stirred in the dark at +4 °C. Included were blanks without pharmaceuticals but with PAC, and controls without PAC but with the selected concentrations of pharmaceuticals (Table 1). PAC used in this study was purchased from Merck, Darmstadt, Germany. The Langmuir surface area was determined and measured to 1036 m²/g and pore volume to 0.61 cc/g with p/po 0.99.

Table 1. Experimental setup, including pharmaceutical concentrations and PAC concentrations.

Types of Test Bottles	PAC Conc. (g/L)	Pharmaceutical Conc. (µg/L)
Blank	0.01	0
Control	0	0.08, 0.4, 2, 10
PAC 10	0.01	0.08, 0.4, 2, 10

The experimental setup enables the evaluation of sorption of the chosen pharmaceuticals present in a mixture of many substances, in typical concentration levels found in a full-scale wastewater treatment plant. Further, the contact time between PAC and pharmaceutical are similar to what can be expected if PAC is dosed to an activated sludge tank. As such, the results have the potential to show the sorption behavior at a level where reasonable prediction of the needed PAC dose to reach a chosen target concentration can be given. However, since the impact on the sorption by other substances that most likely will be present in the wastewater are excluded and the potential effect on sludge characteristics is not evaluated from the batch experiments, further research is needed in order to give detailed advice for the practical needed PAC doses.

2.1. Extraction and Chromatography

Triplicate extractions were made from each 1 L Schott Duran® bottle as earlier described in [7], using Oasis HLB 200 mg, 30 µm (Waters, Solna, Sweden). The analyses were made according to [20], employing LC-MS/MS.

2.2. Data Analyses

For the data, analyses of the solubility, limit of quantification (LOQ) and the linear range of the analytical method [20] were considered for each pharmaceutical included. The idea was to obtain four API equilibria with water concentration (C_w) in the range of 90% of the starting concentration (C_0) and the LOQ. The water solubility should be larger than the starting concentration. The measured concentrations of the pharmaceutical in the water phase (C_0) in the bottles to which no PAC was added and in those where PAC was added (C_w) were used to calculate the sorbed concentration (C_s), $C_s = C_0 - C_w$. By plotting results from the batch sorption experiments including multiple concentrations, sorption isotherms may be obtained, from which the solid–water distribution coefficients can be determined. Sorption isotherms define the equilibrium between the concentration of a chemical in aqueous and solid phases [21]. In the present study, three equations were included: linear Equation (1), Freundlich Equation (2) and Langmuir Equation (3).

$$C_s = K_d \times C_w \quad (1)$$

$$C_s = K_f \times C_w^{\frac{1}{n}} \quad (2)$$

$$C_s = \frac{\tau_{\max} \times K_L \times C_w}{1 + K_L \times C_w} \quad (3)$$

where: C_w is the concentration in the water phase (g/L), C_s is the concentration sorbed to the PAC (g/kg) and K_d is the linear sorption coefficient. K_f is the Freundlich coefficient and n is the Freundlich exponent. τ represents the total number of surface sites per mass of sorbent, and K_L is the Langmuir coefficient. The linear isotherm is the simplest case where the affinity of the pharmaceutical remains constant over the concentration interval.

With the intention of finding the best fitted isotherm, the software GraphPad Prism 5 for Windows (GraphPad Software, Inc., San Diego, CA, USA) was used. A 95% confidence interval was applied for evaluation of the data. In order to qualify as the best fit, the R^2 -value for the curve should be >0.7 ; otherwise, no fit was determined. In order to determine which of the isotherms that had the best fit, two hypotheses were tested: linear against Freundlich and linear against Langmuir. The significance (P) that the linear model has a better fit than the other models was used for that. If both Freundlich and Langmuir isotherms turned out to be better than the linear, the one with the highest R^2 -value was determined to have the best-fitted isotherm.

2.3. Estimation of the Removal of Pharmaceuticals by Use of PAC

The amount of PAC needed in order to remove pharmaceuticals from the treated wastewater was estimated by employing the obtained sorption isotherms as well as known concentrations for pharmaceuticals quantified in Swedish WWTP effluents [4]. The amount of PAC needed in order to reduce the quantity of a pharmaceutical in the water phase was calculated using Equation (4), where F_S was the sorbed fraction of the pharmaceutical at equilibrium for a given amount of PAC.

$$F_S = \frac{\text{PAC} \times K_d}{1 + \text{PAC} \times K_d} \quad (4)$$

The observed concentrations in Swedish WWTPs were supplemented with corresponding, worldwide observations in cases where the Swedish values deviated substantially from data found in the published literature.

