**The Inversion Method of Shale Gas Effective Fracture Network Volume Based on Flow Back Data—A Case Study of Southern Sichuan Basin Shale**

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**Abstract:** Fracture network fracturing is pivotal for achieving the economical and efficient development of shale gas, with the connectivity among fracture networks playing a crucial role in reservoir stimulation effectiveness. However, flow back data that reflect fracture network connectivity information are often ignored, resulting in an inaccurate prediction of the effective fracture network volume (EFNV). The accurate calculation of the EFNV has become a key and difficult issue in the field of shale fracturing. For this reason, the accurate shale gas effective fracture network volume inversion method needs to be improved. Based on the flow back characteristics of fracturing fluids, a tree-shaped fractal fracture flow back mathematical model for inversion of EFNV was established and combined with fractal theory. A genetic algorithm workflow suitable for EFNV inversion of shale gas was constructed based on the flow back data after fracturing, and the fracture wells in southern Sichuan were used as an example to carry out the EFNV inversion. The reliability of the inversion model was verified by testing production, cumulative gas production, and microseismic results. The field application showed that the inversion method proposed in this paper can obtain tree-shaped fractal fracture network structure parameters, fracture system original pressure, matrix gas breakthrough pressure, fracture compressibility coefficient, reverse imbibition index, equivalent main fracture half length, and effective initial fracture volume (EIFV). The calculated results of the model belong to the same order of magnitude as those of the HD model and Alkouh model, and the model has stronger applicability. This research has important theoretical guiding significance and field application value for improving the accuracy of the EFNV calculation.

**Keywords:** shale gas; fracture network fracturing; effective fracture network volume (EFNV); flow back data; genetic algorithm

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**1. Introduction**

The economical and effective development of shale gas plays an important role in the world’s energy structure. The shale gas revolution in the United States has achieved great success and thus the world energy pattern has been reshaped. In 2010, the first shale gas fracturing well was implemented in China. After 10 years of development, shale gas production has achieved a new leap [1]. The practice of shale gas fracturing has found that the information on the characteristics of complex fracture network hidden in the flow back data is very important. In the past, fracturing fluid flow back data were mostly ignored. In recent years, the shale gas effective fracture network volume and fracture characteristics information included in the fracturing fluid flow back data to evaluate hydraulic fracturing...
The water and natural gas production data were analyzed in the Horn River shale, date the mechanisms of early gas production [7] compared to previous mathematical model was used to approximate the effective fracture volume as a possible method to extract the properties of hydraulic fractures. A new mathematical model was used to approximate the effective volume of fractures and elucidate the mechanisms of early gas production [7] compared to previous flow back models [8–11]. The water and natural gas production data were analyzed in the Horn River shale, and the estimation of the effective fracture volume was based on the assumption of a two-phase tank model for the fracture system. In addition, due to the high uncertainty introduced by complex flow back models in the evaluation of fracture pore volume, a two-phase tank model was built for reducing parameter uncertainty in order to estimate the fracture pore volume accurately [12]. Comparing the estimated effective fracture pore volume with fracture design parameters (soaking time and proppant concentration) revealed that fracture closure drives single-phase flow back during further analysis of the effective fracture volume. Therefore, the effective fracture pore volume largely depends on the compressibility of the fracture [13]. The evaluation of fracture compressibility is essential for calculating the effective fracture volume, as well as evaluating the fracture volume change. It was found that fracture compressibility depends on how fracture porosity and pore size vary with effective stress. The fracture compressibility is mainly affected by porosity changes in propped fractures [14]. The harmonic decline (HD) model was used to estimate the water phase flow back and the initial effective fracture volume to study the change in the effective fracture volume. According to the findings, pressure depletion and fracture closure during early-time water flow back can lead to a loss of up to 30% of the effective fracture volume. When gas from the matrix enters the fracture network and offers adequate pressure support during late-time flow back, the rate of fracture volume loss reduces [15]. A gas–water two-phase flow model was established for a fractured horizontal well considering the influence of water saturation on gas–water permeability. Sensitive studies were performed to investigate the impact of various parameters on the productivity of a horizontal well [16,17]. The flow back period can be used to quantitatively identify the characteristics of the formed fracture network and calculate the effective fracture network volume; however, such data analysis is not commonly reported in the literature. Therefore, it is necessary to develop an appropriate model to match the data and acquire valuable information on the volume of the fracture network. In this paper, a tree-shaped fractal fracture network two-phase flow back model was first established based on the flow back data, and then the effective fracture network volume was inverted. And the reliability of the model was verified by cumulative production and microseismic data. The shale gas wells were taken as an example in the southern Sichuan Basin, to obtain the effective fracture network volume, which is useful for evaluating post-fracture effects. The flow back models are summarized in Table 1.
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2. Model Development

2.1. The Model of Two-Phase Flow Back

In order to establish the flow back model, the assumptions were as follows:

1. The effective crack network of 1/2 single cluster is equivalent to the tree-shaped fractal fracture network shown in Figure 1.

2. Consider the reverse imbibition effect and the redistribution of original free gas in activated natural fractures.

3. Ignore the capillary pressure in the effective fracture network system and ignore the influence of gravity.

4. The matrix is only considered as the gas source. Material exchange occurs between the matrix system and the effective fracture network system through the cross-flow equation.

5. The effective fracture network system is an elastic porous medium, and assuming that its compressibility is much greater than that of the shale matrix, the tree-shaped fractal fracture permeability and effective fracture volume are pressure-dependent variables.

As shown in Figure 1, the flow rate of rectangular fractures at level k of 1/2 single-cluster tree-shaped fractal fracture network is described by Equation (1) according to the Hagen–Poiseuille equation:

\[ Q_k = \frac{W_{f_k}^3 h_{f_k}}{12 \mu} \frac{\Delta P_k}{l_k} \]  

where \( \Delta P_k \) is the pressure difference of the k-th level fracture, Pa; \( \mu \) is fluid viscosity, Pa s; \( l_k, W_{f_k}, h_{f_k} \) are the length, width, and height of the k-th level branch fracture, m.

The length, width, and height of cracks at level k are obtained by Equation (2).

\[ \begin{align*}
    l_k &= l_0 R_L^k \\
    W_{f_k} &= W_{f0} R_W^k \\
    h_{f_k} &= h_{f0} R_h^k
\end{align*} \]  

where \( l_0, W_{f0}, \) and \( h_{f0} \) are the length, width, and height of the initial tree-shaped fractal fractures, m; \( R_L, R_W, \) and \( R_h \) are ratio of length, width, and height of fractures, dimensionless.

From Equation (1), it can be known that the viscous resistance of fluid flow in a single fracture is
\[ R_k = \frac{12 \mu l_k}{\beta W_{f_k}^3 h_{f_k}} = \frac{12 \mu R_k^k l_0}{\beta R_{w_k}^k R_h^3 W_{f_k}^3 h_{f_k}} \]  

(3)

where \( \beta \) is the correction coefficient, which can be corrected according to the conductivity experiment in practical applications.

