

Correction

## **Correction: Sarah Jasper and Mahmoud M. El-Halwagi A Techno-Economic Comparison between Two Methanol-to-Propylene Processes *Processes* 2015, 3, 684–698**

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The authors wish to correct Table [A1](#) of the published paper in *Processes* [1]. Flow values were reported instead of temperature and pressure values. The correct version of Table [A1](#) is given on the following page. We apologize for any inconvenience caused to readers of *Processes* by this change.

**Table A1.** The stream data for the methanol to olefins (MTO) process.

Stream	METH-IN	METH-ETH	METH-PRO	ETH-RXN	PRO-RXN	ETHANE	PROPANE	PROD-MIX	WATER	PROD-QUE
<b>Molar Flow of Components (kmol/h)</b>										
Methanol	5558.121	5558.121	5558.121	3779.522	2334.411	0	0	6113.933	1716.889	4397.044
Water	0	0	0	1778.599	3223.71	0	0	5002.309	3350.634	1651.675
Ethylene	0	0	0	889.2994	0	0	0	889.2994	0.0980242	889.2013
Propylene	0	0	0	0	1074.57	0	0	1074.57	0.1935819	1074.376
Propane	0	0	0	0	0	0	41.85	41.85	0.00458169	41.84542
Ethane	0	0	0	0	0	34.88	0	34.88	0.00372998	34.87627
Total Flow, kmol/h	5558.121	5558.121	5558.121	6447.42	6632.691	34.88	41.85	13,156.84	5067.823	8089.018
Temperature, K	723.2	723.2	723.2	723.2	723.2	723.2	723.2	723.2	343.2	343.2
Pressure, atm	1.97	1.97	1.97	1.97	1.97	1.97	1.97	1.97	0.99	0.99

**Table A1.** *Cont.*

Stream	PROD-C1	PROD-H1	DEETH-TO	DEETH-BT	S9	PROD-ETY	SPL-ETHA	PROD-PRO	SPL-PRPA
<b>Molar Flow of Components (kmol/h)</b>									
Methanol	4397.044	4397.044	2.6061E-15	4397.044	4397.044	0	0	0.0246668	4397.019
Water	1651.675	1651.675	2.792E-11	1651.675	1651.675	5.2367E-39	2.792E-11	0.1782296	1651.497
Ethylene	889.2013	889.2013	889.2013	4.44229E-09	4.44229E-09	883.9327	5.268618	4.44229E-09	1.4085E-29
Propylene	1074.376	1074.376	0.9134768	1073.463	1073.463	6.8143E-13	0.9134768	1043.909	29.55438
Propane	41.84542	41.84542	0.00891728	41.8365	41.8365	1.0975E-16	0.00891728	35.88848	5.948022
Ethane	34.87627	34.87627	34.87627	6.3888E-08	6.3888E-08	6.067282	28.80899	6.3888E-08	2.0243E-24
Total Flow, kmol/h	8089.018	8089.018	925	7164.018	7164.018	890	35	1080	6084.018
Temperature, K	561.3	283.2	227.8	275.3	223.2	226.9	243.5	299.5	416.1
Pressure, atm	11.84	11.84	11.84	11.84	11.84	11.84	11.84	0.99	11.84

## References

1. Jasper, S.; El-Halwagi, M.M. A Techno-Economic Comparison between Two Methanol-to-Propylene Processes. *Processes* **2015**, *3*, 684–698. [[CrossRef](#)]



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