3. Results and Discussion

3.1. Sorption Isotherms

For experimentally obtained isotherms, the Freundlich isotherm often provides a better fit compared to the linear fit. The Langmuir isotherm may have the best fit in cases where the sorbent becomes saturated at higher concentrations of pharmaceuticals. The same shape may also be seen where one important sorbent is present, e.g., activated carbon or clay mineral [21].

Sorption isotherms were determined for 71 pharmaceuticals out of the 120 present in the experiments. For 49 of the tested pharmaceuticals, no isotherms were obtained. This was either due to very high sorption and/or to limitations in the ability to quantify the compounds in low concentrations. For amiodarone, bromocriptine, chlorpromazine, dihydroergotamin, fluphenazine, miconazole, perphenazine and roxithromycin, sorption was so strong that the differences in the water concentrations when analyzing the lower applied concentrations, both in water and in water with addition of PAC, were insignificant. Thus, except strong sorption, no conclusion can be made for those pharmaceuticals.

Table 2 presents the obtained sorption coefficients for each of the 71 pharmaceuticals.

The Freundlich isotherm was found to provide the best fit for 51% of the pharmaceuticals, while Langmuir was the best fit in 38% of the cases, and for 8% of the pharmaceuticals the linear isotherm gave the best fit. This made it impossible to gain representative, analytical results for estimation of sorption isotherms. These compounds are consequently not included among the 71 pharmaceuticals presented in Table 2.

Table 2. Sorption isotherms obtained during sorption to PAC. Included here is the linear sorption coefficient K_d , Freundlich coefficient and exponent K_f and n , respectively, and for the Langmuir isotherm, the Langmuir coefficients K_L and τ represent the total number of surface sites per mass of sorbent.

Linear * Isotherm			Freundlich Isotherm			Langmuir Isotherm				
Substance	K_d (L/g)	R ² (%)	K_f (L/g)	n	R ² (%)	p Value (%)	τ_{MAX} (L/g)	K_L	R ² (%)	p Value (%)
Alfuzosin	5440 **	96.8	6.82×10^3	1.04	96.8	60.9	9.47×10^6	6.46×10^{-4}	96.9	51.2
Alprazolam	406	79.0	8.27×10^4	3.53	94.4	6.31	6.91×10^5	2.74×10^{-2}	94.4	6.35
Amitryptiline	482	85.3	4.54×10^4	2.45	96.2	<0.01	1.18×10^6	5.60×10^{-3}	95.6	<0.01
Atenolol	no fit		1.14×10^5	8.88	75.7	<0.01	no fit			
Atracurium	340	82.1	4.34×10^4	3.09	95.7	<0.01	4.49×10^5	3.33×10^{-2}	95.6	<0.01
Azelastine	1730	88.3	2.23×10^4	1.67	94.1	0.16	1.41×10^6	4.56×10^{-3}	93.8	0.25
Biperiden	309	85.0	5.63×10^4	2.82	97.0	<0.01	1.00×10^6	9.13×10^{-3}	97.4	<0.01
Bisoprolol	no fit		7.86×10^4	3.78	93.3	<0.01	6.69×10^5	1.61×10^{-2}	89.3	0.07
Buprenorphin	670	90.3	3.46×10^4	2.20	96.8	0.07	9.82×10^5	9.74×10^{-3}	97.7	0.01
Bupropion	no fit		8.09×10^4	3.92	96.0	<0.01	6.45×10^5	1.97×10^{-2}	94.7	<0.01
Carbamazepin	no fit		6.80×10^4	3.07	99.8	<0.01	no fit			
Chloprothixen	2830	94.6	1.05×10^4	1.30	96.0	3.06	1.69×10^6	3.42×10^{-3}	96.1	2.33
Chlorpromazine	6890	94.9	2.66×10^4	1.33	96.5	2.4	2.75×10^6	5.76×10^{-3}	97.2	0.41
Cilazapril	265	72.4	9.72×10^4	3.72	97.7	<0.01	8.56×10^5	2.30×10^{-2}	98.0	<0.01
Citaprolam	no fit		4.87×10^4	3.27	92.6	<0.01	5.19×10^5	1.25×10^{-2}	87.3	0.07
Clemastine	763	89.8	2.52×10^4	1.99	96.3	<0.01	9.81×10^5	6.56×10^{-3}	97.1	<0.01
Clomipramine	1050	91.2	2.37×10^4	1.87	96.7	<0.01	1.04×10^6	6.01×10^{-3}	96.7	<0.01
Clonazepam	548	80.3	7.31×10^4	2.97	97.4	<0.01	9.03×10^5	1.78×10^{-2}	97.0	0.02
Clotrimazol	1600	92.0	1.55×10^4	1.55	95.3	0.39	1.35×10^6	4.30×10^{-3}	95.9	0.13
Codeine	no fit		4.44×10^4	3.23	97.0	<0.01	4.92×10^5	1.06×10^{-2}	94.7	0.01
Cyproheptadine	422	81.8	4.59×10^4	2.50	95.3	<0.01	1.13×10^6	4.89×10^{-3}	94.3	<0.01
Desloratadin	522	88.7	3.56×10^4	2.32	97.0	<0.01	9.34×10^5	7.58×10^{-3}	97.1	<0.01
Diclofenac	646	87.9	4.51×10^4	2.33	98.2	0.04	1.26×10^6	4.07×10^{-3}	99.5	<0.01
Dicycloverin	458	89.0	4.44×10^4	2.44	97.7	<0.01	1.13×10^6	6.93×10^{-3}	97.9	<0.01
Diltiazem	382	75.4	5.10×10^4	3.03	92.9	<0.01	5.83×10^5	2.33×10^{-3}	91.7	0.02
Diphenhydramin	272	71.0	6.72×10^4	3.77	98.4	<0.01	5.08×10^5	1.78×10^{-2}	93.2	0.02
Donepezil	2880	92.1	1.47×10^4	1.42	95.1	0.68	1.25×10^6	5.53×10^{-3}	95.0	0.86
Duloxetin	973	95.0	1.14×10^4	1.64	98.2	0.5	7.61×10^5	4.32×10^{-3}	98.5	0.24
Eprosartan	376	81.2	7.87×10^4	3.22	97.2	<0.01	8.96×10^5	1.88×10^{-2}	97.9	<0.01
Estradiol	1440	88.0	4.11×10^4	2.10	97.3	4.77	1.05×10^6	8.59×10^{-3}	98.3	2.4
Estrone	424	91.3	9.03×10^3	1.69	95.6	18.7	1.07×10^6	1.49×10^{-3}	97.0	9.98