According to the principle of fluid pressure drop in parallel and in series [18], the parallel model was used to convert each branch into a single channel, and then the series model was applied to convert all single channels into a channel. In this way, the total viscous resistance of the network can be calculated, and the total flow resistance of the tree-shaped fractal fracture network can be expressed as Equation (4):

\[ R = \sum_{k=0}^{n} \frac{R_k}{N_k} = R_0 \left( 1 - \left( \frac{R_l}{n R_w^3 R_h} \right)^{n+1} \right) \]

(4)

where

\[ R_0 = \frac{12 \mu l_0}{\beta W_{f_{0}}^3 h_{f_{0}}} \]

(5)

\[ N_k = n^k \]

(6)

where \( n \) is the total number of branches fractal fracture, \( n = 2 \).

Then the flow rate is described by Equation (7):

\[ Q = \frac{\Delta P}{R} = \frac{\beta W_{f_0}^3 h_{f_{0}} \left( 1 - \left( \frac{R_l}{n R_w^3 R_h} \right)^{n+1} \right) \Delta P}{12 \mu l_0 \left( 1 - \left( \frac{R_l}{n R_w^3 R_h} \right)^{n+1} \right)} \]

(7)

where \( \Delta P \) is the total pressure difference of fractal fracture network, MPa.

\[ \Delta P = P_t - P_w \]

(8)

As the fracturing fluid is produced, the fracture pressure decreases, and the fracture will be compressed under the closure stress. At this time, assuming that its height and length remain unchanged, and the width of \( W_{f_k} \) at the \( k \)-th level has a width of \( W_{f_{k+1}} \) after compression, then the volume change is shown in Equation (9):

\[ V_{f_k} - V_{f_{k+1}} = C_f V_{f_k} \Delta P_l \]

(9)

where \( C_f \) is the fracture compression coefficient; \( V_{f_k} \) is the \( k \)-level single fracture volume under original fracture pressure; \( V_{f_{k+1}} \) is the \( k \)-level single fracture volume under current fracture pressure; and \( \Delta P_l \) is fracture system pressure drop, \( \Delta P_l = P_{i-w} - P_t \).

\[ V_{f_k} = W_{f_k} h_{f_k} l_k \]

(10)

\[ V_{f_{k+1}} = W_{f_{k+1}} h_{f_k} l_k \]

(11)

where \( W_{f_k} \) is the width of the \( k \)-th level single fracture under the current fracture pressure.

Equations (10) and (11) are substituted into Equation (9), and then Equation (12) can be obtained.

\[ W_{f_{k+1}} = \left( 1 - C_f \Delta P_l \right) W_{f_k} \]

(12)

The flow rate of 1/2 single-cluster tree-shaped fractal fracture network is expressed in Equation (13) by considering the fracture closure effect.
where

$$W_{fc} = (1 - C_f \Delta P_f) W_0$$

(14)

The two-phase flow depends on the relationship between gas–water relative permeability and water saturation in the fractal fracture system. In the flow model of a single-phase tree-shaped fracture network, the relative permeability is taken into account. Equation (15) illustrates the flow rate calculation model for a 1/2 single-cluster tree-shaped fracture network in gas/water two-phase flow.

$$Q_1 = \frac{\beta K_{ri} (S_w) W_{fc}^3 h_{f0} \left(1 - \frac{R_{L}}{nR_{W}^{1/3} R_h} \right) (P_i - P_{wf})}{12 \mu_i l_0 \left(1 - \left(\frac{R_{L}}{nR_{W}^{1/3} R_h} \right)^{n+1} \right)}$$

(15)

where $P_i$ is the average pressure in the fracture system, which changes as fluid is produced, MPa; $P_{wf}$ is the wellbore bottom flow pressure in a horizontal well, MPa; $I$ is water or gas; $B_i$ is volume coefficient, m$^3$/m$^3$; and $K_0(S_w)$ is the relative permeability of gas/water, dimensionless.

In this paper, the linear relative permeability model was adopted:

$$K_{rw} = S_w$$

(16)

$$K_{rg} = 1 - S_w$$

(17)

where $S_w$ is the water saturation in the fracture.

Gas production superposition model is as follows:

$$Q_g = \sum_{j=1}^{2N_f} Q_{gj}$$

(18)

Water production superposition model is as follows:

$$Q_w = \sum_{j=1}^{2N_f} Q_{wj}$$

(19)

where $N_f$ is the total clusters in horizontal well, which satisfies the following relationship:

$$N_f = n_f \cdot n_{CL}$$

(20)

where $n_f$ is the number of operation stages, dimensionless; and $n_{CL}$ is the clusters number, dimensionless.

### 2.2. Calculation of Fracture Network Volume

The volume of the fractal fracture network is

$$V_f = 2 N_f \sum_{k=0}^{n} N_k V_k = 2 N_f \sum_{k=0}^{n} n^k W_{f0} h_{f0} l_k$$

$$= 2 N_f V_0 \left(1 - \left(nR_{W} R_h R_{L} \right)^{n+1} \right)$$

(21)
Recently, the initial effective fracture volume $V_0$ has been used internationally as an important parameter for preliminary evaluation of shale gas fracture network fracturing \cite{19,20}. In the above formula,

$$V_0 = W_0 f h h_0$$  

(22)

where $V_0$ is initial volume of effective fracture, $m^3$; and $V_0$ is initial fracture volume, $m^3$.

It can be seen from Figure 1 that the longitudinal equivalent fracture half-length is

$$x_f = l_0 \left[ 1 + \frac{R_L \left( 1 - R_L^m \right) \cos \theta}{1 - R_L} \right]$$  

(23)

where $\theta$ represents the bifurcation fractures, which varies from 0 to $\pi/2$.

As shown in Figure 1, the lateral extension width is given by

$$w_f = l_0 R_L \sin \theta \left( 1 - R_L^m \right)$$  

(24)

The effective fracture network volume can be obtained by Equation (25):

$$\text{EFNV} = N_f x_f h h_0 - V_{b\text{, overlap}}$$  

(25)

where $x_f$ denotes the longitudinal expansion degree and $w_f$ denotes the lateral expansion degree. It is an important parameter commonly used in quantitative evaluation of shale gas fracture network fracturing \cite{21,22}, where

$$w_f = l_0 R_L \sin \theta \left( 1 - R_L^m \right)$$  

(26)

$$V_{b\text{, overlap}} = \begin{cases} 
2S_{\text{overlap}} h h_0 (N_f - 1) & w_f > \frac{L_w}{N_f} \\
0 & w_f \leq \frac{L_w}{N_f} 
\end{cases}$$  

(27)

where $V_{b\text{, overlap}}$ signifies the volume of overlap area within the EFNV.

In the matrix, the gas is entered the fracture network through the reverse imbibition of the fracturing fluid and the redistribution of the original free gas in the activated natural fractures during the process of fracturing and soaking. The reverse imbibition index ($I_{imb}$) is adopted to represent the combined effect. The primary origin of initial free gas in the effective fracture system is the reverse imbibition process \cite{23}. The shale reverse imbibition index $I_{imb}$ represents the proportion of free gas in the fracture network to the fracture volume, $0 \leq I_{imb} \leq 1$. Obviously, there is the following relationship, the gas saturation of the original fracture is

$$S_{gi} = I_{imb}$$  

(28)

The volume of free gas within the subsurface fractures is

$$V_{gfi} = I_{imb} V_f$$  

(29)

Then the volume occupied by water within the fracture is

$$V_{wi} = (1 - I_{imb}) V_f$$  

(30)

Water saturation of fractures is as follows:

$$S_{wi} = \frac{V_{wi}}{V_f} = 1 - I_{imb}$$  

(31)

where $S_{gi}$ represents the original gas saturation within fractures, dimensionless; $V_{gfi}$ represents the volume of free gas within the subsurface fractures, $m^3$; $V_{wi}$ is water volume
in fractures, m³; and \( S_{wi} \) is water saturation in fractures under initial conditions, dimensionless.