Table 2. *Cont.*

Linear * Isotherm			Freundlich Isotherm				Langmuir Isotherm			
Substance	K _d (L/g)	R ² (%)	K _f (L/g)	n	R ² (%)	p Value (%)	τ _{MAX} (L/g)	K _L	R ² (%)	p Value (%)
Fentanyl	311	76.7	1.06 × 10⁵	3.12	94.6	<0.01	1.92×10^6	6.25×10^{-3}	94.4	<0.01
Fexofenadine	572	81.2	6.26×10^4	2.87	95.4	0.01	7.88 × 10⁵	2.69 × 10⁻²	96.8	<0.01
Finasteride	2430	94.1	1.70×10^4	1.48	97.8	3.44	1.70 × 10⁶	3.39 × 10⁻³	98.3	1.65
Flecainide	no fit		6.88 × 10⁴	3.58	93.0	<0.01	6.61×10^5	1.43×10^{-2}	89.6	<0.01
Fluconazole	no fit		7.35 × 10⁴	3.50	96.1	<0.01	7.66×10^5	1.22×10^{-2}	95.6	<0.01
Fluoxetin	471	87.4	3.15 × 10⁴	2.23	96.3	<0.01	1.05×10^6	4.88×10^{-3}	96.0	0.01
Flutamid	2230	84.8	7.07×10^4	2.26	96.3	5.49	1.26 × 10⁶	1.39 × 10⁻²	97.7	2.61
Glibenclamide	7210	82.6	6.34×10^3	0.97	82.6	88.8	1.19×10^7	6.66×10^{-4}	82.8	72.25
Haloperidol	2430	90.6	2.00×10^4	1.59	95.6	0.09	1.04 × 10⁶	7.74 × 10⁻³	95.6	0.09
Hydroxyzine	351	80.4	4.00 × 10⁴	2.74	94.1	<0.01	6.33×10^5	1.22×10^{-2}	93.3	<0.01
Ibersartan	1600	89.9	7.04×10^4	2.29	96.6	<0.01	1.38 × 10⁶	2.18 × 10⁻²	98.0	<0.01
Ibuprofen	310	84.5	9.27×10^3	1.91	91.3	2.56	no fit			
Levonorgestrel	529	89.9	no fit				no fit			
Loperamide	1760	91.8	3.12×10^4	1.74	96.3	0.17	1.85 × 10⁶	5.55 × 10⁻³	96.6	0.08
Maprotilin	440	86.9	3.08 × 10⁴	2.36	95.6	<0.01	7.54×10^5	7.88×10^{-3}	95.3	<0.01
Megestrol	1950	93.7	2.08 × 10⁴	1.66	99.5	1.01	1.18×10^6	4.85×10^{-3}	99.3	1.56
Memantin	no fit		4.52×10^4	3.83	97.4	<0.01	4.38 × 10⁵	4.81 × 10⁻³	98.0	<0.01
Metoprolol	no fit		8.21 × 10⁴	3.94	97.9	<0.01	6.04×10^5	1.84×10^{-2}	93.4	0.11
Mianserin	360	80.6	3.58 × 10⁴	2.63	94.6	<0.01	6.47×10^5	8.17×10^{-3}	92.5	0.02
Naloxon	no fit		5.32 × 10⁴	3.51	96.8	<0.01	5.13×10^5	1.85×10^{-2}	98.6	<0.01
Nefazodon	13,200	77.3	1.23 × 10²	0.45	95.7	<0.01				
Orphenadrin	374	85.9	5.28×10^4	2.74	97.3	<0.01	9.37 × 10⁵	1.13 × 10⁻²	98.1	<0.01
Oxazepam	178	84.5	no fit				no fit			
Paroxetin	1350	89.2	2.79 × 10⁴	1.84	95.2	0.21	1.29×10^6	5.88×10^{-3}	95.8	0.9
Pizotifen	419	85.6	3.33 × 10⁴	2.40	96.2	<0.01	8.20×10^5	7.04×10^{-3}	96.1	<0.01
Progesteron	6040	96.9	8.58×10^3	1.08	97.1	76.5	3.73×10^6	2.00×10^{-3}	97.5	58.3
Promethazin	1120	91.7	3.75×10^4	2.10	96.6	0.33	9.93 × 10⁵	1.38 × 10⁻²	97.4	0.08
Repaglinide	609	71	7.54 × 10⁴	2.88	94.7	0.08	1.05×10^6	8.92×10^{-3}	91.7	0.41
Risperidon	4220	94.6	1.15×10^4	1.24	95.7	5.4	1.99×10^6	3.57×10^{-3}	95.7	5.58
Roxithromycine	799	88.3	2.99×10^4	2.11	96.0	0.13	8.80 × 10⁵	8.19 × 10⁻³	97.1	0.02
Sertraline	1030	92.0	1.60×10^4	1.67	96.0	0.12	1.26 × 10⁶	3.53 × 10⁻³	96.0	0.1
Sotalol	no fit		8.07 × 10⁴	4.64	98.3	<0.01	4.63×10^5	2.00×10^{-2}	92.4	0.01

Table 2. *Cont.*

Linear * Isotherm			Freundlich Isotherm				Langmuir Isotherm			
Substance	K_d (L/g)	R ² (%)	K_f (L/g)	n	R ² (%)	p Value (%)	τ_{MAX} (L/g)	K_L	R ² (%)	p Value (%)
Sulfamethoxazol	226	83.8	2.99×10^4	2.47	99.8	0.5	9.26×10^5	2.21×10^{-3}	99.4	1.98
Tamoxifen	3550	94.1	1.05×10^3	0.81	95.6	5.25	no fit			
Terbutaline	no fit		1.67×10^4	4.40	95.9	<0.01	8.83×10^5	2.41×10^{-2}	88.4	<0.01
Tramadol	no fit		6.56×10^4	3.87	95.7	<0.01	5.59×10^5	1.89×10^{-2}	97.3	<0.01
Trihexyphenidyl	264	82.9	5.86×10^4	3.02	96.8	<0.01	8.70×10^5	1.15×10^{-2}	97.5	<0.01
Venlafaxin	no fit		1.13×10^5	5.59	96.7	<0.01	5.11×10^5	2.09×10^{-2}	82.9	0.02
Verapamil	2120	94.2	1.32×10^4	1.44	97.2	0.29	1.42×10^6	3.63×10^{-3}	97.6	0.1
Zoldipem	1160	87.5	5.38×10^4	2.34	96.4	<0.01	1.01×10^6	1.90×10^{-2}	97.2	<0.01

* Forced through zero. ** The best fitted isotherm of linear, Freundlich and Langmuir for the pharmaceuticals studied are shown in bold. Further, the significance (p) shows that the linear model has a better fit than the other models tested.