2.3. Material Balance Equation

The change of fracture volume is very complicated in the process of flow back. The pressure of the fracture system drops from the original fracture pressure \( P_i \) to the current fracture pressure \( P_f \), and the fracture pressure drop is \( \Delta P_f = P_i - P_f \) when a certain amount of fracturing fluid \( (W_p) \) is discharged from the fracture. The reduction of the fracture volume, the expansion of the free gas volume in the fracture, and the entry of matrix gas into the fracture will all reduce the volume of the fracturing fluid.

(1) The reduction of fracture volume is calculated by

\[
\Delta V_f = V_i C_f \Delta P_f
\]

(a) In fracture network, the expansion of free gas can be expressed as

\[
\Delta V_{ gf} = V_{ gf} - V_{ gfi} = I_{mb} V_i \left( \frac{B_{gf}}{B_{gfi}} - 1 \right)
\]

where \( V_{gf} \) is the gas volume in the current fracture, m³; \( V_{gfi} \) is the gas volume in the original fracture, m³; \( B_{gf} \) is the gas volume factor in the fracture, m³/m³; \( B_{gfi} \) is the original gas volume factor in the fracture, m³/m³; \( P_i \) is original fracture pressure, MPa; and \( P_f \) is current fracture pressure, MPa.

(b) Intrusion of matrix gas

The ground volume of intrusion of matrix gas channeling into the tree-shaped fractal fracture network is obtained using Equation (34) by considering the compressibility of matrix pores and the desorption effect of adsorbed gas in shale matrix.

\[
G_{mf} = \frac{V_b \phi_m - V_b \phi_m \left(1 - C_m \Delta P_m \right)}{B_{gmi}} + V_b \left(1 - \phi_m\right) \left(V_{Ei} - V_E \right)
\]

where \( B_{gmi} \) and \( B_{gmi} \) are matrix gas volume coefficient under the condition of current matrix pressure and original matrix pressure, m³/m³; \( \phi_m \) is matrix porosity of shale reservoir, dimensionless; \( C_m \) is rock compressibility coefficient of shale matrix, 1/MPa; \( V_{Ei} \) and \( V_E \) are unit shale adsorbed gas volume under original matrix pressure and current matrix pressure, m³/m³; and \( \Delta P_m \) is matrix pressure drop, MPa.

\( V_b \) is the effective fracture network volume and the calculation method is shown in Equation (25). The average pressure drop of the matrix system and the desorption of matrix adsorbed gas are calculated as follows:

\[
\Delta P_m = P_{mi} - P_m
\]

\[
V_{Ei} = V_L \frac{P_{mi}}{P_L + P_{mi}}
\]

\[
V_E = V_L \frac{P_m}{P_L + P_m}
\]

The underground volume of matrix shale gas intrusion can be obtained as Equation (38) by combining it with the gas volume coefficient under the fracture pressure.

\[
V_{mt} = G_{mf} B_{gf}
\]

where \( P_{mi} \) is shale original matrix pressure, MPa; \( P_m \) is shale current matrix pressure, MPa; \( V_L \) is Langmuir volume, sm³/m³; \( P_i \) is Langmuir pressure, MPa; and \( G_{mf} \) is matrix shale surface volume of intrusion of gas channeling into the tree-shaped fractal fracture network, m³.

(c) Produced free gas (underground volume)
\[
\Delta V_{gp} = G_p B_{gf}
\]  
(39)

The gas storage capacity of fractures is obtained by combining Equations (33), (38), and (39).

\[
\Delta V_{g} = \Delta V_{gr} + V_{mf} - \Delta V_{gp}
\]  
(40)

where \(G_p\) is cumulative gas production, m³.

(2) The remaining volume of fracturing fluid in the fracture system

The volume of fracturing fluid in fractures will all be reduced due to the reduction of fracture pore volume, the expansion of fracturing fluid in fractures, and the gas storage capacity in fractures. Therefore, when the fracture original pressure \(P_f\) decreases to \(P_i\), the fracture fracturing fluid volume is

\[
V_w = V_{wi} - \Delta V_f - \Delta V_g
\]  
(41)

Then, Equation (42) can be obtained by combining Equations (32), (40), and (41):

\[
V_w = V_{wi} - V_i C_f \Delta P - I_{imb} V_{fi} \left( \frac{B_{gf}}{B_{gfi}} - 1 \right) - G_{mf} B_{gf} + G_p B_{gf}
\]  
(42)

The remaining fracturing fluid volume is converted to surface conditions:

\[
W_{res} = \frac{V_w}{B_{wf}} = \frac{\left( V_{wi} - V_i C_f \Delta P - I_{imb} V_{fi} \left( \frac{B_{gf}}{B_{gfi}} - 1 \right) - G_{mf} B_{gf} + G_p B_{gf} \right)}{B_{wf}}
\]  
(43)

The basic form of the fracturing fluid material balance equation in the fracture is as follows:

\[
\frac{V_{wi}}{B_{wi}} = W_p + W_{res}
\]  
(44)

where \(B_{wi}\) is the fracturing fluid volume coefficient under original pressure, dimensionless; \(W_p\) is current cumulative fracturing fluid volume of flow back m³; and \(W_{res}\) is the remaining fracturing fluid volume, m³.

The remaining fracturing fluid volume \(W_{res}\) is inputted into the above formula:

\[
\frac{V_{wi}}{B_{wi}} = W_p + \frac{\left( V_{wi} - V_i C_f \Delta P - I_{imb} V_{fi} \left( \frac{B_{gf}}{B_{gfi}} - 1 \right) - G_{mf} B_{gf} + G_p B_{gf} \right)}{B_{wf}}
\]  
(45)

Then,

\[
W_p B_{wf} + G_p B_{gf} = V_{wi} \left( \frac{B_{wf} - B_{wi}}{B_{wi}} \right)
\]  
+ \(V_i C_f \Delta P_f + I_{imb} V_{fi} \left( \frac{B_{gf}}{B_{gfi}} - 1 \right) + G_{mf} B_{gf}
\]  
(46)

where \(B_{wf}\) is the fracturing fluid volume coefficient under the current fracture pressure, m³/m³; and \(B_{wi}\) is the fracturing fluid volume coefficient under the original fracture pressure, m³/m³.

The compressibility coefficients of gas and water are
\[ C_g = \frac{B_{gf} - B_{gfi}}{B_{gfi} \Delta P_f} \]  

(47)

Then,

\[ W_p B_{wf} + G_p B_{gf} = V_{fi} \Delta P \left[ (1 - I_{imb}) C_{wf} + C_f + I_{imb} C_g \right] + G_{mf} B_{gf} \]  

(48)

The function \( h \) representing the fracture pressure and matrix pressure at the \( k + 1 \)th time step is defined as follows:

\[ h(P_{f}^{k+1}, P_{m}^{k+1}) = \]

\[ V_{fi} \left( P_{fi} - P_{f}^{k+1} \right) \left( (1 - I_{imb}) C_{wf} + C_f + I_{imb} C_g \right) + G_{mf} B_{gf} \left( P_{f}^{k+1} \right) - W_p B_{wf} \left( P_{f}^{k+1} \right) - G_p B_{gf} \left( P_{f}^{k+1} \right) \]  

(49)

where

\[ B_{gf} \left( P_{f}^{k+1} \right) = \frac{P_{sc}}{Z_{sc} T_{sc} P_{f}^{k+1}} \]  

(50)

where \( C_{mf} \) is fracturing fluid compression coefficient in fractures, dimensionless; \( P_{sc} \) is ground pressure, MPa; \( Z_{sc} \) is gas deviation factor in ground conditions, dimensionless; \( T_{sc} \) is ground temperature, K; \( Z_{f} \) is gas deviation factor in fractures, dimensionless; and \( T_{i} \) is original formation temperature of reservoir, K.