3.2. Removal of Pharmaceuticals by Use of PAC

In order to estimate the quantity of PAC needed in an additional treatment in WWTPs, the obtained distribution coefficients were used in combination with measured concentrations in the effluent at Swedish WWTPs (data from [4]). Only for the 19 pharmaceuticals given in Table 3 does substantial data exist. The target concentration in the effluent after treatment was set to 10 ng/L. A target concentration was defined since neither discharge limit values nor environmental quality standards had been decided on for pharmaceuticals. There is no scientific evidence saying that 10 ng/L is low enough to avoid unwanted biological effects, especially not in a cocktail containing numbers of micropollutants. However, this approach at least illustrates how much PAC is needed to reach ng/L levels of these pharmaceuticals. It should be noted that the target concentration of 10 ng/L is lower than the majority of the environmental quality standards decided on in the Water Framework Directive [22]. Another reason is that it is not viable to set a concentration limit for any compound in wastewater effluent, which is below present LOQ, since monitoring would not be possible. A literature review showed that LOQ for many of the pharmaceuticals is in the range 1–20 ng/L level when using LC-MS/MS [20,23,24]. However, for some pharmaceuticals, LOQ are higher (50–120 ng/L; [17,20,25]). This means that the target set would be too low to allow quantification for some compounds and the required target concentration has, in practice, to be adjusted after the LOQ. In Switzerland, the choice has fallen on an 80% reduction of micropollutants in the wastewater effluent [26] without considering the concentration in the effluent. However, this approach is not in accordance with the Water Framework Directive, which applies environmental quality standards [22], and consequently was a different approach compared to the one taken in this study.

Table 3. Pharmaceuticals divided into groups based on their concentrations in Swedish wastewater effluents [4], and the desired level of reduction for each group to reach the target concentration.

Conc:	1–10 ng/L	10–100 ng/L	100–1000 ng/L
Preferred reduction	0%	90%	99%
Pharmaceuticals	estrone	desloratadine	atenolol
	glibenclamide	estradiol	carbamazepine
	risperidon	fluoxetine	codeine
	zoldipem	progesterone	citalopram
		sertraline terbutaline	diclofenac ibuprofen
			atenolol
			metoprolol
			oxazepam
			tramadol

Since the target concentration in the effluent after treatment was set to 10 ng/L, no additional removal is needed for those pharmaceuticals that are present at low concentrations, i.e., <10 ng/L. A 90% reduction was applied for pharmaceuticals present in concentrations in the range of 10 to 100 ng/L, while a 99% reduction was applied for those found in concentrations >100 ng/L (Table 3).

The doses of PAC needed in order to reduce the pharmaceuticals present in the highest concentrations (100–1000 ng/L) in Swedish WWTP effluents by 99% are presented in Figure 1. It is seen that the needed dose to reach >99% reduction varies a lot, from almost nothing to up to more than 500 g/m³.

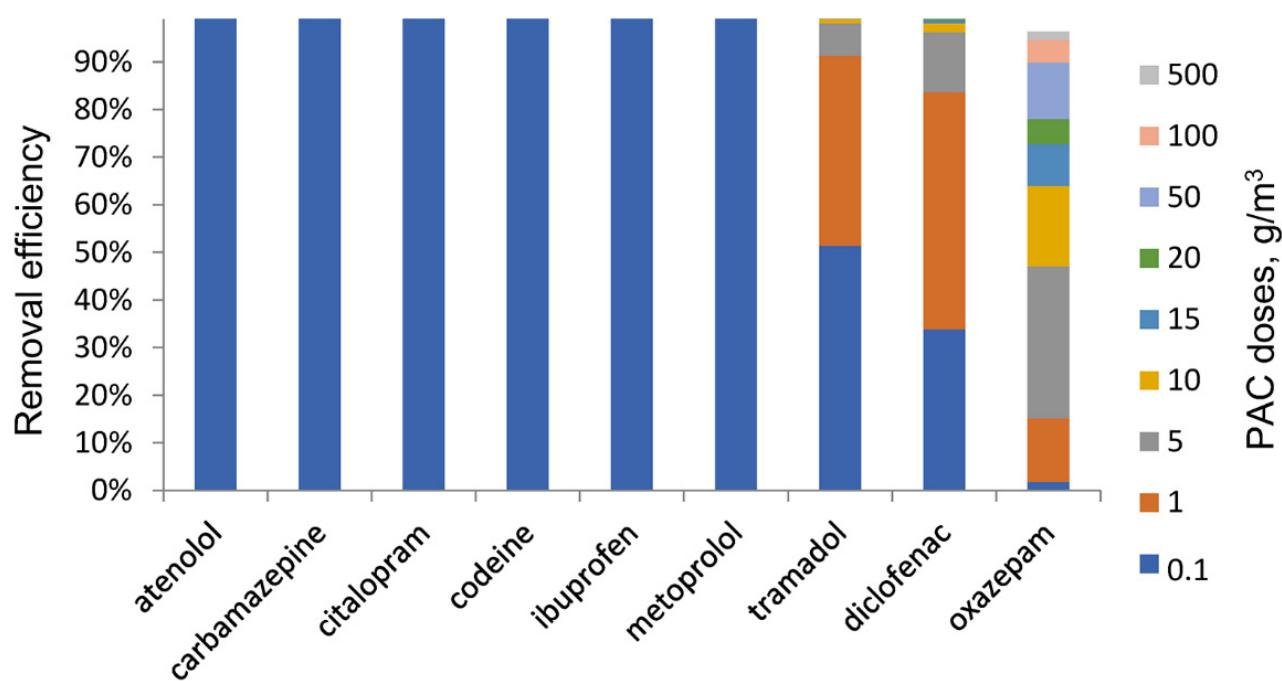


Figure 1. Amount of PAC needed in order to reach 99% reduction if the concentration of the pharmaceuticals was 1000 ng/L in the wastewater effluents. These pharmaceuticals were measured in the range of 100–1000 ng/L.

Most of the pharmaceuticals in this group will be sufficiently removed by the addition of a low amount of PAC, e.g., 0.1 g/m³. However, three of the pharmaceuticals require greater amounts. For tramadol and diclofenac, 10 g/m³ and 15 g/m³, respectively, are required in order to reach 99% reduction, while for oxazepam more than 500 g/m³ would be required. Doses >50 g/m³ are not practically realistic.

A literature review showed that these nine pharmaceuticals have been observed worldwide in wastewater effluents. The range is large, from 1 to 7043 ng/L, where the concentrations of the individual pharmaceuticals varied between 65–3494, 13–4609, 1–189, 10–1502, 209–4200, 6–660, 87–1603, 60–7043 and 5–1766 ng/L, for atenolol, carbamazepine, citalopram, codeine, ibuprofen, metoprolol, tramadol, diclofenac and oxazepam, respectively (e.g., [17,27–29]). The reported worldwide concentrations showed that these pharmaceuticals are discharged in relatively high concentrations. The first six pharmaceuticals in Figure 1 (from the left) remain easily reduced with the low doses of PAC, even if the concentration in the effluent is in the higher range of the above listed. As Figure 1 demonstrates, tramadol, diclofenac and oxazepam are not substantially reduced by PAC. This means, in practice, that PAC may not be a relevant choice if legislation will require concentrations < 10 ng/L of those pharmaceuticals, and other treatments should be considered.

In the middle group (10–100 ng/L) consisting of six pharmaceuticals, the amount of PAC required in order to reduce them by 90% is presented in Figure 2. It is shown that only fluoxetine will be reduced to the target level by the lowest dose of 0.1 g/m³. Increasing the amount of PAC to 1 g/m³ will cause terbutaline to be reduced to the target level, while by applying 5 g/m³, all pharmaceuticals in this group will be reduced to at least 90%.

Most of these pharmaceuticals are found in the same concentration range in wastewater effluents worldwide (e.g., [30–32]), except for desloratadine, for which no commentary can be made as no measurements have been found elsewhere, and terbutaline, for which the levels reported are below 10 ng/L [27].