Water saturation of fractures under current formation conditions is as follows:

\[ S_w = \frac{V_w}{V_w + V_{gfi} + \Delta V_g} \]  

(51)

The equation can be simplified to

\[ S_w = \frac{V_w}{V_{fi} - \Delta V_f} \]  

(52)

The equations for fracture and matrix pressure at time \( k + 1 \) can be derived by setting Equation (49) equal to zero.

\[ h(P_{f}^{k+1}, P_{m}^{k+1}) = 0 \]  

(53)

The material balance equation needs to be established of the shale matrix system to solve this equation due to there being two unknowns, \( P_{f}^{k+1} \) and \( P_{m}^{k+1} \).

If the fracture pressure \( (P_f) \) falls below the matrix gas breakthrough pressure \( (P_{BT}) \), it will result in channeling between the matrix and fractures. The pressure \( P_{BT} \) is related to the porosity and permeability of the matrix. The channeling equation [24] is described by Equation (54).

\[ q_m = \frac{k_m \alpha_{mf} (P_m - P_f)}{\mu_g} \]  

(54)

If \( P_{BT} \leq P_f \), then the channeling from the matrix to the fracture system from time \( k \) to \( k + 1 \) is 0:

\[ \Delta G_{mf} = 0 \]  

(55)

If \( P_{BT} > P_f \), the channeling from the matrix to the fracture system from time \( k \) to \( k + 1 \) is

\[ \Delta G_{mf} = \Delta V_b \phi_m q_m = \Delta V_b \frac{\phi_m k_m \alpha_{mf} (P_m - P_{f}^{k+1})}{\mu_g} \]  

(56)
where $\Delta G_{mf}$ is the channeling of gas from the shale matrix to the fracture system from time $k$ to time $k + 1$, m$^3$; $\Delta t$—the time from time $k$ to time $k + 1$, s; $V_b$ is shale reservoir stimulation volume, m$^3$; $\phi_m$ is matrix porosity of reservoir, dimensionless; $q_m$ is gas channeling flow from matrix to fracture system per unit time, m$^3$/s; $k_m$ is matrix permeability, m$^2$; $\alpha_{mf}$ is matrix to fracture channeling factor [25], m$^{-2}$; $P_{mk}$ is average pressure of shale matrix system at time $k$, MPa; $P_{fk+1}$ is average pressure of fracture system at time $k + 1$, MPa; and $\mu_g$ is shale gas viscosity, Pa·s.

The channeling flow diffusion from the matrix to the fracture system from time $k$ to $k + 1$ can also be expressed as

$$\Delta G_{mf} = G_{mf}^{k+1} - G_{mf}^k$$

where

$$G_{mf}^k = \frac{V_b \phi_m}{B_{gmi}} - \frac{V_b \phi_m \left(1 - C_m \left(P_{mk} - P_m^k\right)\right)}{B_{gmi}^k}$$

$$+ V_b \left(1 - \phi_m\right) \left(V_E - V_i \left(P_m^k\right)\right)$$

$$G_{mf}^{k+1} = \frac{V_b \phi_m}{B_{gmi}} - \frac{V_b \phi_m \left(1 - C_m \left(P_{mk} - P_m^{k+1}\right)\right)}{B_{gmi}^{k+1}}$$

$$+ V_b \left(1 - \phi_m\right) \left(V_E - V_i \left(P_m^{k+1}\right)\right)$$

$$V_E = \frac{V_L P}{P + P_L}$$

where $V_L$ is Langmuir volume, sm$^3$/m$^3$; $P_L$—Langmuir pressure, MPa. $B_{gm}$ and $B_{gmi}$ are matrix gas volume coefficient under current matrix pressure and original matrix pressure, m$^3$/m$^3$; $C_m$ is rock compressibility coefficient of shale matrix, 1/MPa; and $V_i$ and $V_E$ are the unit shale adsorbed gas volume under original matrix pressure and current matrix pressure, m$^3$/m$^3$.

Equations (58) and (59) are substituted into Equation (57), then Equation (61) can be obtained.

$$\Delta G_{mf} = G_{mf}^{k+1} - G_{mf}^k$$

$$= \frac{V_b \phi_m \left(1 - C_m \left(P_{mk} - P_m^k\right)\right)}{B_{gmi}^k}$$

$$- \frac{V_b \phi_m \left(1 - C_m \left(P_{mk} - P_m^{k+1}\right)\right)}{B_{gmi}^{k+1}}$$

$$+ V_b \left(1 - \phi_m\right) \left(V_E \left(P_m^k\right) - V_E \left(P_m^{k+1}\right)\right)$$

The function $g$ representing the fracture and matrix pressure at the k + 1 time step is derived from Equation (62) by combining Equations (56) and (61):
The equations for the fracture network and matrix pressure at time $k + 1$ can be derived by setting Equation (62) to zero:

$$g(P_{f}^{k+1}, P_{m}^{k+1}) = 0$$

There are two unknowns, $P_{f}^{k+1}$ and $P_{m}^{k+1}$, in the above equation, and the fracture pressure $P_{f}^{k+1}$ and matrix pressure $P_{m}^{k+1}$ at time $k + 1$ can be obtained by solving Equations (53) and (63), and the fracture pressure $P_{f}^{k}$ and matrix pressure $P_{m}^{k}$ at time $k$ are known.

2.4. Model Solution

1. The tree-shaped fracture network structure parameters are preset, including $l_0$, $W_0$, $h_0$, $R_t$, $R_w$, $R_h$, $\theta$, $m$, $n$, and $C_l$, and initial fracture network and matrix average pressure ($P_f(k = 1) = P_{f0}$, $P_m(k = 1) = P_{m0}$) and the bottom hole flow pressure $P_{wf}$, then $Q_w(k)$ and $Q_g(k)$ is calculated by Equation (15), $k = 1, 2, \ldots, \text{Num}$;

2. The cumulative production of step $k$ is solved, the cumulative flow back $W_p = \sum(Q_w(k))$, and the cumulative gas production $G_p = \sum(Q_g(k));$

3. If $P(k) > P_{fr}$, then there is no matrix gas channeling into the effective fracture network, $G_{mf} = 0$, and then $P_{m}(k + 1) = P_{m}(k)$. Based on the dichotomy method, the fracture pressure $P_{f}(k + 1)$ is calculated by combining the fracture material balance Equation (49), and the network average pressure $P_{f}(k + 1)$ ranges from $[0, P_{f}^{k}]$. When $P_{f}(k) < P_{fr}$, the matrix gas channeling into fractures, the fracture pressure $P_{f}(k + 1)$ range $[0, P_{f}^{k}]$, under the condition of known $P_{f}(k + 1)$, the matrix pressure $P_{m}(k + 1)$ range $[0, P_{m}^{k}]$. The matrix pressure $P_{m}(k + 1)$ is calculated in combination with the matrix material balance Equation (62), and then $G_{mf}$ is calculated by using Equation (34), which is then brought into the Equation (49), and $P_{f}(k + 1)$ is solved by the dichotomy method.

4. The $P_{f}(k + 1)$ and $P_{m}(k + 1)$ are assigned to $P_{f}(k)$ and $P_{m}(k)$, and steps (1), (2), and (3) are repeated until $k = \text{Num}$.

2.5. Flow Back Model Validation

The rate transient analysis (RTA) method was used to identify and calculate the flow back flow stage of early shale fracturing. Since a constant flow rate or bottom hole flow pressure was rarely used in the flow back, a small oil nozzle is usually used to control the discharge, step by step amplification, and adjust a stable drainage system in southern Sichuan. Therefore, the rate normalized pressure (RNP) and its derivative (RNP') were used to observe the flow back characteristics. The equations are as follows [26]:

$$\text{RNP} = \frac{P_{wf} - P_{f}^{k}}{q_w}$$

$$\text{RNP} = \frac{d\text{RNP}}{d\lnfr}$$
\[ r_{MB} = \frac{W_f}{q_w} \tag{66} \]

where \( P_b \) is initial fracture network pressure, MPa; \( P_w \) is bottom hole flow pressure, MPa; \( q_w \) is water production rate, m³/h; \( t_{MB} \) is equivalent time, h; and \( W_f \) is cumulative water production, m³.

The established shale gas fracturing two-phase flow back model was used to calculate the flow back data of 1000 h. The model parameter settings are shown in Table 2. As shown in Figure 2, in the initial state, the effective fracture network volume is completely filled with water \( (I_{imb} = 0) \) and the observed flow stages are consistent with field data [27] and analytical models [26] and Williams-Kovacs [28]. For the case of \( I_{imb} = 0 \), the two phases in RNP' are characterized by a slope equal to 1. If the free gas is contained in the effective fracture network volume in the initial state, the more free gas content, the smaller the slope in stage 2 (for example, the slope of 0.70 at \( I_{imb} = 0.1 \) is greater than the slope of 0.65 at \( I_{imb} = 0.3 \)), and the slope of stage 3 is always 1. Stage 2 and stage 3 last for a long time, and the characteristics of these two stages can be fully reflected by the flow back model proposed in this paper, so the established model is reasonable.

Some assumptions were made on the real seepage state of the fracturing fluid in order to be used in the inversion of the effective fracture network volume, so that the model will deviate from the real characteristics of the fluid flow back stage. But because the permeability of the effective fracture network is very large, the pressure wave propagates very fast, and this flow stage is usually impossible to observe in traditional low-frequency flow back data (transient flow in the fracture system may last only 10 s [29], and the absence of this stage has little error in the inversion). Stage 2 and stage 3 are the main stages in the production process of flow back, and the model proposed in this paper can fully reflect the characteristics of these two stages. It shows that the flow back model proposed in this paper is reasonable.

<table>
<thead>
<tr>
<th>Parameter</th>
<th>Unit</th>
<th>Value</th>
<th>Parameter</th>
<th>Unit</th>
<th>Value</th>
</tr>
</thead>
<tbody>
<tr>
<td>( P_{mi} )</td>
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<td>50</td>
<td>( T_i )</td>
<td>K</td>
<td>365.15</td>
</tr>
<tr>
<td>( P_{fi} )</td>
<td>10⁶ Pa</td>
<td>60</td>
<td>( P_{BT} )</td>
<td>10⁶ Pa</td>
<td>50</td>
</tr>
<tr>
<td>( I_{imb} )</td>
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<td>0, 0.1, 0.3</td>
<td>( C_f )</td>
<td>10⁻⁹ Pa⁻¹</td>
<td>20</td>
</tr>
<tr>
<td>( C_m )</td>
<td>10⁻⁹ Pa⁻¹</td>
<td>0.1</td>
<td>( C_w )</td>
<td>10⁻⁹ Pa⁻¹</td>
<td>0.4</td>
</tr>
<tr>
<td>( \mu_w )</td>
<td>10⁻³ Pa·s</td>
<td>0.88</td>
<td>( \mu_g )</td>
<td>10⁻³ Pa·s</td>
<td>0.02</td>
</tr>
<tr>
<td>( T_{pc} )</td>
<td>K</td>
<td>201</td>
<td>( P_{pc} )</td>
<td>10⁶ Pa</td>
<td>4.5</td>
</tr>
<tr>
<td>( P_L )</td>
<td>10⁶ Pa</td>
<td>2.95</td>
<td>( V_L )</td>
<td>sm³/m³</td>
<td>0.3</td>
</tr>
<tr>
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<td>m</td>
<td>1200</td>
<td>( h_l )</td>
<td>m</td>
<td>50</td>
</tr>
<tr>
<td>( m_l )</td>
<td>Dimensionless</td>
<td>20</td>
<td>( n_{cl} )</td>
<td>Dimensionless</td>
<td>3</td>
</tr>
<tr>
<td>( \varphi_{pm} )</td>
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<td>0.04</td>
<td>( K_m )</td>
<td>10⁻⁹ µm²</td>
<td>200</td>
</tr>
<tr>
<td>( B_w )</td>
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<td>( \alpha_m )</td>
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</tr>
<tr>
<td>( W_{fo} )</td>
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<td>( l_o )</td>
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<td>( R_W )</td>
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<td>0.7</td>
</tr>
<tr>
<td>( R_L )</td>
<td>Dimensionless</td>
<td>0.7</td>
<td>( \theta )</td>
<td>rad</td>
<td>( \pi/6 )</td>
</tr>
<tr>
<td>( m )</td>
<td>Dimensionless</td>
<td>20</td>
<td>( a )</td>
<td>s</td>
<td>100,000</td>
</tr>
</tbody>
</table>
Figure 2. The relationship between RNP’, RNP, and tMB for flow back of shale gas wells.

3. EFNV Inversion

In this section, a mathematical model was developed to invert the volume of an effective fracture network in shale gas using a tree-shaped fractal fracture flow back approach. Then, based on the flow back data of shale gas well, a set of genetic algorithm workflows suitable for the effective fracture network volume inversion of shale gas is developed and combined with a genetic algorithm. An example was taken from shale fracturing wells in southern Sichuan, where the inversion of effective fracture network volume was conducted for 162 wells. A basic data set of fracture network volume was obtained.

3.1. Statistical Evaluation Methods

The following four statistical descriptors are introduced to evaluate the reliability of the fitting between the flow back data (Qwsc and Qgsc) and in the predicted data of the model (Qw and Qg), yi is the observed value, fi is the predicted value, and N is the number of samples.