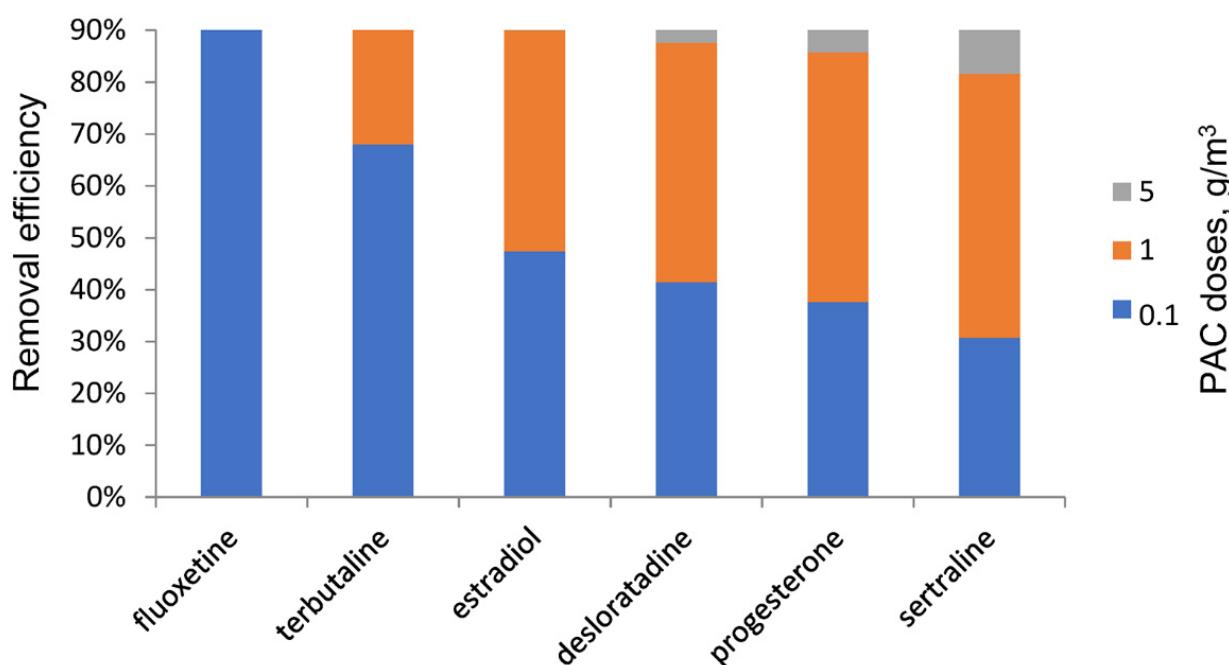


Figure 2. Amount of PAC needed in order to reach 90% reduction of the pharmaceuticals present in the range of 10–100 ng/L in wastewater effluents.

Among the 19 pharmaceuticals, which have been measured in Swedish wastewater effluents, 4 of them were found in the range of 1–10 ng/L. Consequently, no further treatment would be needed. However, there are other studies published where the concentrations of these pharmaceuticals in wastewater effluents are higher. The concentration for the individual pharmaceuticals varied between 3–78, 1–43, 3–86 and 1–43 ng/L for estrone, glibenclamide, risperidon and zoldipem, respectively (e.g., [17,27]). In comparison with the concentrations observed worldwide, the concentrations observed in Swedish wastewater effluents are in the lower end of the scale. When present in the upper end of the scale, a 90% reduction would be required in order to reach the target level. The required dose of PAC needed when applying concentrations observed outside Sweden for these four pharmaceuticals are presented in Figure 3.

As seen in Figure 3, when these four pharmaceuticals are present in concentrations of 10–100 ng/L, at least a 90% reduction will be achieved by applying 5 g/m³ for three of the pharmaceuticals, whereas estrone would require 50 g/m³.

Among the pharmaceuticals included in this study, three of them (diclofenac, oxazepam and tramadol, Figure 1), are difficult to reduce to the target level by using PAC as the treatment, since the sorption of PAC is too low. Consequently, other treatment methods should be considered if the target level cannot be reached by applying realistic doses of PAC, i.e., less than 10–20 g/m³, as stated in [17]. Based on the concentrations observed worldwide in WWTPs' effluents, estrone also qualifies for the group of pharmaceuticals where PAC is not an appropriate choice.

In [33], it is stated that the ability to remove compounds depends on the dose of PAC, contact time and the structure of the target compound. The present study clearly support the idea that the target compound and the dose affect removal efficiency.

Addition of 5 g/m³ PAC to an activated sludge system will not increase the sludge production significantly compared to the typical total sludge production of ca 400 g/m³ (dry matter), which suggests that PAC treatment-by-addition in the activated sludge system can be an easy way to upgrade WWTPs. Thus, by addition of PAC to the activated sludge system, the existing system for removal of sludge can be used for removal of sludge and PAC.

Another advantage of PAC is that no transformation products or by-products are formed, which means that no new, more-harmful compounds are added to the wastewater.