(1) Coefficient of determination ($R^2$)

The closer the $R^2$ value is to 1, the better the predictive performance of the model.

$$ R^2 = 1 - \frac{\sum_{i=1}^{N} (y_i - f_i)^2}{\sum_{i=1}^{N} (y_i - \bar{y})^2} $$

(67)

$$ \bar{y} = \frac{1}{N} \sum_{i=1}^{N} y_i $$

(68)

(2) Root mean square error (RMSE)

RMSE is the standard deviation of the error between the observed values (Qwsc and Qgsc) and the predicted values (Qw and Qg). The smaller the RMSE, the better the prediction performance of the model.

$$ RMSE = \sqrt{\frac{1}{N} \sum_{i=1}^{N} (y_i - f_i)^2} $$

(69)

(3) Slope of regression line ($K$)

The $K$ value is the slope of the fitted linear regression equation between the observed values (Qwsc and Qgsc) and predicted values (Qw and Qg).
(4) Willmott’s index of agreement ($IA$)

The range of $IA$ is $[0,1]$: $IA = 1$ indicates that the forecast is perfect, and $IA = 0$ indicates that the forecast is invalid.

$$IA = 1 - \frac{\sum_{i=1}^{N} (y_i - f_i)^2}{\sum_{i=1}^{N} (|f_i - \bar{y}| + |y_i - \bar{y}|)^2}$$

(71)

According to statistical recommendations, a reliable result can be evaluated by $R^2 > 0.64$, $0.85 < K < 1.15$, or $IA > 0.80$ [30].

3.2. Fitness Function

The goal was to find the most suitable fracture network structure through flow back data inversion, that is, the flow back water and gas production predicted by the model should be the same or very close to the actual monitored flow back data. Therefore, the fitness function was established based on the idea of maximizing the determination coefficient $R^2$ between the predicted and the observed value. The fitness function is as follows:

$$F(\tilde{x}) = \begin{cases} f(\tilde{x}) & \tilde{x} \in \text{feasible region} \\ f(\tilde{x}) + \text{penalty}(\tilde{x}) & \tilde{x} \notin \text{feasible region} \end{cases}$$

(72)

where

$$f(\tilde{x}) = \frac{\sum_{i=1}^{N} (Q_{wsci} - Q_{wpredi})^2 \sum_{i=1}^{N} (Q_{gsci} - Q_{gpredi})^2}{\sum_{i=1}^{N} (Q_{wsci} - Q_{wsci})^2 \sum_{i=1}^{N} (Q_{gsci} - Q_{gsci})^2}$$

(73)

$$\text{penalty}(\tilde{x}) = \begin{cases} 10^k p_f & \text{or} \ p_m \notin \text{feasible region} \\ 0 & \text{or} \ p_f \text{ or } p_m \notin \text{feasible region} \end{cases}$$

(74)

The decision variables were as follows:

$$\tilde{x} = (x_1, x_2, \ldots, x_{12})$$

(75)

where

$$x_1 = l_0 \quad x_2 = W_{f0} \quad x_3 = m \quad x_4 = R_w$$
$$x_5 = R_h \quad x_6 = R_L \quad x_7 = \theta \quad x_8 = p_{BT}$$
$$x_9 = p_{f_i} \quad x_{10} = \alpha_{mf} \quad x_{11} = C_f \quad x_{12} = I_{imb}$$

(76)

The optimization goal was as follows:

$$\minimize F(\tilde{x})$$

(77)

The variable upper and lower bounds were as follows:

$$LB_i \leq x_i \leq UB_i \quad (i = 1, 2, \ldots, 12)$$

(78)

The constraints were as follows:

$$V_{fi} \leq TIV$$

(79)
where

$$V_{fi} = x_1 x_2 h_{l0} \frac{(1 - (nx_4 x_5 x_6)^{n+1})}{1 - nx_4 x_5 x_6}$$  \hspace{1cm} (80)$$

where \(\text{Penalty}(x)\) is the penalty function, which is taken as \(10^8\) in this paper; \(Q_{wsci}\) is the flow back fluid volume actually measured at the i-th moment, \(m^3/\text{min}\); \(Q_{gsci}\) is the gas production volume actually measured at the i-th moment, \(m^3/\text{min}\); \(Q_{wpredi}\) is the gas production volume calculated by the flow back model at the i-th time moment, \(m^3/\text{min}\); \(\overline{Q}_{wsci}\) is the average flow back fluid volume actually measured, \(m^3/\text{min}\); \(\overline{Q}_{gsci}\) is the average gas production volume actually measured by the shale gas well, \(m^3/\text{min}\); \(l_0\) is the initial fracture length, \(m\); \(W_0\) is the initial fracture width, \(m\) is the number of fractures; dimensionality; \(R_w\) is the fracture width ratio, dimensionless; \(R_h\) is the fracture height ratio, dimensionless; \(R_l\) is the fracture length ratio, dimensionless; \(\theta\) is the fracture bifurcation angle, rad; \(p_{BT}\) is the matrix gas breakthrough pressure, MPa; \(p_{fi}\) is the initial fracture pressure, MPa; \(\alpha_{mf}\) is the channeling factor, \(m^{-2}\); \(C_f\) is fracture compression coefficient, \(10^{-9} \text{ Pa}^{-1}\); \(I_{imb}\) is the shale reverse imbibition index, dimensionless; \(L_B\) is the lower limit of fitting parameters for flow back data inversion; \(U_B\) is the upper limit of fitting parameters for flow back data inversion; \(V_0\) is the initial effective fracture volume, \(m^3\); \(TIV\) is the total injected fracturing fluid volume, \(m^3\); \(h_0\) is the initial height of tree-shaped fractal fractures, \(m\); and \(n\) is the bifurcation number of the tree-shaped fractal fracture, dimensionless.

### 3.3. Genetic Algorithm Workflow

The genetic algorithm (GA) was established by Holland [31] and inspired by natural selection in biological evolution. Three basic operators were used to generate high-quality solutions for optimization and search problems: selection, crossover, and mutation. The GA is used to optimize a given objective function (fitness function). The inversion work was conducted using shale gas well flow back data to minimize errors between the actual flow back data \((Q_{wsci} \text{ and } Q_{gsci})\) and the predicted data from the fracture network model \((Q_w \text{ and } Q_g)\). Therefore, the fitness function included the optimization of the dual objectives of gas production and water production.

The genetic algorithm was used to predict the fracture network. The workflow for inversion of effective fracture network volume is shown in Figure 3. The inversion simulation process is as follows:

Step 1: The inversion simulation starts. Genetic algorithm parameters are shown in Table 3, and the upper and lower limits of the flow back model parameters are shown in Table 4;

Step 2: The basic parameters of shale gas wells are inputted, including flow back data, fracturing operation parameters, initial reservoir parameters, etc.;

Step 3: The bottom hole flowing pressure is calculated as the input value through the Beggs–Brill model [32];

Step 4: An initial total group of genetic algorithm fitting parameters is formed;

Step 5: The predicted values \((Q_w \text{ and } Q_g)\) are calculated through the flow back model;

Step 6: The fitness function value is calculated;

Step 7: Judging whether all the best fitting parameter values are found, or whether the termination condition is met;

Step 8: If the judgment result is “yes”, then the fitting parameters are stored; if the judgment result is “no”, then genetic algorithm selection operation, crossover operation, and mutation operation are performed to generate the next generation population of fitting parameters, and from step 5 one starts recounting.

**Table 3.** Parameter settings of genetic algorithm for fitting flow back model parameters.
<table>
<thead>
<tr>
<th>Genetic Algorithm Parameters</th>
<th>Value</th>
</tr>
</thead>
<tbody>
<tr>
<td>Population size</td>
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<tr>
<td>Maximum algebra</td>
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</tr>
<tr>
<td>Population initialization method</td>
<td>Random method</td>
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<tr>
<td>Fitness function</td>
<td>Equation (72)</td>
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<td>Genetic selection</td>
<td>Roulette</td>
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<tr>
<td>Termination condition</td>
<td>Maximum algebra</td>
</tr>
<tr>
<td>Crossover probability</td>
<td>85%</td>
</tr>
<tr>
<td>Mutation probability</td>
<td>15%</td>
</tr>
</tbody>
</table>

Table 4. Upper and lower limits of fitting parameters for flow back data inversion.