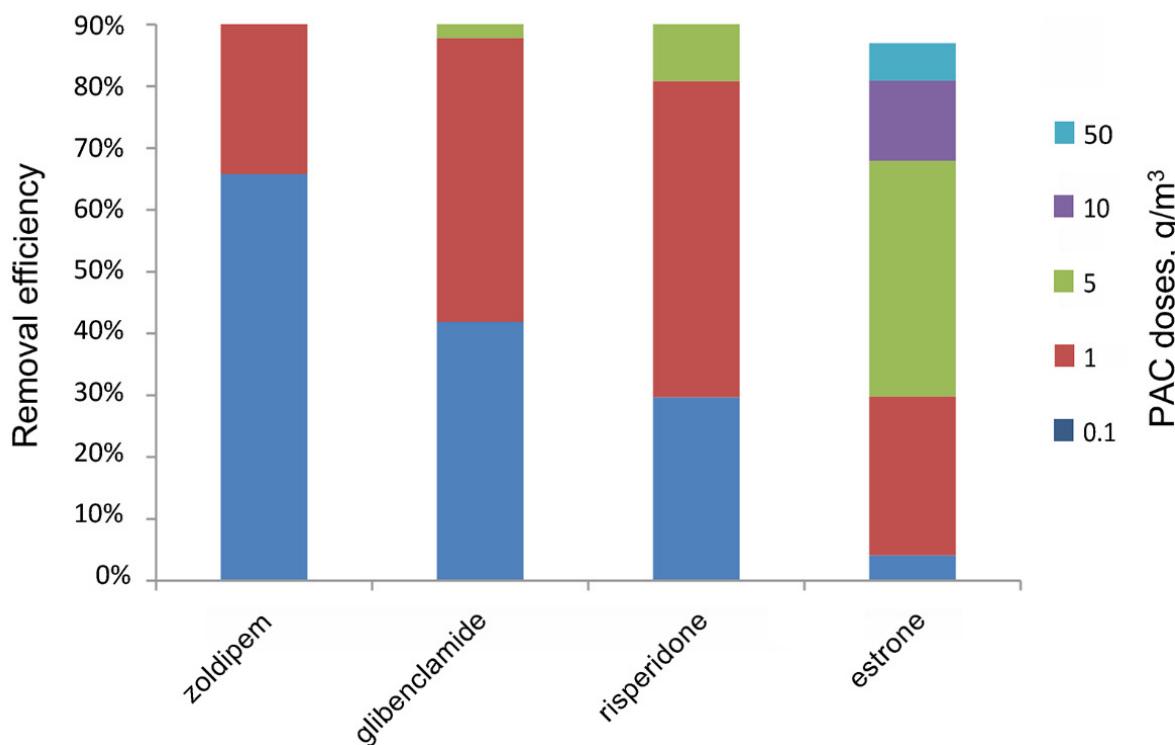


Figure 3. Amount of PAC needed in order to reach 90% reduction of the pharmaceuticals present in the range of 10–100 ng/L in wastewater effluents.

4. Conclusions

Sorption isotherms for 71 pharmaceuticals towards PAC were determined in the present study, while for 49 of the tested pharmaceuticals, no isotherms were obtained. This was either due to very high sorption and/or to limitations in the ability to quantify the compounds in low concentrations.

For 19 of the pharmaceuticals, the ranges of concentrations found in Swedish wastewater treatment plants were from levels of ng/L to μ g/L. Subdivision of the substances into three ranges, 1–10 ng/L, 10–100 ng/L and 100–1000 ng/L, were used to find the amount of PAC needed to reach a common target of 10 ng/L. Four substances in the lowest range (estrone, glibenclamide, risperidone and zoldipem) do not need any reduction. At a 10-fold higher concentration observed internationally for estrone, a high dose (up to 50 g/m³ PAC) will be needed, whereas the other three compounds could easily be removed to the target concentration at a dose of up to 5 g/m³ PAC. Six substances in the medium range (fluoxetine, terbutaline, estradiol, desloratadine, progesterone and sertraline) could easily be removed to the target concentration with a dose of 5 g/m³ or lower. In the highest range, six out of nine pharmaceuticals (atenolol, carbamazepine, citalopram, codeine, ibuprofen and metoprolol) could easily be removed to the target concentration with a low doses of <1 g/m³ PAC. Two of the remaining three (tramadol and diclofenac) could be reduced with moderate doses of 10 and 15 g/m³, respectively, whereas oxazepam have very low potential to be, in practice, removed with PAC since a dose of more than 500 g/m³ would be needed. Other treatment options have to be considered to reach the target value of 10 ng/L for that pharmaceutical.

More research is needed in order to evaluate the effect of the pharmaceuticals on sorption in a real wastewater matrix.

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