<table>
<thead>
<tr>
<th>Parameter</th>
<th>Unit</th>
<th>Lower</th>
<th>Upper</th>
</tr>
</thead>
<tbody>
<tr>
<td>$l_0$</td>
<td>m</td>
<td>1</td>
<td>300</td>
</tr>
<tr>
<td>$W_0$</td>
<td>m</td>
<td>0.000001</td>
<td>0.02</td>
</tr>
<tr>
<td>$m$</td>
<td>Dimensionless</td>
<td>1</td>
<td>500</td>
</tr>
<tr>
<td>$R_w$</td>
<td>Dimensionless</td>
<td>0.00001</td>
<td>1</td>
</tr>
<tr>
<td>$R_h$</td>
<td>Dimensionless</td>
<td>0.00001</td>
<td>1</td>
</tr>
<tr>
<td>$R_L$</td>
<td>Dimensionless</td>
<td>0.00001</td>
<td>1</td>
</tr>
<tr>
<td>$\theta$</td>
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<td>$\pi/2$</td>
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<td>MPa</td>
<td>0</td>
<td>$p_{mi}$</td>
</tr>
<tr>
<td>$p_{6}$</td>
<td>MPa</td>
<td>0</td>
<td>$2p_{mi}$</td>
</tr>
<tr>
<td>$\alpha_{mi}$</td>
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<td>1000</td>
</tr>
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<td>$C_i$</td>
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<td>0.1</td>
<td>1000</td>
</tr>
<tr>
<td>$I_{imb}$</td>
<td>Dimensionless</td>
<td>0</td>
<td>1</td>
</tr>
</tbody>
</table>

Figure 3. Genetic algorithm workflow for inversion of effective fracture network volume.

3.4. Model Validation

3.4.1. Analysis of Production

The shale gas wells in southern Sichuan were evaluated by the established EFNV inversion method, and the EFNV data set of the block was obtained. The average EFNV
was $1497.8 \times 10^4$ m$^3$, the standard deviation was $517.0 \times 10^4$ m$^3$. The relationship between EFNV and test production, 60-day cumulative gas production, 90-day cumulative gas production, 120-day cumulative gas production, and 20-year technically recoverable reserves were analyzed.

The relationships between the EFNV obtained from the inversion and the test production, 60-day cumulative gas production, 90-day cumulative gas production, 120-day cumulative gas production, and 20-year technically recoverable reserves are shown in Figures 4–8. It can be seen that the correlation decreases in the order (test production ($R = 0.684$) > 60-day cumulative gas production ($R = 0.576$) > 90-day cumulative gas production ($R = 0.566$) > 120-day cumulative gas production ($R = 0.541$) > 20-year technically recoverable reserves ($R = 0.371$)). The reason is that the EFNV obtained based on the flow back in this paper was mainly obtained from the inversion of the data within the first few hundred hours to two thousand hours of the flow back production, so its correlation with the test production is the highest.

The longer the production time is, the correlation with cumulative gas production gradually decreases. This is due to the limitations of the flow back data. However, the positive correlation between the effective fracture network volume and test production, 60-day cumulative gas production, 90-day cumulative gas production, 120-day cumulative gas production, and 20-year technically recoverable reserves (EUR) shows that if a larger effective fracture network volume is obtained, the probability of obtaining a larger gas production is greater. From the perspective of fracturing engineering, which can be used as an important parameter to evaluate fracturing effects and production prediction, this proves the reliability of the inversion results.

![Figure 4. Relationship between effective fracture network volume and test production.](image1)

![Figure 5. Relationship between effective fracture network volume and 60-day cumulative gas production.](image2)
3.4.2. Microseismic Monitoring

Some wells were monitored by microseismic monitoring during the fracturing process in southern Sichuan. The relationship between the stimulated reservoir volume (SRV) of 20 microseismic monitoring wells and the EFNV obtained by flow back inversion was statistically analyzed. As shown in Figure 9, the correlation coefficient between them was $R = 0.705$, which belongs to a moderate positive correlation ($0.5 < R < 0.8$). The more fractured the reservoir detected by microseismic monitoring, the larger the SRV, and the greater the probability that the corresponding effective fracture network volume will be
larger, which further indicates that the EFNV inversion method is reliable based on flow back, and the obtained EFNV can be used as an important parameter for evaluating fracturing effects and optimizing fracturing operation parameters.

Figure 9. Relationship between inversion EFNV and microseismic monitoring SRV.

4. Field Application

We gathered flow back data post-fracturing to input into the established tree-shaped fractal fracture flow back mathematical model for EFNV inversion. Then, we utilized the genetic algorithm workflow to process the data and predict fracture network parameters for optimization. We applied the inversion model to shale gas wells in the field, such as those in southern Sichuan Basin, to calculate the EFNV and key parameters for optimizing fracturing operations.

The fracturing fluid flow back analysis model and the EFNV inversion workflow were used for a field application. The flow back production data of a shale gas well H3 in southern Sichuan (Figure 10) was taken as an example. The statistics of the basic parameters are shown in Table 5.

Table 5. Basic parameters of shale gas well H3.

<table>
<thead>
<tr>
<th>Parameter</th>
<th>Unit</th>
<th>Value</th>
<th>Parameter</th>
<th>Unit</th>
<th>Value</th>
</tr>
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<tbody>
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</tr>
<tr>
<td>$C_m$</td>
<td>$10^{-9}$ Pa$^{-1}$</td>
<td>0.3</td>
<td>$C_w$</td>
<td>$10^{-9}$ Pa$^{-1}$</td>
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</tr>
<tr>
<td>$\mu_w$</td>
<td>$10^{-3}$ Pa$\cdot$s</td>
<td>0.28</td>
<td>$\mu_g$</td>
<td>$10^{-3}$ Pa$\cdot$s</td>
<td>0.042</td>
</tr>
<tr>
<td>$T_{PC}$</td>
<td>K</td>
<td>190</td>
<td>$P_L$</td>
<td>$10^6$ Pa</td>
<td>2.98</td>
</tr>
<tr>
<td>$n_l$</td>
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<td>28</td>
<td>$n_{eL}$</td>
<td>Dimensionless</td>
<td>0.29</td>
</tr>
<tr>
<td>$\phi_m$</td>
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<td>$K_m$</td>
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</tr>
<tr>
<td>$B_w$</td>
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<td>1.05</td>
<td>$n$</td>
<td>Dimensionless</td>
<td>2</td>
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The hydraulic fracturing fracture network characteristics inversion was performed on the flow back production data of Well H3 based on the proposed flow back model and the flow back data inversion genetic algorithm. The water transient history fitting of well H3 is shown in Figure 11. Among them, $R^2(Q_w) = 0.883$, $R^2(Q_g) = 0.927$, $IA(Q_w) = 0.969$, $IA(Q_g) = 0.982$, $K(Q_w) = 1.03$, and $K(Q_g) = 0.95$; according to the statistical recommendation standard, the inversion of fracture characteristics of Well H3 was reliable. The root mean square error $RMSE$ of the predicted value and the measured value of $Q_w$ and $Q_g$ were 1.54 m$^3$/h and 0.14 × 10$^4$ m$^4$/h, respectively. The changes in the bottom hole flow pressure, fracture network pressure, shale matrix pressure, and wellhead nozzle size during the flow back process are shown in Figure 12. It can be seen that the pressure drop in the fracture network is larger than that in the shale matrix after the well is opened. After the first well shut-in, the gas in the matrix channeled into the fractures due to the pressure difference between the fracture network system and the matrix system. In the network, the fracture network pressure gradually rises to be equal to the matrix pressure. After the second well opening, the fracture network pressure begins to decrease again until the second well shut-in, and the fracture pressure gradually rises again. The network pressure did not rise back to equal the matrix pressure due to the short shut-in time of the second well. It can be clearly seen from Figure 11 that the fitting effect of the flow back water data is average in the early part. It is speculated that the possible reason is that the flow back data records on site are not accurate due to frequent changes in the size of the choke nozzle, and the size of the choke nozzle changed four times before the first shut-in and changed nine times before the second shut-in (Figure 12).
The fracture characteristics of Well H3 obtained through the genetic algorithm workflow inversion are shown in Table 6, including tree-shaped fractal fracture network structure parameters, fracture system original pressure, matrix gas breakthrough pressure, fracture compressibility coefficient, reverse imbibition index, effective fracture network volume, etc. Two types of hydraulic fracture networks will be formed after fracture network fracturing. Some fractures contribute to flow conduction and others are isolated due to fracture closure and for other reasons. The fracture network with a conductivity contribution is a highly conductive fracture network that allows matrix shale gas to enter and flow into the wellbore along it; these are also called effective fractures. A law of harmonic decline (HD) from the relationship between water production and cumulative water production can be observed by Lee [33], which can estimate the effective fracture volume (Table 7 and Figure 13). It can be seen from Figure 13 that when the HD model was applied to Well H3, the previous water flow data were overestimated, so the effective initial fracture volume would be overestimated.

Alkouh [2] observed a linear relationship between flow normalized pressure (RNP) and mass balance time \( t_{MB} \) during the flow back process, and the effective initial fracture volume could be obtained (Table 7 and Figure 14). However, the fracture compressibility coefficient was ignored in the Alkouh model when the total compressibility coefficient was calculated, so the effective fracture volume would be overestimated.

As shown in Figure 15, the effective initial fracture volume calculated by the method proposed in this paper, in which the gas-water two-phase flow and fracture compressibility were taken into account, and the calculation results were of the same order of magnitude as those of the HD model and the Alkouh model, and were smaller than those of the two models. It shows that the inversion model of fracture network characteristics based on flow back is reasonable, and the applicability of the model is stronger. Shale gas fracturing generally has the problem of a low flow back rate [34], and the final estimated flow back rate of Well H3 was 20.8%. Most of the fracturing fluid is locked in the isolated ineffective fracture network with no conductivity, and it is difficult to flow back. This is the main reason for the low flow back rate.

Table 6. Inversion results of genetic algorithm workflow.

<table>
<thead>
<tr>
<th>Parameter</th>
<th>Unit</th>
<th>Value</th>
<th>Parameter</th>
<th>Unit</th>
<th>Value</th>
</tr>
</thead>
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<tr>
<td>( \bar{l}_0 )</td>
<td>m</td>
<td>50.9</td>
<td>( W_{fl} )</td>
<td>m</td>
<td>0.0154</td>
</tr>
<tr>
<td>( m )</td>
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<td>( R_L )</td>
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</tr>
<tr>
<td>( R_W )</td>
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<td>0.614</td>
<td>( R_n )</td>
<td>Dimensionless</td>
<td>0.616</td>
</tr>
<tr>
<td>( \theta )</td>
<td>rad</td>
<td>1.07</td>
<td>( P_{BT} )</td>
<td>( 10^6 ) Pa</td>
<td>58.79</td>
</tr>
<tr>
<td>( P_B )</td>
<td>( 10^6 ) Pa</td>
<td>58.81</td>
<td>( \alpha_{inf} )</td>
<td>m(^2)</td>
<td>575</td>
</tr>
<tr>
<td>( C_t )</td>
<td>( 10^{-9} ) Pa(^{-1})</td>
<td>179</td>
<td>( I_{imb} )</td>
<td>Dimensionless</td>
<td>0</td>
</tr>
<tr>
<td>EFNV</td>
<td>( 10^4 ) m(^3)</td>
<td>1172</td>
<td>( x_I )</td>
<td>m</td>
<td>90.85</td>
</tr>
</tbody>
</table>
Table 7. Results comparison of different models for estimating the initial EIFV.

<table>
<thead>
<tr>
<th>Model</th>
<th>Unit</th>
<th>Value</th>
</tr>
</thead>
<tbody>
<tr>
<td>HD model</td>
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<td>21,192</td>
</tr>
<tr>
<td>Alkouh model</td>
<td>m³</td>
<td>15,895</td>
</tr>
<tr>
<td>Established model</td>
<td>m³</td>
<td>10,643</td>
</tr>
</tbody>
</table>

Figure 13. HD model.

Figure 14. Alkouh model [2].

Figure 15. Comparison of initial effective fracture network volume estimated by different models.

The inversion effective fracture network volume fitting curves of some shale gas fracture network fracturing wells in southern Sichuan are shown in Figure 16. The model established can fit the actual field data very well in this paper, and it can be used to invert the EFNV efficiently after shale gas reservoir stimulation in southern Sichuan.
5. Conclusions

The inversion method of shale gas effective fracture network volume based on flow back data was established. Several effective fracture network volume inversion cases were simulated. The main conclusions are summarized below:

1) A two-phase flow back model of the tree-shaped fractal fracture network was established based on the flow back data, and the reliability of the model was verified by combining the RNP and RNP'. The model is reasonable, reliable, and has strong field adaptability.

2) Based on the principle of the genetic algorithm (GA), the GA workflow of EFNV inversion was established and combined with the two-phase flow back model, and then the EFNV inversion was carried out for shale gas wells in southern Sichuan. The results showed that the inversion of EFNV had a positive correlation with production and microseismic monitoring results, which confirmed the reliability of the inversion results.
(3) The calculation showed that the results were in the same order of magnitude as those of the HD model and the Alkouh model, and were smaller than the calculation results of the two models, indicating that the fracture network inversion model proposed is reasonable and more applicable.

(4) The fracture network feature inversion method can obtain tree-shaped fractal fracture network structure parameters and effective fracture network volume. It has important theoretical guiding significance and field application value for improving the calculation accuracy of EFNV and fracturing effect evaluation.

(5) The model does not consider the effects of interference between wells and well channeling from adjacent wells, and accordingly the prediction of water production after well strings is relatively weak. It is recommended that the model can further consider the impact of simultaneous flow back of multiple wells and layers and the salinity of flow back water in the future.

Author Contributions: D.T.: conceptualization, methodology; J.W.: writing—review and editing; J.Z.: writing—original draft preparation; B.Z.: data collection; Y.S.: visualization, investigation; C.S.: formal analysis; L.R.: visualization; Y.H.: original draft preparation; Z.W.: software. All authors have read and agreed to the published version of the manuscript.

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Conflicts of Interest: The authors declare no conflicts of interest.

References


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